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CSTP VARIATION APPLICATION

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# HPC COMPANY DOCUMENT

## COMPANY DOCUMENT ENVIRONMENTAL PERMIT VARIATION APPLICATION: HINKLEY POINT C CONSTRUCTION SEWAGE TREATMENT PLANT

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Date of Issue	Refer to EDRMS
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Technical Reviewer	James Holbrook
Author	Dr Richard Mitchener / Jessica Harris

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**APPROVAL: ENVIRONMENTAL PERMIT VARIATION APPLICATION:  
HINKLEY POINT C CONSTRUCTION SEWAGE TREATMENT PLANT**

<b>Prepared by:</b>	<b>Name:</b> Dr Richard G.R. Mitchener <b>Title:</b> Site Environmental Engineering Lead	Date: Refer to EDRMS
	<b>Name:</b> Jessica Harris <b>Title:</b> Environmental Compliance Specialist	
<b>Verified by:</b>	<b>Name:</b> James Holbrook <b>Title:</b> Environmental Compliance Manager	Date: Refer to EDRMS
<b>Approved by:</b>	<b>Name:</b> Chris Fayers <b>Title:</b> Head of Environment	Date: Refer to EDRMS

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# Non-Technical Summary

NNB Generation Company (HPC) Limited, is building a new nuclear power station on the northern coast of Somerset. To support the workforce required to deliver the power station, a construction-phase sewage treatment plant (CSTP) has been installed and commissioned at the site. The CSTP provides primary and secondary treatment of domestic-type sewage from the welfare facilities as well as ultraviolet disinfection of the effluent. The treated effluent is discharged from site via a discharge point towards the end of the site's jetty which minimises any potential impacts on the foreshore. The discharge is regulated under an Environmental Permit issued by the Environment Agency (EPR/XP3321GD).

The number of workers required on site is now predicted to be higher than the number for which the plant was designed. It is also possible that an extension to the workers' accommodation campus may be required, with the provision of an additional 500 beds being considered. This means that the CSTP as currently installed would not be able to manage the amount of ammonia that would be produced.

In addition, it is apparent that sewage effluent produced by Hinkley Point C is different from the best-available predictions that were used for the design; the volume produced is lower than anticipated, but ammonia concentrations are higher than anticipated and this leads to challenges for the CSTP. The nature of the working patterns on a large construction site also leads to challenges. Workforce numbers on site vary over a 24-hour period and through the week. This means that the flows and concentrations into the CSTP vary significantly; as the CSTP is primarily a biological degradation process this variability impacts the CSTP's efficiency. Due to the large variation in inputs at the site it is not feasible to design a plan that will work well under all conditions. A number of modifications have been made to improve the CSTP's performance. These are detailed in this report.

In order to address these challenges, NNB Generation Company (HPC) Limited is proposing to increase the concentration of ammonia that can be discharged from the site to 80mg/l. Detailed modelling has been undertaken which demonstrates that this concentration will not have an adverse impact on the environment.

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# 1 INTRODUCTION

NNB Generation Company (HPC) Limited (NNB HPC) is developing the first of new generation of nuclear power station on the north Somerset coast, approximately 13km northwest of Bridgwater. To support the construction works, welfare facilities are provided on site and a construction-phase sewage treatment plant (CSTP) has been constructed to deal with the foul waste from these facilities. This plant treats the sewage to specified criteria before the final effluent is discharge into the Bristol Channel from the site's jetty.

## 1.1 Purpose

The variation application, for which this report provides supporting information, seeks to amend the permitted levels of ammoniacal nitrogen that may be discharged from the Hinkley Point C (HPC) Construction Sewage Treatment Plan (CSTP).

## 1.2 Scope

The permit (EPR/XP3321GD/004) which NNB HPC is seeking to vary covers the discharge of domestic-type sewage after secondary treatment and ultraviolet disinfection. Other aqueous effluents arising from the construction activities at HPC are treated and discharged under the Construction Water Discharge Activity (CWDA) permit (EPR/JP3122GM/V009&010).

This application only relates to the construction phase; a separate Operational Water Discharge Activity (OWDA) permit (EPR/HP3228XT) will govern discharges from the power station once it is operational. This permit includes treated sewage effluent from the workers that will operate the plant.

## 1.3 Summary description of the proposed variation

NNB HPC is requesting an increase in the ammoniacal nitrogen limit to support the continued development of the project in an environmentally sustainable way. The current limit is 20 mg/l and it is requested that this be increased to 80mg/l. As detailed in Sections 2.1.1 and 2.2 of the report, this is necessary because of need for an increased workforce above that for which the CSTP was designed, the unusual working patterns at HPC and the dynamic nature of the site which precluded a fully piped sewerage network.

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### 1.4 Contents of this report

The report includes the following sections:

- Section 2 summarises the Water Discharge Activity as currently permitted including a description of the plant and the measures that NNB HPC has taken to address the challenges at HPC;
- Section 3 sets out the proposed variation including the assessment of the potential environmental effects and further improvement measures that may be implemented.
- Section 3 summarises the conclusions.

The application forms are included in Appendix A, and the technical reports are included in Appendices B and C. Modelling files will be provided to the Environment Agency under sperate cover.

### 1.5 Definitions

Abbreviation	Definition
HPC	Hinkley Point C
NNB HPC	NNB Generation Company (HPC) Limited
CWDA	Construction Water Discharge Activity (Permit)
CSTP	Construction Sewage Treatment Plant
HAI	Construction Sewage Treatment Plant
PST	Primary Settlement Tank
FST	Final Settlement Tank
RBC	Rotating Biological Contactor
MCERTS	Monitoring Certification Scheme
BOD	Biological Oxygen Demand
TSS	Total Suspended Solids
OSM	Operator Self-monitoring
MBBR	Moving Bed Bioreactor
DIN	Dissolved Inorganic Nitrogen (the sum of total ammonia, nitrate and nitrite expressed as mass of nitrogen).

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## 2 CURRENT WATER DISCHARGE ACTIVITY

### 2.1 Description of designed plant

HPC is a large construction site with a variety of office-based and site-based personnel on site each day. Office and welfare space, including showers, is provided for these workers in four large buildings. Canteen facilities are provided for those staff within these buildings; food preparation is split between on-site cooking and a central production kitchen. In addition, a 510-bedroom accommodation campus is provided adjacent to the site with the sewage produced therein being pumped onto the main construction site.

The plant was designed to address the expected effluent volumes and quality from the then-predicted workforce and resident numbers using the industry-standard approach (British Water, 2013).

On the basis of the predicted flow rates and loading of key contaminants a multi-phase treatment approach was designed and installed. This was described in detail on the original application report (NNB HPC, 2018), but in summary comprises:

- An inlet pumping station that receives flows from the gravity and pumped networks as well as providing a reception point for sewage delivered by tankers. This pumping station provides flow balancing to smooth out the operational parameters.
- A primary screen to remove “rag” and other coarse materials; this comprised a screen and screw conveyor to move the debris to a skip from where it is taken to an appropriately permitted facility for disposal;
- A flow splitting step to distribute incoming flows between the three treatment trains;
- Primary settlement tanks (PSTs) to allow settlement of sludge including sludge pumped from the final settlement step. Sludges are removed from site by tanker to a permitted sludge reception centre.
- Rotating Biological Contactors (RBCs) where biological films are developed on rotating media; the bacteria within these films treat the liquid portion of the sewage by oxidising the ammonia to nitrate or nitrite (the nitrification process). Each treatment train contains two RBCs operating in parallel so there are six in total in the plant.
- Final settlement tanks (FSTs) take the effluent from the RBCs and settle out the remaining solids including the bacterial film that are sloughed off the rotating discs as part of the natural process. There is one FST per RBC and therefore there are six FSTs on site. The settled water flows over a weir and the settled sludges are pumped into the primary settlement tanks.

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- Tertiary treatment by ultraviolet light to provide disinfection; three ultraviolet units, one per treatment train, were provided.
- Recirculation options for each treatment stream to allow maintenance, support the UV lamps which require cooling and to allow diversions back to the inlet tank in emergencies; and
- A final effluent pumping station to pump the combined flow to the header tank before discharge into the Bristol Channel via pipes along the HPC jetty. MCERTS flow monitoring is provided at the Final Effluent Pumping Station and a sampling tap is provided at the header tank at the landward end of the jetty.

#### 2.1.1 Compliance challenges

Commissioning of the sewage treatment plant was undertaken over an extended period until compliant samples for the three numerical compliance values (ammoniacal nitrogen, total suspended solids (TSS) and biological oxygen demand (BOD) were received for 28 consecutive days. After achieving this condition discharge of treated effluent commenced on 16<sup>th</sup> February 2022. Although the frequency of accredited laboratory analysis was reduced to that needed under the permit at that point, site-based unaccredited analyses of ammoniacal nitrogen and “clarity” (an analogue for TSS) continues to be monitored daily. These data, together with the externally analysed Operator Self-Monitoring (OSM) samples have indicated that the plant continues to be challenged in dealing with the site’s effluent of the reasons set out hereunder.

The site is operational for 24 hours per day, albeit numbers for staff overnight are much reduced from the daytime peaks. Similarly, the site is operational 7 days per week with numbers varying at the time of writing from c. 10,000 in a 24-hour period in the middle of the week to c. 2,000 on a “non-working” weekend. This “shock loading” is challenging for a biological plant to address, leading to elevated levels of ammoniacal nitrogen in the later part of the week. This challenge is exacerbated in winter when lower ambient temperatures further impinge on the efficiency of the biological treatment.

The plant was designed based on “best estimate” application of the code of practice (British Water, 2013). However, it has become apparent that these values overstated the volume produced but underestimated the concentration of ammoniacal nitrogen. Therefore, although the flow rates into the plant remain well below the design volume for the loading such that only two of the three treatment trains have been brought into full use, the ammoniacal nitrogen loading is sometimes above that that can be managed by these two modules. The BOD (a measure of the amount of organic material present) is consistent with the original calculations and the imbalance also affects the plant’s efficacy. In addition, testing has indicated that the alkalinity of the influent is lower than would be expected and it is known (USEPA, 1973) that elevated acidity can significantly affect the efficiency of ammonia removal. It is likely that the lower-than-expected flow rates are, to some extent contributing to the elevated ammonia as sewage residence time within the site’s network will be longer than originally anticipated allowing biological processes to develop.

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A further challenge arises due to the dynamic nature of site and then need to provide welfare facilities close to the working areas. It is not practicable to plumb many of these facilities into the sewerage network and therefore for raw sewage is stored for an extended period beyond the eight-hours usually taken as the point at which septicity may develop. Septicity leads to significantly elevated ammonia levels (averaging 200mg/l) which is above what would usually be expected. This effluent is currently collected by tanker and removed from site as it is beyond the plant's current treatment capability.

### **2.1.2 Plant Amendments to support Compliance**

During and after the commissioning of the plant a number of improvements were made to support compliance in the novel circumstances at HPC. These included:

- Installing cloth filters (known as meccana filters) which operates in duty/standby arrangement to reduce suspended solids and adsorbed ammonia;
- The provision of a single UV plant to treat the total volume which enabled duty/standby to be provided and allowed for enhanced control to ensure that the required dose is provided;
- Provision of enhanced sludge settlement via addition tanks which enhanced the efficacy of the PSTs and reduced the residence time (age) of the sludge therein;
- Utilisation of spare RBC units to provide tertiary treatment to reduce ammoniacal nitrogen levels;
- Optimisation of pumping station controls to reduce sludge aging within the network despite the lower than anticipated flow rates;
- Amendments to the sludge removal system from the FSTs to improve sludge removal and limit sludge age;
- Installation of automatic monitoring of ammoniacal nitrogen and total suspended solids to enable any compliance challenges to be identified in real time and investigations undertaken in a timely way; and
- Utilisation of a bio-stimulant to support bacterial health during the winter period.

These modifications allowed the plant to meet the commissioning criteria such that discharge could be commenced and remained compliant for several months. However, when pumping of sewage from the east office commenced in June 2022 compliance became challenging with a number of breaches recorded. These were managed by changing plant operation and the plant came back into compliance rapidly. Further compliance challenges were realised during the winter months due to cold weather and especially after the Christmas period when the very reduced site numbers impact the biofilm's health.

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## 2.2 Further Site Development

Further increases in site workforce are being considered to support the completion of HPC and the generation of low carbon electricity as soon as possible. It is likely that the site's daily workforce peak will reach c.12,000. It is also possible that it may be necessary to expand the on-site workers' accommodation campus (Hinkley Campus) by up to 500 bed-spaces to support this effort. This will increase the load of ammoniacal nitrogen that the CSTP is required to treat significantly beyond the design loading. It is also likely that the diurnal, weekly and seasonal variations experienced by the plant will remain or increase, adding additional compliance challenges.

Consideration has been given to upgrading the CSTP to deal with the additional loading to deliver compliance with the existing permit. However, given the unusual challenges inherent in the treatment of sewage from a construction site it is unlikely that the existing limits could be met consistently.

### 2.2.1 Proposed Plant upgrades

It is intended to upgrade the CSTP to allow injection of magnesium hydroxide into effluent after the PST stage; this will increase the alkalinity within the system (that is the ability to buffer the acidity produced by the nitrification process). It is anticipated that this will allow the nitrification reaction to proceed at a higher rate; this will be confirmed by a trial on one of the treatment trains before wider deployment. Magnesium has been chosen as it is less corrosive than sodium hydroxide (the as-delivered pH will be 10) which reduces the health, safety and environmental challenges. Dosing rates will be set based on laboratory scale tests and a pH meter will also be used to monitor pH of effluent, stopping dosing if it rises above 9. During the trial, dosing will only be undertaken on weekdays, as the treatment of the lower inputs at the weekend is less likely to be constrained by the availability alkalinity. NNB HPC may automate this process in due course. The product used will consist of magnesium hydroxide and water only with no other chemicals. Therefore, so long as the pH is controlled as described there is no risk to the environment given that magnesium ions are ubiquitous in the sea and not hazardous.

NNB HPC is also considering providing additional treatment via the use of Moving Bed Biofilm Reactors (MBBRs), subject to successful trials. An MBBR may be used to provide a polishing step (as currently undertaken by Module 3) when site volumes are such that all three modules are needed for their original purpose. One or more MBBRs may also be used to provide some pre-treatment of the higher strength influent arising from the "deep-dig" welfare facilities.

All changes will be subject to control under the site's design change procedures and reflected in the Operation and Maintenance Manual for the plant.

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### 3 PROPOSED VARIATION

In order to support the project and the delivery of Net Zero, it is proposed to vary the permit to allow an increased concentration of ammoniacal nitrogen in the treated effluent to 80mg/l while still ensuring a high level of environmental protection. This will also facilitate the on-site treatment of the higher-strength wastes from the “deep-dig welfare facilities removing the need for this waste to be tankered from site. This will result in a reduction in lorry movements with the concomitant reduction in carbon dioxide emissions.

#### 3.1 Predicted flow rates

The likely flow rates from the increased population have been estimated following an analysis of the existing data. Due to the presence of the campus and the daily workforce analysis is complex however, a range of data has been used to enable realistic estimates to be derived.

Water usage at the campus is metered, and the daily occupancy is also recorded. This provides an estimate of what are use and as soon as production at the site. This data has been analysed over a period of approximately 13 weeks on the estimated flow rate per person is 110 L per head per day. This includes a margin to allow for beverages consumed on site and other external influences.

The volume produced by the workforce on site can then be estimated as the number of people on site each day is known, as is the volume of sewage produced. The volume removed from site by tanker was also included in the calculations. This calculation indicates that a reasonable estimate of the sewage produced by each worker is 50 litres per head per day.

Using these data, it was concluded that there is no requirement for an increase in flow rate to allow for the additional personnel on site required to complete the project.

#### 3.2 Predicted composition

Biological oxygen demand and total suspended solids produced to date have remained consistently with the estimates provided within flows and loads (British Water, 2013). Therefore, it is anticipated that the loading from the increased population will remain within the parameters that the plant was designed to deal with given the lower flow rates per person observed. It is not anticipated that there were any compliance challenges related to these parameters. However, ammoniacal nitrogen levels are higher than predicted, therefore, design criteria of plant will be exceeded for this parameter. In order to allow the continued

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development of HPC it is proposed that limit for ammoniacal nitrogen in the treated effluent is increased to 80mg/l.

## 3.3 Environmental Assessment

CEFAS (2023) was engaged to assess the potential impact of a range of scenarios and the report is included in Appendix A. This was undertaken to support NNB HPC's assessment of options and was undertaken before the analysis of flow rated from the campus and workforce was completed. Following the flow rate analysis, it is apparent that no increase in the permitted flow rate is needed and therefore only the existing flow rate scenario needs to be considered.

New modelling of the mixing of the effluent with the saline waters of the Bristol Channel was not required. Previous work (CEFAS, 2019 – see Appendix B) has assessed the dispersion of, *inter alia*, sewage-derived ammoniacal nitrogen into the estuary to support the CSTP permit application and the most recent variation to the CWDA Permit. This modelling therefore included:

- Groundwater containing up to 9.5mg/l of ammoniacal nitrogen with a flow rate of up to 20l/s;
- Tunnel effluent containing up to 9.5mg/l of ammoniacal nitrogen with a flow rate of up to 30l/s;
- Cold commissioning effluent with up to 271mg/l of ammoniacal nitrogen and a flow rate of up to 70l/s for up to 5.95 hours per day; and
- Treated sewage effluent containing up to 20mg/l of ammoniacal nitrogen and a flow rate of up to 20l/s.

It should be noted that the modelling did not consider tunnel effluent and cold commissioning together as it is expected that tunnel works will be completed in advance of significant commissioning starting.

CEFAS (2023) utilised the existing modelling to consider the extent of any plume that would arise as a result of the higher concentrations of ammoniacal nitrogen within the treated sewage effluent discharge. A simple mathematical approach was considered appropriate with a scaling factor applied to the previously reported results to consider the effects of the increased flow rate. The assessment concluded that:

- The extent of the plume where concentrations are above the Environmental Quality Standard (DEFRA, 2015), remains small in the context of the receiving water; and
- The plume is not predicated to interact with the specific interest features, *Sabillaria spp.* reefs (*S. spinulosa* and *S. alveolata*) and *Corallina spp.* that are recorded in the vicinity of the site.

Furthermore, although the effects of dissolved inorganic nitrogen (DIN) associated with sewage discharges have not been explicitly assessed, CEFAS (2019) has considered the effects of DIN released from site overall.

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Modelling described therein, using the CPM Model (Aldridge et al, 2008) indicates that due to the high turbidity of the receiving water nitrogen is not the limiting factor for phytoplankton growth within the estuary with light levels actually being the control. Therefore, the slight local increase in DIN levels that may arise from the increased limit will not adversely affect the receiving water's ecological health.

Data regarding ammoniacal nitrogen and DIB concentration in the effluent streams discharged via Outlet 12 is presented in appendix D.

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## 4 CONCLUSIONS

Previously undertaken complex hydrodynamic and hydro-chemical modelling has been utilised to assess the potential effects on the Bristol Channel of increasing the permitted concentration of ammoniacal nitrogen in the treated sewage effluent discharged from the HPC Construction site. These assessments have concluded that:

- The additional extent of any plume is very small with concentrations reducing to EQS within 46.04 metres of the discharge point compared to less than 7.16m under the already permitted limit;
- The area of the SAC with levels above the EQS is less than 0.002%; and
- The key species and habitats of interest are not exposed to concentrations above the EQS and therefore further assessment of any potential effects is not needed.

It is therefore concluded that the proposed variation will not have any likely significant effects on the protected site. Similarly, it is concluded that, due to the very localised effects, there will be no impact of Water Framework Directive status of either the Bridgwater Bay or River Parrett waterbodies.

It is therefore requested that the permit is varied such that:

- the limit for ammoniacal nitrogen set out in Schedule 3, Table S3.1 of the permit is increased to 80mg/l; and
- the description of the activity in Schedule 1, Table S1.1. is modified to read “Discharge treated sewage effluent after secondary treatment (including addition of approved chemicals) and subject to disinfection by ultraviolet irradiation via outlet 12”.

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## 5 REFERENCES

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**APPENDIX A ASSESSMENT OF AMMONIA DISCHARGES  
ASSOCIATED WITH TREATED SEWAGE AND  
COMMISSIONING AT HPC (TR581)**

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**CEFAS REPORT TR581 ASSESSMENT OF AMMONIA DISCHARGES ASSOCIATED WITH  
TREATED SEWAGE AND COMMISSIONING OF HPC  
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<b>DOCUMENT TITLE</b>	Cefas Report TR581 Assessment of ammonia discharges associated with treated sewage and commissioning of HPC
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<b>ISSUE REASON</b>	P1 - implementation
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03	12/06/2023	A. Griffith	Principle Scientist	D. Haverson	BEEMS Modelling Lead	H. Buckley	Nuclear Programme Site Lead (Hinkley Point)
04	19/06/2023	A. Griffith	Principle Scientist	D. Haverson	BEEMS Modelling Lead	H. Buckley	Nuclear Programme Site Lead (Hinkley Point)

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**BEEMS Technical Report TR581  
Assessment of Ammonia Discharges  
Associated with Treated Sewage and  
Commissioning of HPC**

Dr David Haverson, Andrew Griffith

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### Executive summary

The Hinkley Point C (HPC) Development Consent Order (DCO) was granted by the UK Secretary of State for Energy and Climate Change in March 2013. HPC environmental permit for the Construction Sewage Treatment System (Environment Agency's Permit number EPR/XP3321GD/V004) permits NNB GenCo to discharge a maximum of 20 mg/l of ammoniacal nitrogen from the sewage treatment system. The cold commissioning discharge permit (EPR/JP3122GM/V009&010) also allows for additional discharges of ammonia associated with the commissioning phase, tunnelling, and groundwater. Notably these two discharges will overlap during commissioning and therefore need to be considered together for assessment purposes. To support the delivery of HPC, NNB GenCo is considering varying the Construction Sewage Treatment System environmental permit (EPR/XP3321GD/V004) to allow an increased concentration of ammoniacal nitrogen within the permitted discharge. The aim of this assessment is to provide the evidence to support the decision to vary the discharge.

Presently, the discharge of ammoniacal nitrogen from the sewage treatment works was assessed, as 20 mg/l at an average flow rate of 13.3 l/s. To investigate the impact of varying the sewage treatment discharge, three different concentrations have been considered; 40, 60 and 80 mg/l of sewage. Additionally, an alternative flow rate mix has been considered, based on the current dewatering during construction, whereby the sewage flow rate is increased by 10 l/s and the groundwater decreased by 10 l/s, maintaining the overall average 38.3 l/s flow.

The assessments considered the release from the sewage treatment works as both a construction only discharge, plus a combined construction and commissioning discharge.

Applying the Environment Agency's Screening tests, the results of 'test 5' (allowable effective volume flux) showed that when considering construction alone, each scenario tested was within permissible limits. However, the partitioning of un-ionised ammonia is influenced by the physical conditions and this partitioning is not factored into the basic screening tests. Therefore, while the screening test was passed, further assessment of the discharges in terms of mixing calculations and nearfield modelling was conducted. When considering the combined construction and commissioning discharges, due to the considerable increase in ammonia from the commissioning phase, the screening tests were not passed. However, this is consistent with previous assessments (BEEMS Technical Report TR428) which required modelling to fully assess the potential implications of the commissioning discharges.

For the construction discharge alone, nearfield modelling using CORMIX showed that concentrations of un-ionised ammonia fall below the environmental quality standard (EQS) (21 µg/l) within <7.16 m of the discharge point for the original scenario (i.e., 20 mg/l total ammonia). This distance required to mix the discharge down to the EQS increased to a maximum of 46.04 m for the 80 mg/l discharge scenario, with the original flows, and to 82.08 m for 80 mg/l discharge with the alternative flow rates. While the estimated mixing zone was considerably larger under the new scenarios compared to the baseline scenario (increasing from ~7m to over 80 m), the mixing zone was still very small in respect to the scale of the receiving environment and therefore would not be expected to cause any significant environmental effects.

Reanalysis of the General Estuarine Transport Model (GETM) modelling results showed that during the period where the construction and commissioning discharges overlap, the discharge scenarios led to an estimated additional 0.11 to 0.31 µg/l of un-ionised ammonia with the original flow rates and 0.06 to 0.61 µg/l of un-ionised ammonia with the alternative flow rates at the locations of the sensitive biological receptors. From the time series of instantaneous un-ionised ammonia concentrations at the eight *Corallina* locations and seven *Sabellaria* locations, the maximum instantaneous value (10.4 µg/l) was below the EQS of 21 µg/l. For all scenarios, the area of exceedance of un-ionised ammonia, as a 95<sup>th</sup> percentile, had a maximum value of 0.2 ha at the surface and was not exceeded at the bed. For context the receiving water body (Bridgwater Bay) has a surface area of 9,224.5 ha, and therefore the area of exceedance would represent 0.002% of the water body.

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For construction and commissioning the maximum allowable concentration for total ammonia, (8 mg/l as a 95<sup>th</sup> percentile) was not exceeded at the surface or bed in any scenario, but the PNEC (1.1 mg/l as a mean) was exceeded at the surface only, however only for a maximum of 0.04 ha (equivalent to 1 grid cell in the model and the point of immediate discharge).

The overall conclusion was that all of the scenarios considered would not lead to significant environmental effects.

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## 1 Background

The Hinkley Point C (HPC) Development Consent Order (DCO) was granted by the UK Secretary of State for Energy and Climate Change in March 2013. The DCO and associated Licences and Permits detail NNB Gen Co's (HPC) environmental monitoring requirements with respect to the construction and operation of the new station.

HPC environmental permit (Environment Agency's Permit number EPR/XP3321GD/V004) for the Construction Sewage Treatment System consents NNB GenCo to discharge a maximum of 20 mg/l of ammoniacal nitrogen from the HPC Sewage Treatment plant during construction. Additionally, during commissioning, NNB GenCo are permitted to release 271 mg/l of ammoniacal nitrogen (EPR/JP3122GM/V009&010) and to discharge groundwater during the construction period. To support the delivery of HPC, NNB GenCo is considering varying the site's Construction Sewage Treatment System environmental permit (EPR/XP3321GD/V004) to allow an increased concentration of ammoniacal nitrogen within the permitted discharge. NNB GenCo has commissioned Cefas under the BEEMS programme to undertake appropriate additional modelling studies to support the discharge control strategy.

### 1.1 Scenarios

The currently permitted discharge of ammoniacal nitrogen from the sewage treatment works was assessed as 20 mg/l at a flow rate of 13.3 l/s, see Case D of BEEMS TR428. The flow from the sewage treatment works represents only a partial flow of the total contribution of ammoniacal nitrogen to the total 38.3 l/s flow of Case D. During the construction period the total flow of Case D is comprised of 13.3 l/s coming from the sewage treatment works and 25 l/s from general groundwater and tunnelling effluent flow.

To investigate the impact of varying the sewage treatment discharge, three different concentrations of ammoniacal nitrogen in the treated sewage flow were considered; 40, 60 and 80 mg/l. Additionally, an alternative flow rate mix has been considered, based on the current dewatering during construction, whereby the treated sewage flow rate is increased by 10 l/s and the groundwater decreased by 10 l/s, maintaining the overall 38.3 l/s flow. Table 1 summaries the different scenarios being tested and their respective ammonia concentrations.

As discussed further in Section 2.3 ammoniacal nitrogen will be discharged during commissioning as well as during the construction phase and while the commissioning discharge will not be varied the implications of altered construction discharges when combined with the commissioning discharges must be considered and are therefore factored into the assessment.

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Table 1: Summary of the discharge scenarios and their ammoniacal nitrogen concentrations.

Flow	Scenario (ammoniacal nitrogen in treated sewage)	Total flow (m <sup>3</sup> /s) <sup>1</sup>	Total ammonia (µg/l) <sup>2</sup>	Un-ionised ammonia (µg/l) <sup>3</sup>
Original	20 mg/l	0.038	10,034	44.8
	40 mg/l	0.038	16,979	75.7
	60 mg/l	0.038	23,924	106.7
	80 mg/l	0.038	30,869	137.7
Alternative	20 mg/l	0.038	14,020	62.5
	40 mg/l	0.038	26,187	116.8
	60 mg/l	0.038	38,355	171.1
	80 mg/l	0.038	50,522	225.3

<sup>1</sup>: Comprised of 25 l/s groundwater and tunnelling effluent plus 13.3 l/s treated sewage or the original case, or 15 l/s groundwater plus 23.3 l/s treated sewage for the alternative case.

<sup>2</sup>: Derived from the mixing of the sewage ammonia scenario plus groundwater at 4,732 µg/l total ammonia (refer to BEEMS Technical Report TR428).

<sup>3</sup>: Derived using the Environment Agency un-ionised ammonia calculator based on discharge with salinity of 1, pH of 7.3 and temperature of 12.5°C (refer to BEEMS Technical Report TR428).

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## 2 Assessment Methodology

### 2.1 Screening and un-ionised ammonia mixing

The first step in assessing the alternative treated sewage discharges was to apply the Environment Agency screening tests (Environment Agency and Department for Environment Food and Rural Affairs, 2022). The concentration of substances present in the discharge were assessed against lists of specific pollutants and priority hazardous substances and compared to environmental quality standards (EQS). There are several different 'tests' depending on the nature of the discharge and surrounding conditions. For the construction and commissioning discharges, and in line with previous assessments in BEEMS Technical Report TR428, test 1 and test 5 for 'estuaries and coastal waters' are applicable.

Test 1 is a comparison of the concentration of each assessment substance to the representative EQS. If concentrations of substances are below their EQS levels in the discharges the test is passed and the substance is screened out of further assessment.

Test 5 compares the discharge to calculated Effective Volume Flux (EVF) levels. The EVF is determined based on the discharge rate, the concentration of the substance and the EQS of that substance. The calculation applied is as follows:

$$\text{EVF} = (\text{Discharge Rate (m}^3\text{/s)} * \text{Concentration (}\mu\text{g/l)}) / (\text{EQS} - \text{background concentration})$$

The result is compared to the Allowable EVF (AEVF), which is determined by the water depth at the point of discharge. The water depth at the discharge point is at least 3 m. Consistent with previous assessments (BEEMS Technical Report TR428) an AEVF of 3 has been applied. Background concentrations applied are consistent with BEEMS Technical Report TR428 and follow either baseline measurements from the area (Amec, 2009) or concentrations recommended by the environment Agency.

Ammonia is a key consideration in treated sewage discharges and is considered as both total ammonia (ammoniacal nitrogen  $\text{NH}_3 + \text{NH}_4^+$ ) and un-ionised ammonia ( $\text{NH}_3$ ) alone. Un-ionised ammonia is a specific pollutant with a EQS (at 21  $\mu\text{g/l}$  annual average). All measures of ammonia are expressed 'as N' referring to the mass of nitrogen in the compound.

In general, the un-ionised form of ammonia is more toxic than the ionised form. The partitioning between ammonium ( $\text{NH}_4^+$ ) and un-ionised ammonia is controlled by environmental variables, principally, pH, temperature and salinity. At higher pH values, un-ionised ammonia represents a greater proportion of the total ammonia concentration. Temperature increase also raises the relative proportion of un-ionised ammonia, but this effect is much less marked than for pH change. A greater percentage of ammonia will also be in the un-ionised form when the salinity is lower. Un-ionised ammonia concentrations have been calculated using the Environment Agency calculator (following the formulas in Clegg & Whitfield, 1995).

The discharged source will be primarily freshwater with different properties to the seawater it will mix with. Therefore, the proportion of un-ionised ammonia will change as the discharge mixes with the surrounding seawater. Mixing curves have been calculated to determine the proportion of un-ionised ammonia at different levels of mixing. Interpolation of these curves at the EQS level provides to amount of mixing required to reach the EQS. Parameters used in the mixing calculations are given in Section 4.

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### 2.2 Construction only discharges

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The seven additional discharge scenarios described in Section 1.1 were assessed alone to consider the period of construction discharges before the commissioning discharges are added.

Initial screening was based on the characteristics of the discharge, with a salinity of 1, pH of 7.3 and background temperature of 12.5°C (BEEMS Technical Report TR428). While initial screening showed that construction only discharges are below the AEFV (see Section 3) the partitioning of ammonium and un-ionised ammonia varies significantly with pH. The ground water pH (7.3) is lower than the background seawater pH (7.86) so as the discharge mixes the proportion of un-ionised ammonia will increase (although notably while being diluted). Therefore, mixing calculations and nearfield modelling were applied to determine the range at which the EQS level would be reached. Whilst the total flow rate considered during the construction only scenario is 38.3 l/s, the flow rate modelled in CORMIX was conservatively increased to 45 l/s, mirroring what was previously modelled using CORMIX in BEEMS Technical Report TR428.

Mixing calculations are described in Section 4 and were used to determine the extent of mixing required to reach the EQS for un-ionised ammonia. Notably these calculations are independent of the volumes of the discharge. Initial mixing was therefore further investigated with the nearfield CORMIX model to determine the range at which the EQS would be met under the different scenarios. The construction discharge was modelled using CORMIX US EPA supported mixing zone model (CORMIX Version 12.0GT HYDRO1 Version 12.0.1.0 January 2023), using the same hydrodynamic model parameters as used in BEEMS Technical Report TR428 which has been previously agreed with the Environment Agency<sup>1</sup>.

To investigate how the discharge evolves over the state of the tide, multiple stages of the tide were considered: peak flood, peak ebb, high water, and low water. Whilst the plume is buoyant<sup>2</sup>, the water depth at the discharge is only 3 m at low water, there is a risk of slack water pooling at low water, where the depths and low velocities will inhibit mixing. Therefore, an additional scenario was also modelled in BEEMS Technical Report TR428 and replicated here, of low tide +1 hour.

### 2.3 Construction and commissioning discharges

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High levels of ammonia will be discharge during commissioning overlapping with the construction discharge. Previous modelling of ammonia discharges during construction and commissioning were presented in BEEMS Technical Report TR428. The release and mixing of ammonia was modelled using the validated Hinkley Point 25 m resolution GETM model. This is a 3D hydrodynamic model with an inbuilt passive tracer to represent ammonia. The model setup, calibration and validation are described in BEEMS Technical Report TR267 Edition 2. As with the 100 m resolution Hinkley Point GETM model (BEEMS Technical Report TR177) the surface is forced with reanalysed data from a meteorological model (ERA40 interim from ECMWF). The boundary conditions were forced by a broader 3D GETM domain, described in BEEMS Technical Report TR177.

The discharge outfall is attached to a jetty pile and located approximately 1 m above the seabed (approximately 2 m below lowest astronomical tide (LAT)). CORMIX modelling (shown in Appendix D of TR428) indicates that the plume will be buoyant and form a surface pool (or pond) at slack water which will become increasingly elongated as the tidal flow increases, forming a long thin streak at peak tidal flow.

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<sup>1</sup> Comments from the Environment Agency noted that CORMIX was run with a temperature of 12°C for both the discharge and the receiving environment, however this differs from the 12.5°C used in the calculation of unionised ammonia. Both represent mean background conditions and the difference is a function of rounding. Notably, as the mixing is driven by the density difference between the fresh and saline waters, the rounding error has no significant effect on the results. Re-running the CORMIX model using 12.5°C results in the distance before EQS is reached increasing by 3cm for results discussed in section 5.1..

<sup>2</sup> The plume is buoyant because it is a freshwater discharge into a saline environment. The discharge is not considered to be heated and has been modelled at ambient temperature (i.e. there is no thermal uplift).

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CORMIX is unable to replicate many of the features simulated by the GETM model, and GETM is therefore a better model to use away from the near field (further than 10s of metres from the outfall). Specifically, GETM can replicate wind driven behaviour and has precise bathymetry so that interactions with the tidal flow (e.g. eddies) are well replicated. Whilst CORMIX can include winds, they are applied omnidirectionally and are used for determining heat loss fluxes at the surface. As the discharges considered in this report are released at ambient sea temperature and are not considered to be heated, wind has not been included in the CORMIX model. Neither the CORMIX nor the GETM model includes the effects of waves which enhance vertical mixing and increase dilution. The modelling predictions of plume areas above the EQS are therefore conservative: the actual discharge will be subject to more mixing and dilution (caused by wave action) than the models are able to replicate and so the actual concentrations in the environment will be lower than those predicted.

As the scenarios considered here maintain the same total flow rate as previously modelled, no new GETM modelling was undertaken, but instead the results were scaled according to the change in the concentrations. BEEMS Technical Report TR428 considered two discharge scenarios during the construction + commissioning assessment: 38.3 l/s construction discharge at 10 mg/l ammoniacal nitrogen plus commissioning discharge at either 37 l/s or 70 l/s discharge at 271 mg/l ammoniacal nitrogen, depending on the release from one or two treatment tanks. For the assessment here, the worst case scenario of two treatment tanks has been assessed, due to the higher total ammonia content in the combined discharges. To determine the predicted effect of the treated sewage variation, the previous GETM results are scaled by determining the percentage increase in total mass of ammonia from the various waste streams. This percentage increase was then also applied to un-ionised ammonia results.

To assess the impact of varying the treated sewage discharge, the spatial extent of the total ammonia was assessed at the surface and bed against the (non-statutory) Predicted No Effect Concentration (PNEC) of 1.1 mg/l as a mean and the Maximum Allowable Concentration (MAC) of 8 mg/l as a 95<sup>th</sup> percentile. Likewise, for the un-ionised ammonia, the spatial extent was assessed against the (statutory) EQS of 21 µg/l at the surface and bed as a mean and 95<sup>th</sup> percentile.

In addition to the spatial extents, the exposure of un-ionised ammonia to sensitive biological receptors was also considered, specifically *Sabellaria* and *Corallina* (see Section 2.4 for more details on the biological receptors). Figure 1 shows a time series of un-ionised ammonia at the locations of *Corallina*<sup>3</sup> for the 38 l/s at 10 mg/l +70 l/s at 271 mg/l scenario, as shown in BEEMS Technical Report TR428. From the time series, the average concentration of un-ionised ammonia at the eight stations of *Corallina* is approximately 2 µg/l with periodic spikes in concentration. This is due to the discharge strategy during construction and commissioning. The construction discharge is a small continuous discharge, whereas the commissioning discharge is a pulsed discharge with a higher flow rate and concentration. The spikes in concentration, seen in Figure 1, at the locations of the *Corallina* previously assessed in BEEMS TR428 (see Figure 2) correspond to the time of the pulse discharge, whereas the 2 µg/l mean baseline is made up of both the construction discharge and the dispersion of the commissioning discharges. Therefore, when applying the percentage increase to the un-ionised ammonia, due to the variation in the treated sewage discharge, it was applied to the 2 µg/l mean baseline, rather than applied as a constant to the whole time series.

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<sup>3</sup> Note: location C4 was omitted in the original version of this figure however baseline for C4 is similar to other locations and results for C4 are shown on Figure 13. This omission does not influence the illustration of the 2µg/L baseline, which is the purpose of this figure.



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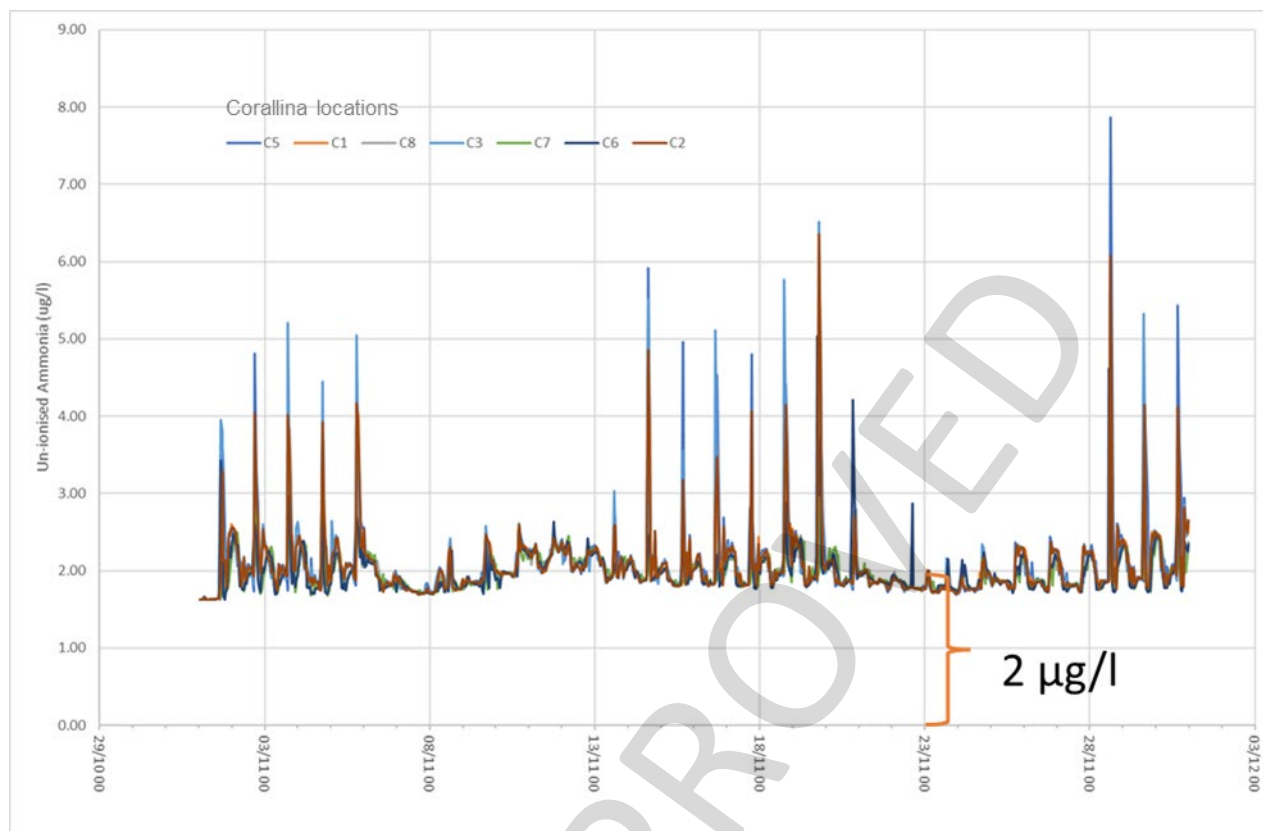


Figure 1: The original time series of un-ionised ammonia at the locations of Corallina (C1 to C8, see Figure 2) for the 38 l/s at 10 mg/l +70 l/s at 271 mg/l scenario, as shown in BEEMS Technical Report TR428.

**2.4 Biological receptors**

There are two biological receptors that the un-ionised ammonia was assessed against to determine the acceptable discharge concentration. These are; *Corallina* spp. and *Sabellaria* spp. This report has investigated the potential exposure of these species to un-ionised ammonia with respect to the EQS (21 µg/l annual average).

**2.4.1 Corallina spp.**

*Corallina* spp. or coral weed is a calcareous, branching red seaweed (Rhodophyta). Fronds can be up to 4 – 20 cm in length rising from a calcareous crustose holdfast. *Corallina* spp. is an intertidal species typically found inhabiting littoral wave-exposed rocky shores and shallow sublittoral habitats forming turfs in pools and gullies, sometimes extending into the sublittoral fringe (Tyler-Walters, 2008). Dense, sometimes monospecific, swards of *Corallina* are a characteristic feature of the mid to low shore rocky ledges to the west of Hinkley Point (Bamber & Irving, 1992). It is found all around the UK extending its range north to Norway and Greenland and south to Morocco and Argentina (Tyler-Walters, 2008). *Corallina* spp. are of national importance although official conservation status is uncertain (BEEMS Technical Report TR029).

An unusual geological formation at Hinkley Point has caused conditions which favour the development of lush red algal turfs composed mainly of *Corallina* spp. The topography is such that a series of scarps and slopes run parallel to the shore and retain water as the tide retreats, creating a series of narrow pools or streams along the shore. In places where the scarps are breached, water can spill down to the lower shore, thus creating a permanently wet environment suitable for growth of algal species which would otherwise exist only fully submerged in rock pools (BEEMS Technical Report TR029).

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Until recently two species of *Corallina* were recognised for the British flora: *Corallina elongata* and *Corallina officinalis* (Irvine and Johansen, 1994). The *Corallina* species found at Hinkley Point has provisionally been described as '*officinalis*', but the taxonomy of the Corallinales has recently been revised (Walker *et al.*, 2009) and a new species *Corallina caespitosa* sp. nov. has been added. Hence, there are three possible species which may exist at Hinkley Point (BEEMS Technical Report TR068B).

Figure 2 shows the location of *Corallina* spp. habitat in relation to the Hinkley Point site. There are eight patches of *Corallina* spp. indicated on the map, as defined in BEEMS Technical Report TR428. Concentrations of un-ionised ammonia were assessed at these locations. As the *Corallina* is intertidal the un-ionised ammonia concentrations at the eight stations will be assessed using the surface concentrations, as in BEEMS Technical Report TR428.

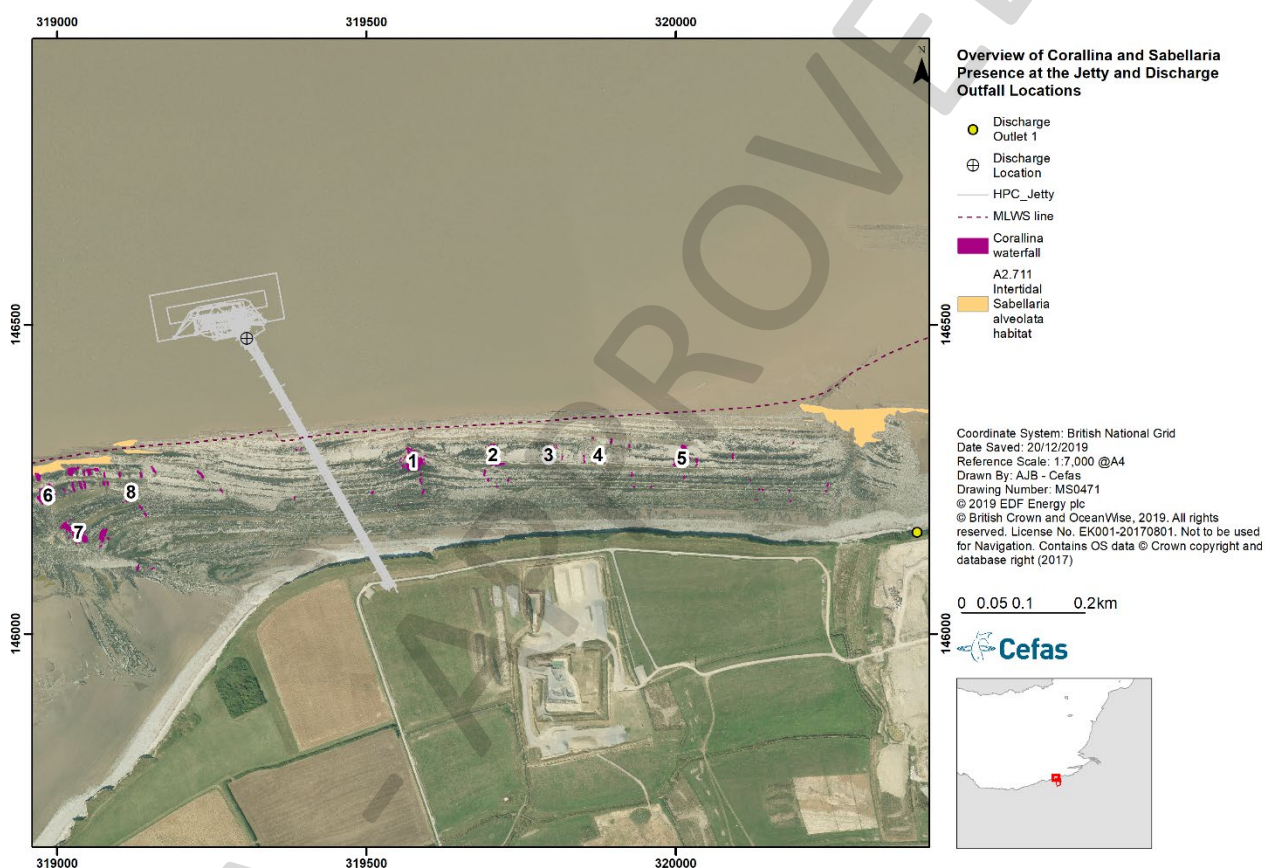


Figure 2: Location of the intertidal *Corallina* spp. around Hinkley Point.

### 2.4.2 Sabellaria spp.

As part of the Severn Estuary Special Area of Conservation (SAC), *Sabellaria* spp. reefs are a key ecological feature of the site and are included, as biogenic reef habitat, under the SAC designation. The two species of *Sabellaria* spp. that are of interest are *Sabellaria spinulosa* and *Sabellaria alveolata*. As well as a qualifying interest feature of the Severn Estuary SAC, both *S. alveolata* and *S. spinulosa* also have their own UK Biodiversity Action Plans and reef structures are listed under Annex I of the EC Habitats Directive (see BEEMS Technical Report TR068 Version 2).

Both species are sabellariid polychaetes which form reef structures through the aggregation of growth tubes. *S. spinulosa* is a predominantly subtidal species that is relatively widespread around the UK and is found either individually or as crusts or reefs; settling directly on the seabed, on tubes of the same species or on

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hard body parts of other benthic species (such as large bivalves). *S. alveolata* is a predominantly intertidal species that is found mainly around the west and south-west of the UK, settling on exposed bedrock and hard substrates from boulders to pebbles (BEEMS Technical Report TR039). *Sabellaria* reefs are common around Hinkley Point and elsewhere in the Severn Estuary and Bristol Channel but is unusual in that *S. alveolata* occurs in the subtidal, as well as the intertidal which is not commonly observed in other areas.

Figure 3 shows the location of *S. alveolata* habitat in relation to the Hinkley Point site. There are seven patches of *S. alveolata* indicated on the map, as defined in BEEMS Technical Report TR428. Concentrations of un-ionised ammonia will be assessed at these locations. For stations A and E, the *Sabellaria* is subtidal. For stations B, C, D, F and G, the *Sabellaria* is intertidal. As such, for the subtidal *Sabellaria* the un-ionised ammonia concentrations haven't been assessed against the EQS using the seabed concentrations, whereas the intertidal have been assessed using the surface concentrations. This is as done in BEEMS Technical Report TR428.

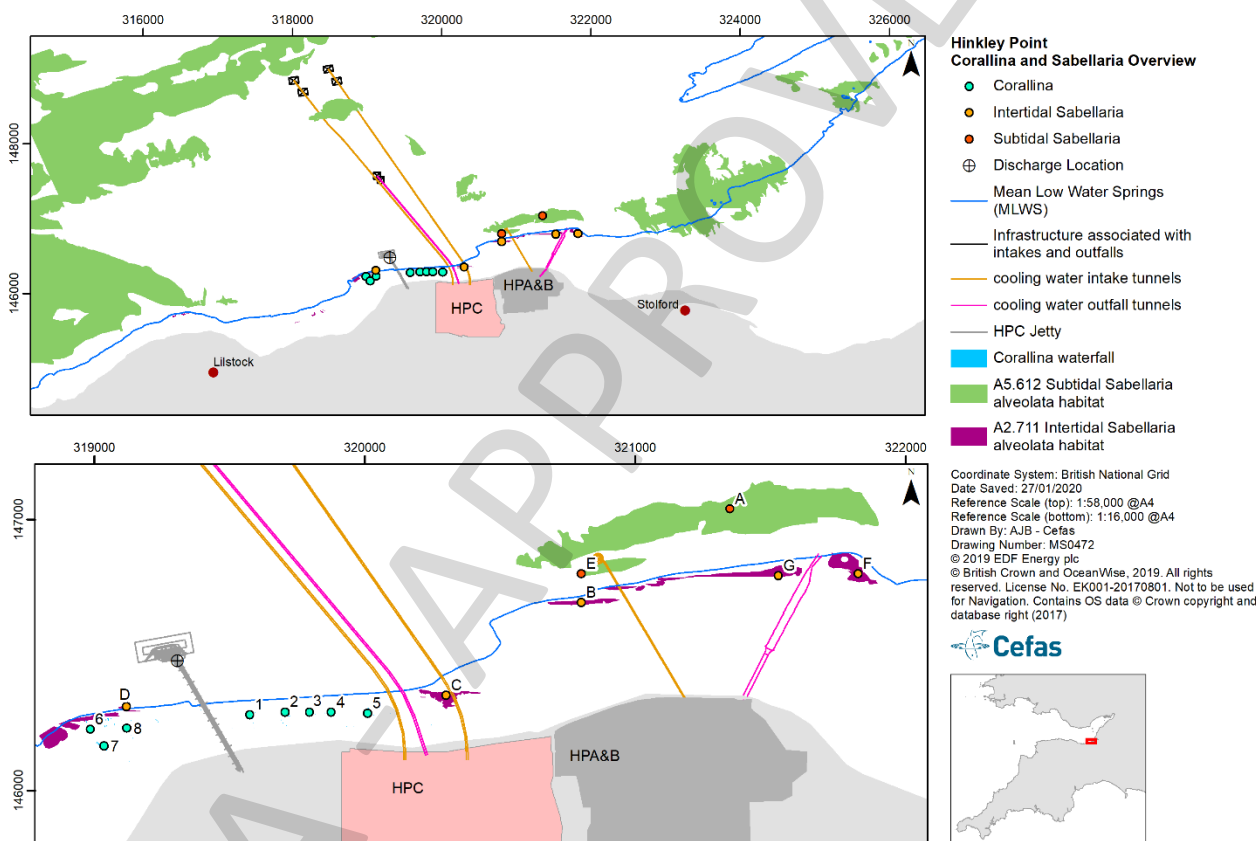


Figure 3: Location of subtidal and intertidal *Sabellaria alveolata* around Hinkley Point.

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## 3 Screening Results

Screening of the seven possible discharge scenarios considering the construction discharge alone showed that all, including the current permitted 20 mg/l ammonia scenario failed test 1 (i.e. are above EQS at the point of discharge). Comparison against the AEVF (test 5) showed that all scenarios were below the threshold. The results of test 5 suggest that when considering construction alone each scenario tested is within permissible limits. The results of the screening tests are shown in Table 2.

As described in Section 2.2, the partitioning of un-ionised ammonia is influenced by the physical conditions and this partitioning is not factored into the basic screening tests. Therefore, while the screening test was passed, further assessment of the discharges in terms of mixing calculations and nearfield modelling is provided in Section 4 and Section 5.1.

Screening of the construction plus commissioning discharges is shown in Table 3. An additional 271,206 µg/l of ammoniacal nitrogen from commissioning was added to construction discharges for these scenarios with the discharge concentration calculated based on a commissioning discharge rate of 70 l/s (refer BEEMS Technical Report TR428, Appendix C for detail of commissioning discharges). Due to the considerable increase in ammonia from the commissioning phase, the screening tests were not passed, however this is consistent with previous assessments (BEEMS Technical Report TR428) which required modelling to fully assess the potential implications of the commissioning discharges. Detailed assessment of the alternative scenarios including the commissioning phase discharges is provided in Section 5.

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Table 2: Screening tests for construction phase alternative treated sewage discharge scenarios.

Scenario (ammoniacal nitrogen in treated sewage)	Flow m <sup>3</sup> /s	Total ammonia µg/l	Un-ionised ammonia µg/l	Saltwater AA EQS µg/l	Background concentration µg/l	Test 1	Test 5 Effective volume flux	TraC Water test 5 EVF < 3.0 (Pass/Fail)
BASELINE (20 mg/l)	0.038	10,034	44.8	21	4.6	2.1	0.1	Pass
40 mg/l	0.038	16,979	75.7	21	4.6	3.6	0.2	Pass
60 mg/l	0.038	23,924	106.7	21	4.6	5.1	0.2	Pass
80 mg/l	0.038	30,869	137.7	21	4.6	6.6	0.3	Pass
BASELINE (20 mg/l) - alt. flow	0.038	14,020	62.5	21	4.6	3.0	0.1	Pass
40 mg/l - alt. flow	0.038	26,187	116.8	21	4.6	5.6	0.3	Pass
60 mg/l - alt. flow	0.038	38,355	171.1	21	4.6	8.1	0.4	Pass
80 mg/l . alt flow	0.038	50,522	225.3	21	4.6	10.7	0.5	Pass

Notes: Un-ionised ammonia calculated based on discharge with salinity of 1, pH of 7.3 and temperature of 12.5°C.

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Table 3: Screening tests for construction and commissioning phase alternative sewage discharge scenarios.

Scenario (ammoniacal nitrogen in treated sewage)	Flow m <sup>3</sup> /s	Total ammonia µg/l	Un-ionised ammonia µg/l	Saltwater AA EQS µg/l	Background concentration µg/l	Test 1	Test 5 Effective volume flux	TraC Water test 5 EVF < 3.0 (Pass/Fail)
BASELINE (20 mg/l) + commissioning	0.108	178,878	32,799	21.00	4.60	1,562	216.6	Fail
40 mg/l + commissioning	0.108	181,334	33,249	21.00	4.60	1,583	219.6	Fail
60 mg/l + commissioning	0.108	183,790	33,700	21.00	4.60	1,605	222.5	Fail
80 mg/l + commissioning	0.108	186,247	34,150	21.00	4.60	1,626	225.5	Fail
BASELINE (20 mg/l) - alt. flow + commissioning	0.108	180,288	33,058	21.00	4.60	1,574	218.3	Fail
40 mg/l - alt flow + commissioning	0.108	184,591	33,847	21.00	4.60	1,612	223.5	Fail
60 mg/l - alt. flow + commissioning	0.108	188,894	34,636	21.00	4.60	1,649	228.7	Fail
80 mg/l alt. flow + commissioning	0.108	193,196	35,425	21.00	4.60	1,687	233.9	Fail

Notes: Un-ionised ammonia calculated based on discharge with salinity of 1, pH of 9 (pH 9 represents the expected pH of the commissioning wastewater as per permit EPR/JP3122GM/V009&010) and temperature of 12.5°C. Commissioning flow of 70 l/s added with a concentration of ammoniacal nitrogen of 271,260 µg/l (see Section 1.1 for volume and concentration calculations).

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### 4 Un-ionised Ammonia Mixing Calculations

The mixing of the construction discharges with seawater influences the partitioning of un-ionised ammonia as described in Section 2. Mixing of the discharge was calculated based on the progressive dilution from the source concentration of ammoniacal nitrogen with the discharge characteristics of pH 7.3 and salinity of 1, through to complete mixing down to background ammoniacal nitrogen levels and average ambient seawater conditions (salinity of 31.5 and pH of 7.86). The components of the mixing calculations are consistent with the previous assessment in BEEMS Technical Report TR428. Mixing curves are shown in Figure 4 and Figure 5 and the level of mixing and dilution required to reach the EQS for un-ionised ammonia is summarised in Table 4. These calculations are independent of the volume of the discharge and therefore must be considered in combination with modelling dilution rates from CORMIX modelling (Section 5.1).

Table 4: Nearfield mixing of un-ionised ammonia under the construction phase alternative scenarios.

Scenario (ammoniacal nitrogen in treated sewage)	Un-ionised ammonia ( $\mu\text{g/l}$ )	Mixing % required to EQS ( $21 \mu\text{g/l}$ )	Dilution factor required to EQS ( $21 \mu\text{g/l}$ )
BASELINE (20 mg/l)	44.8	81	4.4
40 mg/l	75.7	90	9.1
60 mg/l	106.7	93	13.3
80 mg/l	137.7	95	17.6
BASELINE (20 mg/l) - alt. flow	62.5	86	7.0
40 mg/l – alt. flow	116.8	94	14.7
60 mg/l - alt. flow	171.1	96	22.1
80 mg/l – alt. flow	225.3	97	29.5

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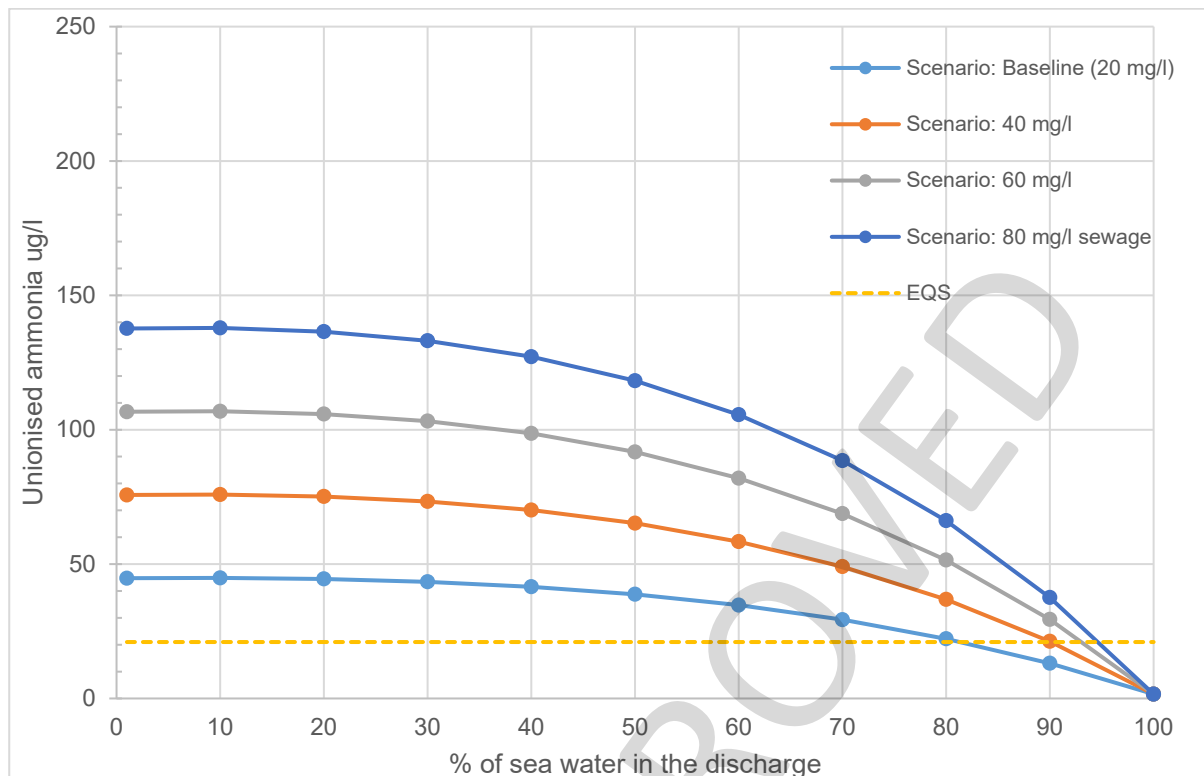


Figure 4: Mixing of the construction discharge and un-ionised ammonia partitioning with baseline flows (treated sewage at 13.3 l/s and groundwater at 25 l/s).

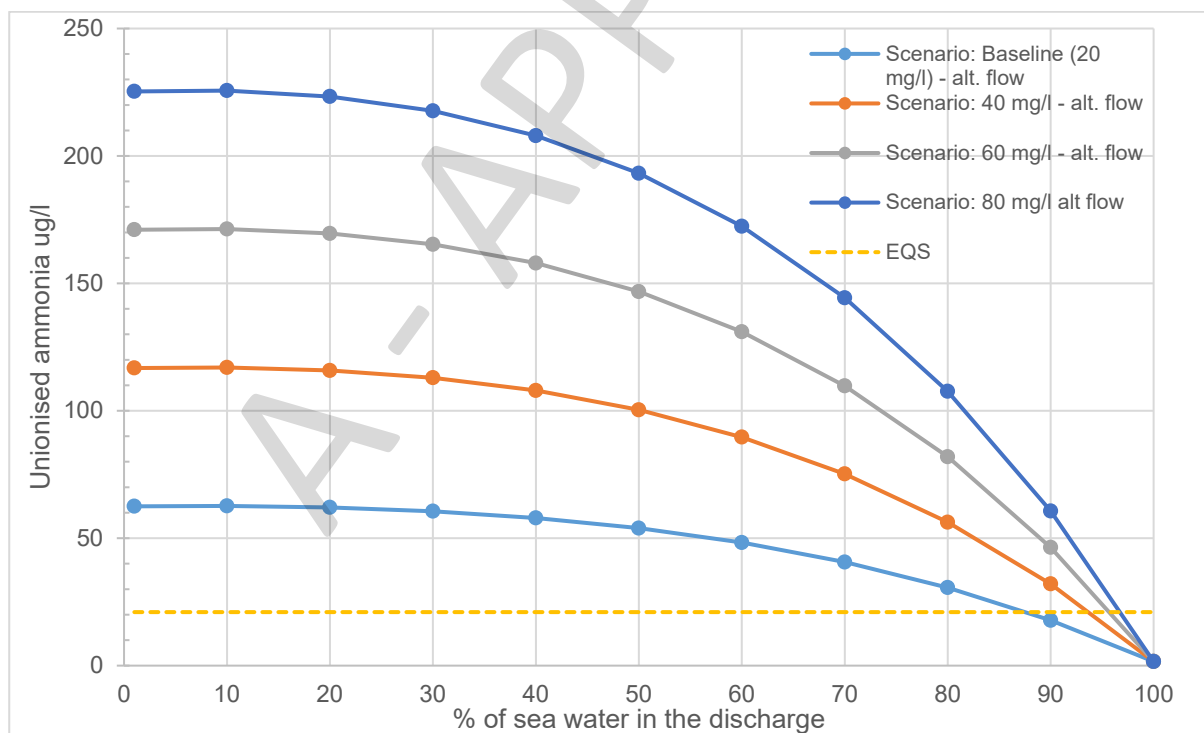


Figure 5: Mixing of the construction discharge and un-ionised ammonia partitioning with alternative flows (treated sewage at 23.3 l/s and groundwater at 15 l/s).

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### 5 Modelling Results

#### 5.1 CORMIX

Figure 6 and Figure 7 show the shape of the plume, from the CORMIX results with a 45 l/s discharge, for the rising tide and low water, respectively. As was seen in BEEMS Technical Report TR428, due to the strong tidal currents, the resulting plume from the construction discharge forms a long elongated shore parallel shape. At low water, this elongated plume expands and pools at slack water. Due to the freshwater nature of the plume, the plume remains buoyant and rises to the surface at all states of the tide. Figure 8 to Figure 12 show the dilution curves for the five states of the tide investigated for the 45 l/s discharge. From these curves, the distance the plume extends before mixing to the required level of dilution can be determined, as summarised in Table 4, in order to fall below the EQS.

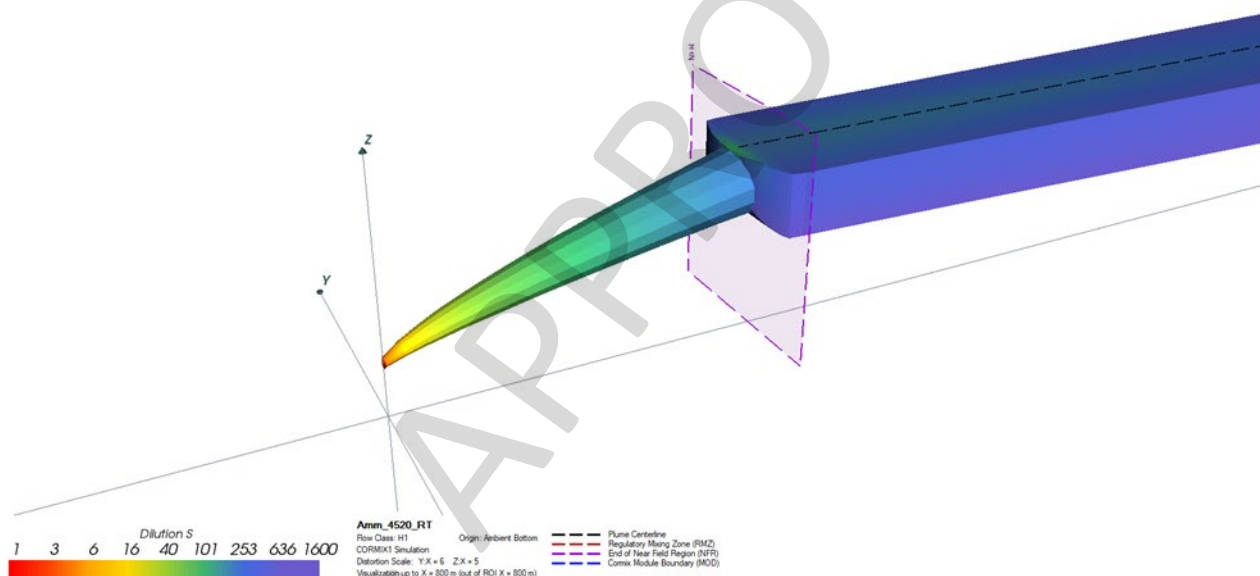


Figure 6: CORMIX output at rising mid tide, showing the long elongated plume due to peak tidal currents.

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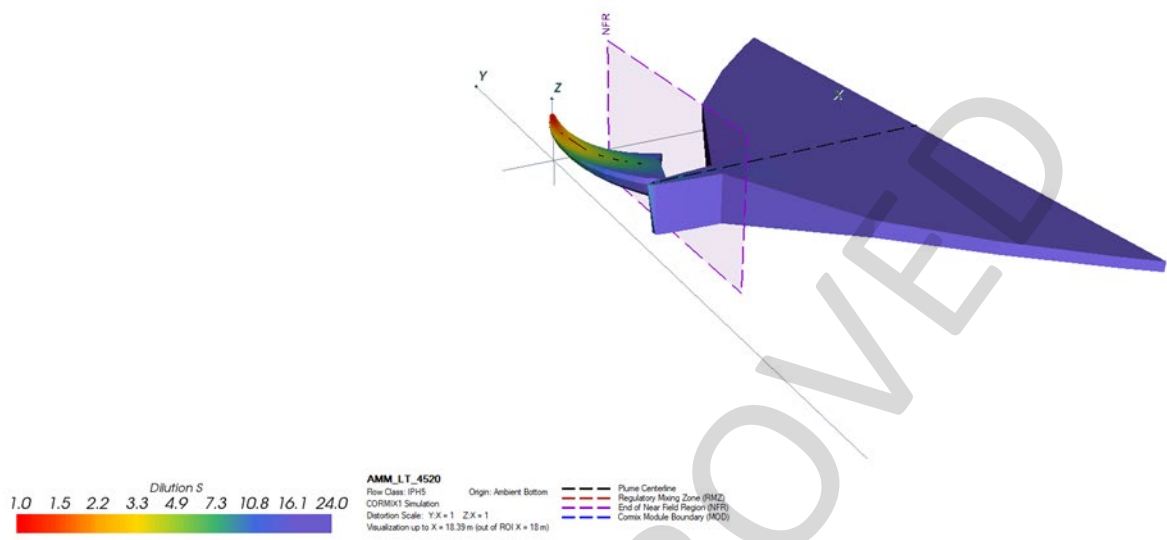


Figure 7: CORMIX output at low tide, showing the buoyant slack water plume.

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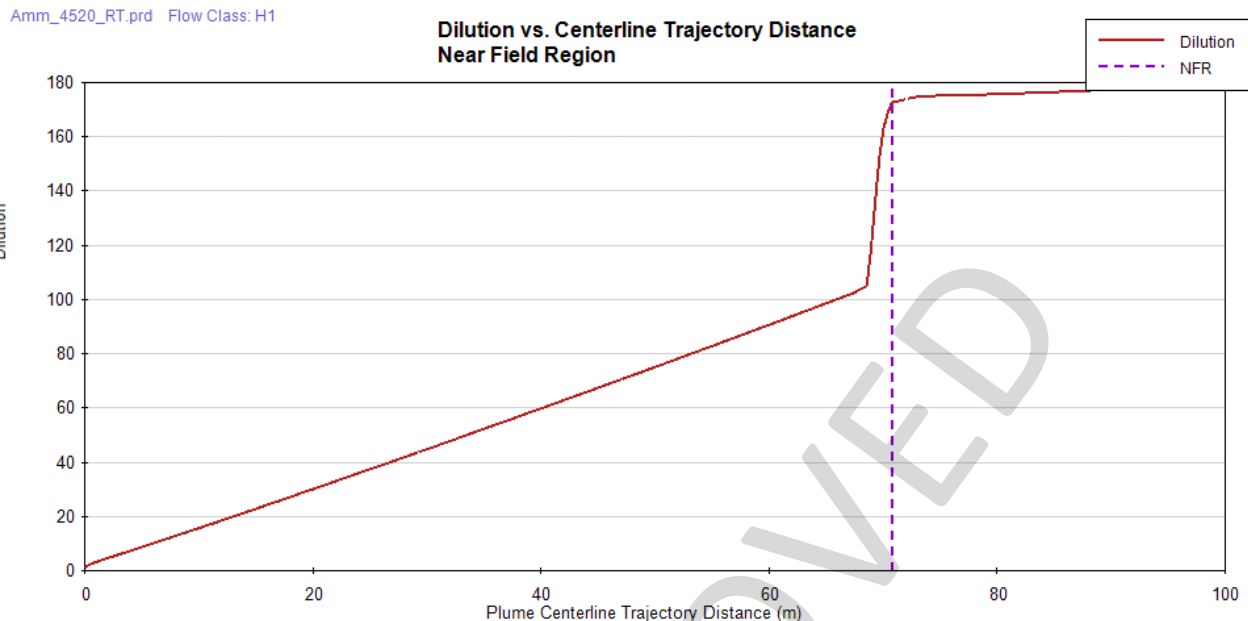


Figure 8: CORMIX outputs showing the dilution of the plume along the centreline for the 45 l/s simulation at rising mid tide.

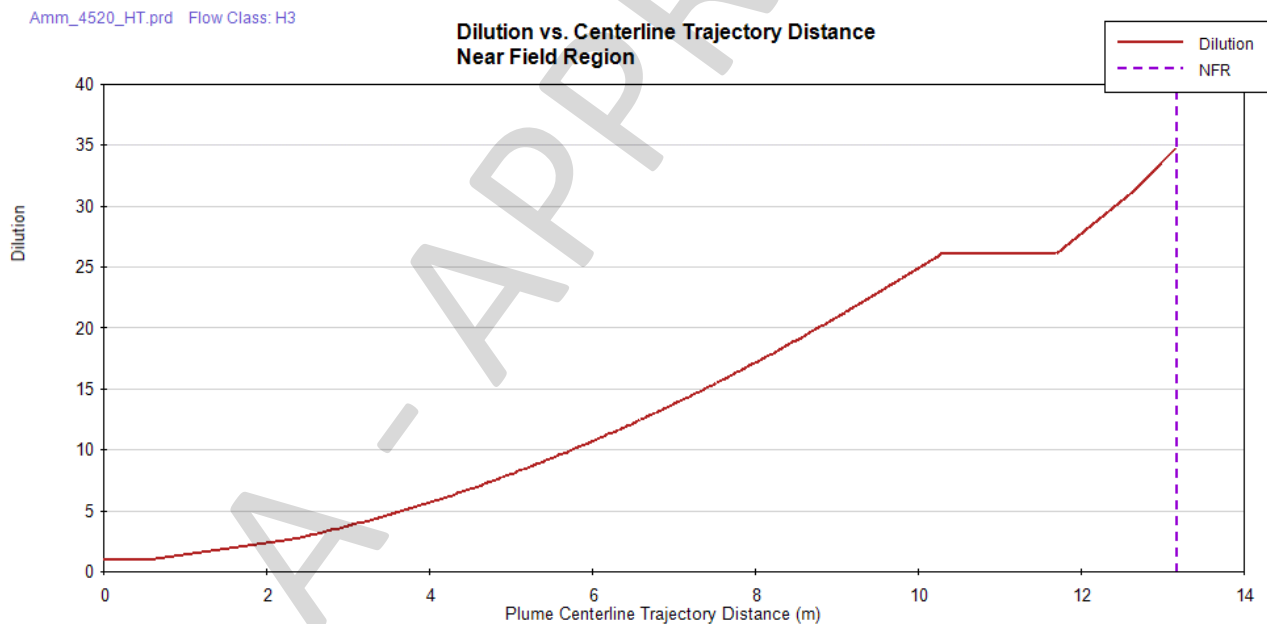


Figure 9: CORMIX outputs showing the dilution of the plume along the centreline for the 45 l/s simulation at high tide.

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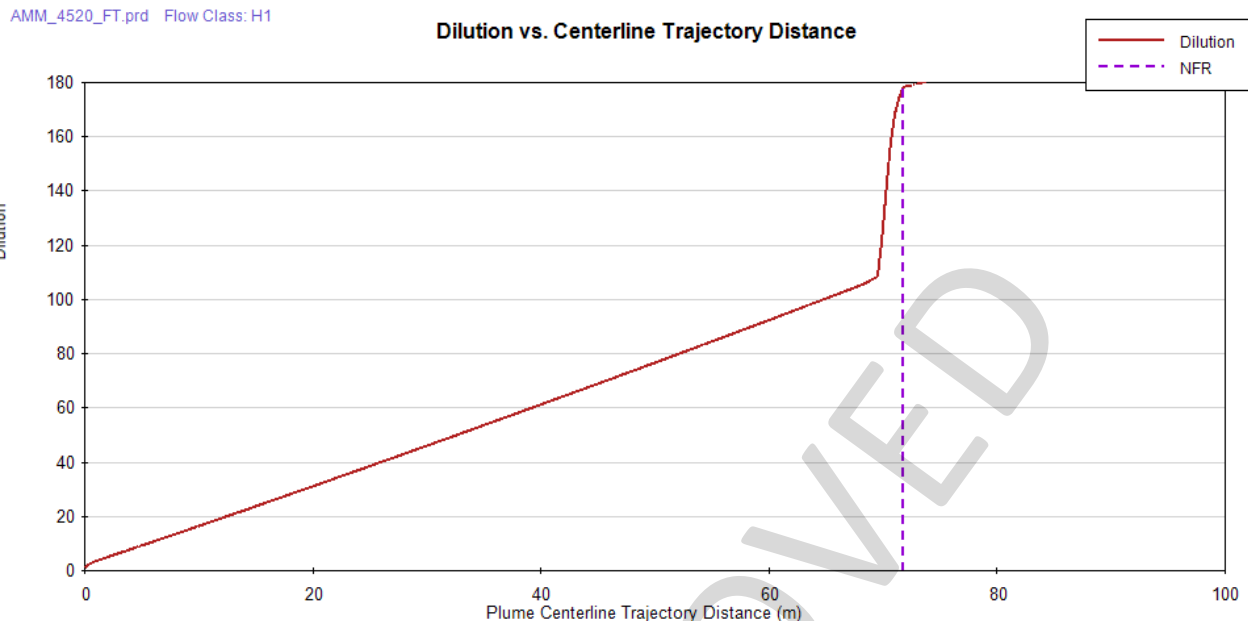


Figure 10: CORMIX outputs showing the dilution of the plume along the centreline for the 45 l/s simulation at falling mid tide.

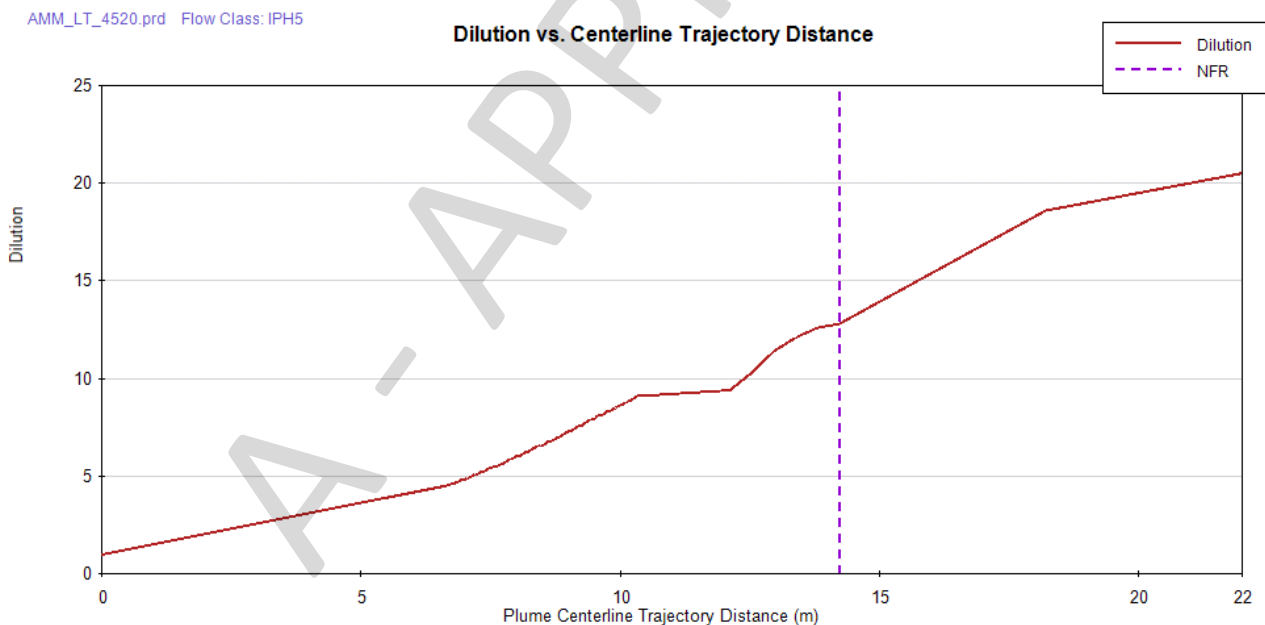


Figure 11: CORMIX outputs showing the dilution of the plume along the centreline for the 45 l/s simulation at low tide.

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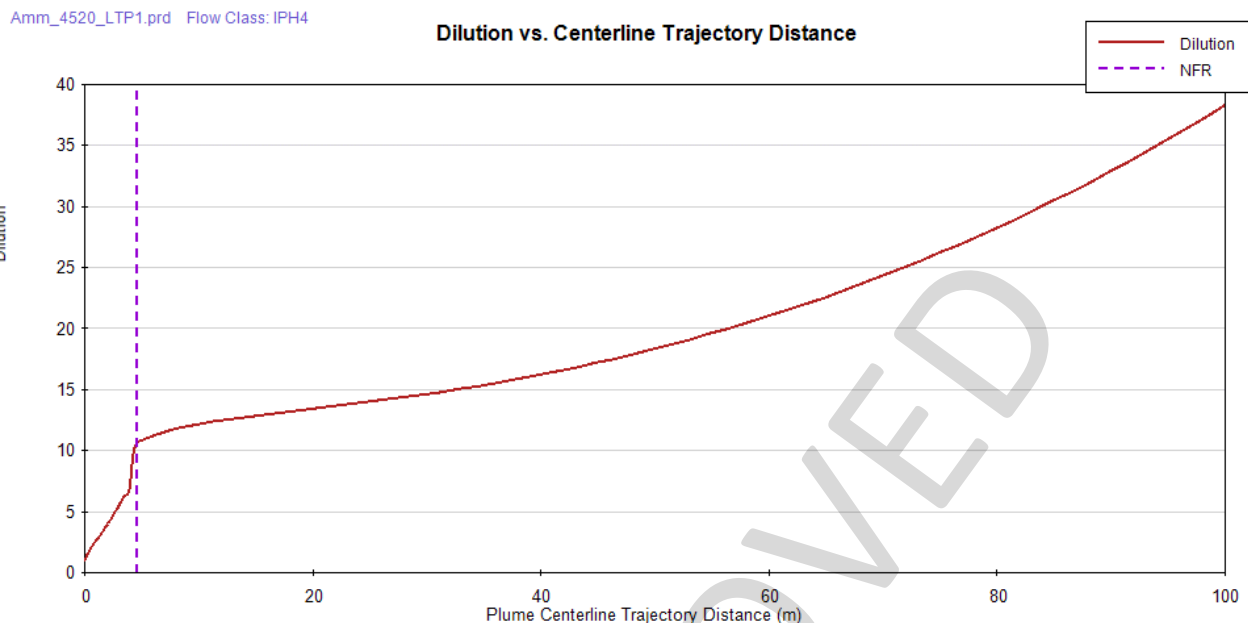


Figure 12: CORMIX outputs showing the dilution of the plume along the centreline for the 45 l/s simulation at low tide +1 hour.

Using the mixing calculations and required dilution to reach the EQS, summarised in Table 4, the CORMIX modelling shows the concentrations of un-ionised ammonia fell below the EQS (21 µg/l) within <7.16 m for the original scenario (i.e. 20 mg/l total ammonia). This distance to the EQS increased to a maximum of 46.04 m for the 80 mg/l discharge scenario, with the original flows, and to 82.08 m for 80 mg/l discharge with the alternative flow rates. The results are summarised in Table 5.

Initial screening of the construction only discharge scenarios shows that while discharges failed test 1 (they are above the EQS), they passed test 5 (the effective volume flux is below 3). This suggests that the construction only discharge should be acceptable at the higher concentrations tested. While the estimated mixing zone is considerably larger under the new scenarios compared to the baseline scenario (increasing from ~7m to over 80m), the mixing zone was still very small in respect to the scale of the receiving environment and therefore is not expected to cause any significant impacts.

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Table 5: Summary of CORMIX results showing the distances whereby the discharge of un-ionised ammonia falls below the EQS.

Ammonia Scenario	EQS (µg/l)	Required mixing %	Dilution	Distance to required mixing (m)				
				Rising tide	High tide	Falling tide	Low tide	Low tide +1 hr
Baseline flows – 45 l/s (treated sewage 13 l/s)								
20 mg/l	21	81.3	4.36	2.75	4.58	2.57	7.16	3.52
40 mg/l	21	90.1	9.13	5.80	6.47	5.33	11.74	4.96
60 mg/l	21	93.0	13.34	8.66	7.76	8.21	12.68	18.77
80 mg/l	21	94.6	17.55	11.63	8.88	11.01	14.16	46.04
Alternate flows – 45 l/s (treated sewage 23 l/s)								
20 mg/l	21	87.5	7.00	4.35	5.73	4.02	8.99	4.8
40 mg/l	21	93.6	14.72	9.61	8.14	9.11	13.17	30.12
60 mg/l	21	95.7	22.09	14.71	9.97	14.13	20.78	62.82
80 mg/l	21	96.7	29.47	19.77	12.44	19.05	21.68	82.08
				Limiting distance (l <sub>max</sub> ) due to TIDAL REVERSAL has been reached <sup>1</sup> .				

<sup>1</sup> l<sub>max</sub> is the maximum distance CORMIX can determine in one direction before the direction of the tidal currents reverses due to the state of the tide and the plume travels back on itself.

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### 5.2 GETM reanalysis

#### 5.2.1 Un-ionised ammonia

High levels of ammonia will be discharge during commissioning overlapping with the construction discharge (38 l/s at 10 mg/l + 70 l/s at 271 mg/l). These discharges have been modelled based on the original flows and concentrations in BEEMS Technical Report TR428. This modelling was then extrapolated to determine the mixing zones for un-ionised ammonia (and total ammonia) by determining the additional total mass as a percentage of the original flows. Table 6 and Table 7 summarise the total mass of each source of ammonia and their contribution to the total mass of ammonia, for the baseline flows and the alternative flows (treated sewage is increased by 10 l/s and groundwater decreased by 10 l/s). From the additional percentage increases for the different flow scenarios, the additional un-ionised ammonia concentration at the location of the *Corallina* and *Sabellaria*, has been calculated and is summarised in Table 8.

During the period where the construction and commissioning discharges overlap, the discharge scenarios led to an estimated additional 0.11 to 0.31 µg/l of un-ionised ammonia with the original flow rates and 0.06 to 0.61 µg/l of un-ionised ammonia with the alternative flow rates at the locations of the sensitive biological receptors (*Sabellaria* and *Corallina*). These values are based on the original un-ionised ammonia time series, shown in BEEMS Technical Report TR428<sup>4</sup>, and apply the additional percentage increase based on the total ammonia which, under the original (baseline) scenario, had an average exposure of 2 µg/l over the length of the combined construction and commissioning discharges.

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<sup>4</sup> The calculation of un-ionised ammonia from total ammonia used the conditions of the receiving ambient seawater with a salinity of 31.5, pH of 7.86 and temperature of 12.5°C (refer to BEEMS Technical Report TR428)

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Table 6: Summary of the contributions to the total mass of ammonia from the different sources, for the different treated sewage scenarios using the baseline flows.

Scenario	Source	Flow	Concentration	Duration	Mass
		(l/s)	(mg/l)	(hrs)	(kg/day)
Baseline - 20 mg/l	Treated sewage	13.3	20	24	22.982
	Groundwater	25	4.732	24	10.221
	Commissioning	70	271	5.95	406.34
	<b>Total mass</b>				<b>439.54</b>
Baseline - 40 mg/l	Treated sewage	13.3	40	24	45.965
	Groundwater	25	4.732	24	10.221
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>462.52 (4.97%)</b>
Baseline - 60 mg/l	Treated sewage	13.3	60	24	68.947
	Groundwater	25	4.732	24	10.221
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>485.51 (9.47%)</b>
Baseline - 80 mg/l	Treated sewage	13.3	80	24	91.930
	Groundwater	25	4.732	24	10.221
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>508.49 (13.56%)</b>

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Table 7: Summary of the contributions to the total mass of ammonia from the different sources, for the different sewage scenarios using the alternative flows.

Scenario	Source	Flow	Concentration	Duration	Mass
		(l/s)	(mg/l)	(hrs)	(kg/day)
Alternative - 20 mg/l	Treated sewage	23.3	20	24	40.262
	Groundwater	15	4.732	24	6.133
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>452.73 (2.91%)</b>
Alternative - 40 mg/l	Treated sewage	23.3	40	24	80.525
	Groundwater	15	4.732	24	6.133
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>492.99 (10.84%)</b>
Alternative - 60 mg/l	Treated sewage	23.3	60	24	120.787
	Groundwater	15	4.732	24	6.133
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>533.26 (17.57%)</b>
Alternative - 80 mg/l	Treated sewage	23.3	80	24	161.050
	Groundwater	15	4.732	24	6.133
	Commissioning	70	271	5.95	406.34
	<b>Total mass (percentage increase)</b>				<b>573.52 (23.36%)</b>

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Table 8: Summary of the additional un-ionised ammonia concentration at the location of the *Corallina* and *Sabellaria*, with the baseline construction and commissioning discharges.

Flow	Source	Un-ionised ammonia	Difference from baseline	Un-ionised ammonia	Difference from baseline	Un-ionised ammonia	Difference from baseline	Un-ionised ammonia	Difference from baseline
		(ug/l)	(ug/l)	(ug/l)	(ug/l)	(ug/l)	(ug/l)	(ug/l)	(ug/l)
		20 mg/l		40 mg/l		60 mg/l		80 mg/l	
Baseline	Treated sewage	0.105	0.000	0.209	0.105	0.314	0.209	0.418	0.314
	Groundwater	0.047	0.000	0.047	0.000	0.047	0.000	0.047	0.000
	Commissioning	1.849	0.000	1.849	0.000	1.849	0.000	1.849	0.000
	Total	2.000	0.000	2.105	0.105	2.209	0.209	2.314	0.314
Alternative	Treated sewage	0.183	0.079	0.366	0.262	0.550	0.445	0.733	0.628
	Groundwater	0.028	-0.019	0.028	-0.019	0.028	-0.019	0.028	-0.019
	Commissioning	1.849	0.000	1.849	0.000	1.849	0.000	1.849	0.000
	Total	2.060	0.060	2.243	0.243	2.426	0.426	2.610	0.610

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To assess the exposure of un-ionised ammonia at the locations of the *Corallina* and *Sabellaria*, the additional un-ionised ammonia, summarised in Table 8, have been added to the instantaneous time series of un-ionised ammonia concentrations at the eight *Corallina* locations (Figure 13) and seven *Sabellaria* locations (Figure 14). Figure 14 shows that for the 80 mg/l scenario with the alternative flow rates, the maximum instantaneous value (10.4 µg/l) was below the EQS of 21 µg/l. Plots of the individual time series for each *Corallina* and *Sabellaria* stations are shown in Appendix A. The mean and 95<sup>th</sup> percentile concentrations of un-ionised ammonia at the *Corallina* and *Sabellaria* features for the 20, 40, 60 and 80 mg/l scenarios with the baseline and alternative flows are summarised in Table 9 to Table 12.

Figure 15 show the spatial plots of the surface 95<sup>th</sup> percentile un-ionised ammonia for the construction and commissioning discharges for the 80 mg/l scenario with alternative flows. Table 13 summarises the area of exceedance above the EQS for un-ionised ammonia for all scenarios.

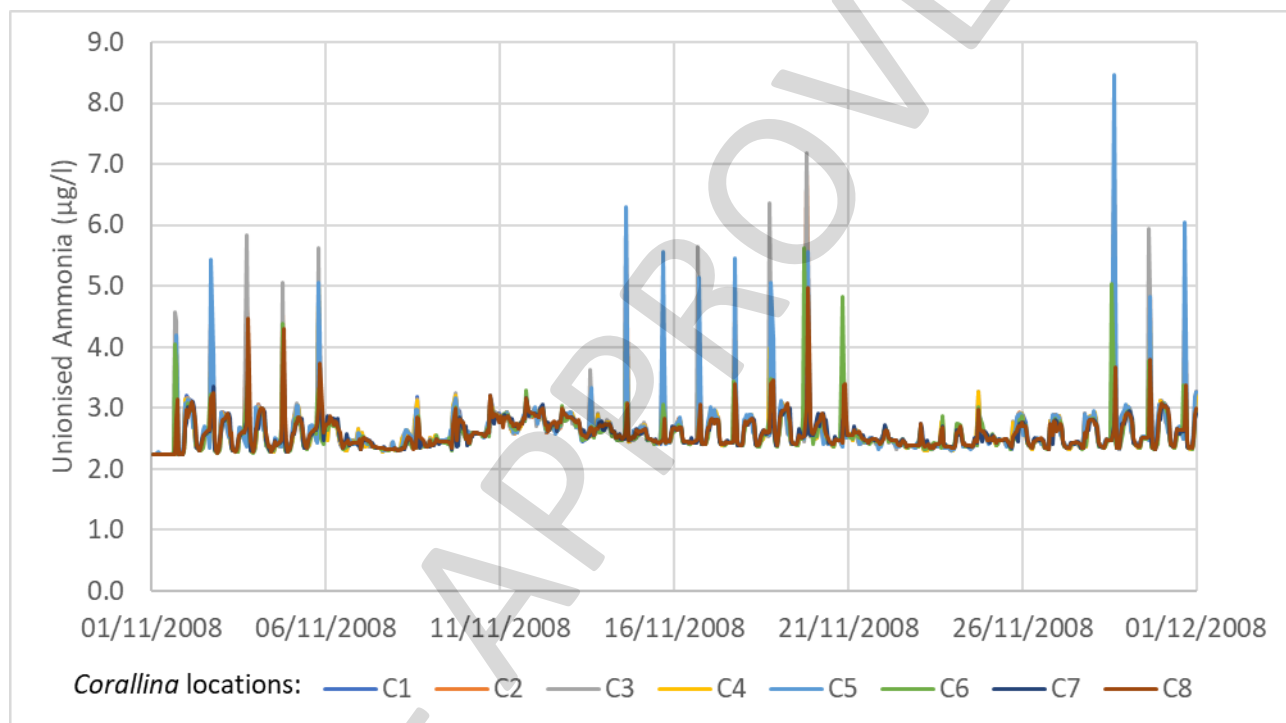


Figure 13: Time series of un-ionised ammonia at the locations of Corallina for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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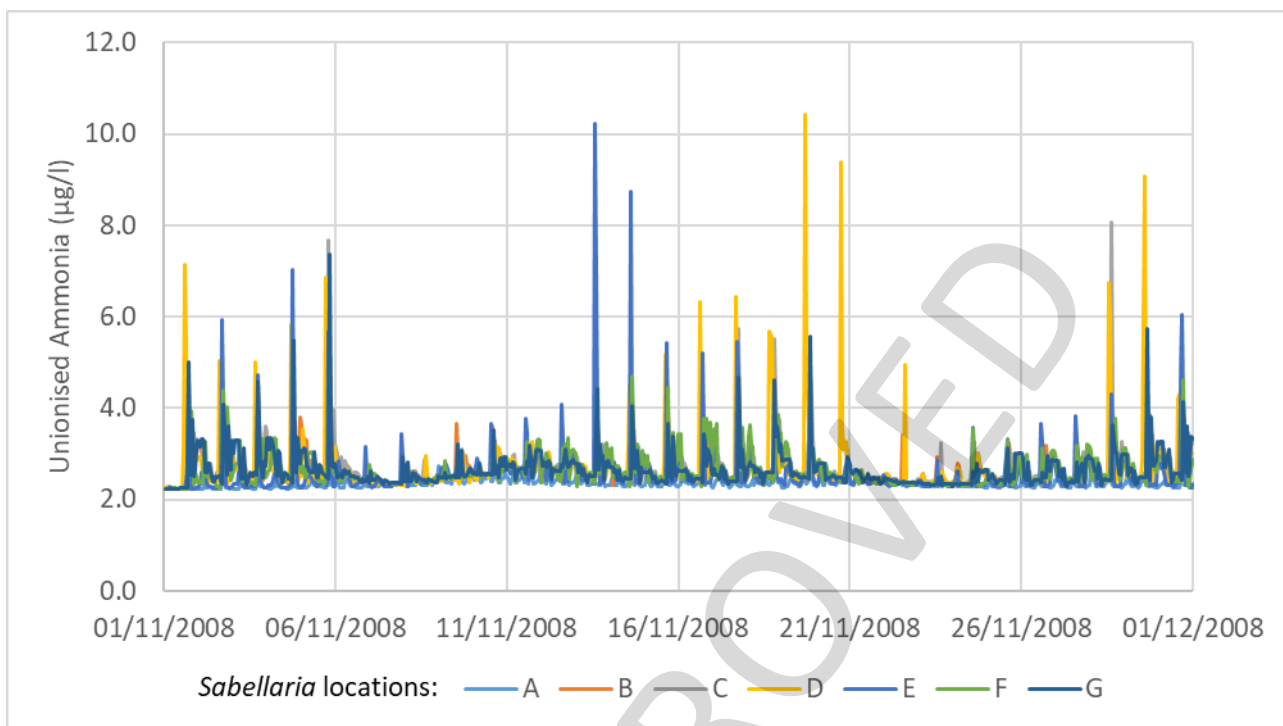


Figure 14: Time series of un-ionised ammonia at the locations of Sabellaria for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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Table 9: Summary of un-ionised ammonia ( $\mu\text{g/l}$ ) at *Sabellaria* features (A – G) for mean temperatures, with the baseline flows.

Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile
A	1.74	1.90	1.84	2.01	1.95	2.11	2.05	2.22
B	2.01	2.60	2.11	2.71	2.22	2.81	2.32	2.91
C	2.08	2.68	2.19	2.79	2.29	2.89	2.40	3.00
D	2.07	2.56	2.18	2.67	2.28	2.77	2.38	2.88
E	1.95	2.54	2.06	2.65	2.16	2.75	2.27	2.86
F	2.03	2.72	2.13	2.82	2.24	2.93	2.34	3.03
G	2.05	2.71	2.15	2.82	2.26	2.92	2.36	3.03

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Table 10: Summary of un-ionised ammonia ( $\mu\text{g/l}$ ) at *Sabellaria* features (A – G) for mean temperatures, with the alternative flows.

Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile
A	1.80	1.96	1.98	2.15	2.16	2.33	2.35	2.51
B	2.07	2.66	2.25	2.84	2.43	3.03	2.62	3.21
C	2.14	2.74	2.33	2.92	2.51	3.11	2.69	3.29
D	2.13	2.62	2.31	2.81	2.50	2.99	2.68	3.17
E	2.01	2.60	2.19	2.79	2.38	2.97	2.56	3.15
F	2.09	2.78	2.27	2.96	2.45	3.15	2.64	3.33
G	2.11	2.77	2.29	2.96	2.47	3.14	2.66	3.32

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Table 11: Summary of un-ionised ammonia ( $\mu\text{g/l}$ ) at *Corallina* features (1 – 8) for mean temperatures, with the baseline flows.

Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile
C1	1.97	2.41	2.07	2.52	2.18	2.62	2.28	2.73
C2	2.01	2.50	2.12	2.60	2.22	2.71	2.33	2.81
C3	2.01	2.48	2.12	2.58	2.22	2.69	2.33	2.79
C4	1.98	2.44	2.09	2.54	2.19	2.65	2.30	2.75
C5	2.03	2.48	2.13	2.58	2.24	2.69	2.34	2.79
C6	1.97	2.43	2.08	2.54	2.18	2.64	2.29	2.75
C7	1.96	2.32	2.06	2.43	2.17	2.53	2.27	2.64
C8	1.98	2.39	2.09	2.49	2.19	2.60	2.30	2.70

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Table 12: Summary of un-ionised ammonia ( $\mu\text{g/l}$ ) at *Corallina* features (1 – 8) for mean temperatures, with the alternative flows.

Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile	Mean	95 <sup>th</sup> percentile
C1	2.03	2.47	2.21	2.66	2.40	2.84	2.58	3.02
C2	2.07	2.56	2.26	2.74	2.44	2.93	2.62	3.11
C3	2.07	2.54	2.26	2.72	2.44	2.90	2.62	3.09
C4	2.04	2.50	2.23	2.68	2.41	2.86	2.59	3.05
C5	2.09	2.54	2.27	2.72	2.46	2.91	2.64	3.09
C6	2.03	2.49	2.22	2.68	2.40	2.86	2.58	3.04
C7	2.02	2.38	2.20	2.57	2.38	2.75	2.57	2.93
C8	2.04	2.45	2.23	2.63	2.41	2.81	2.59	3.00



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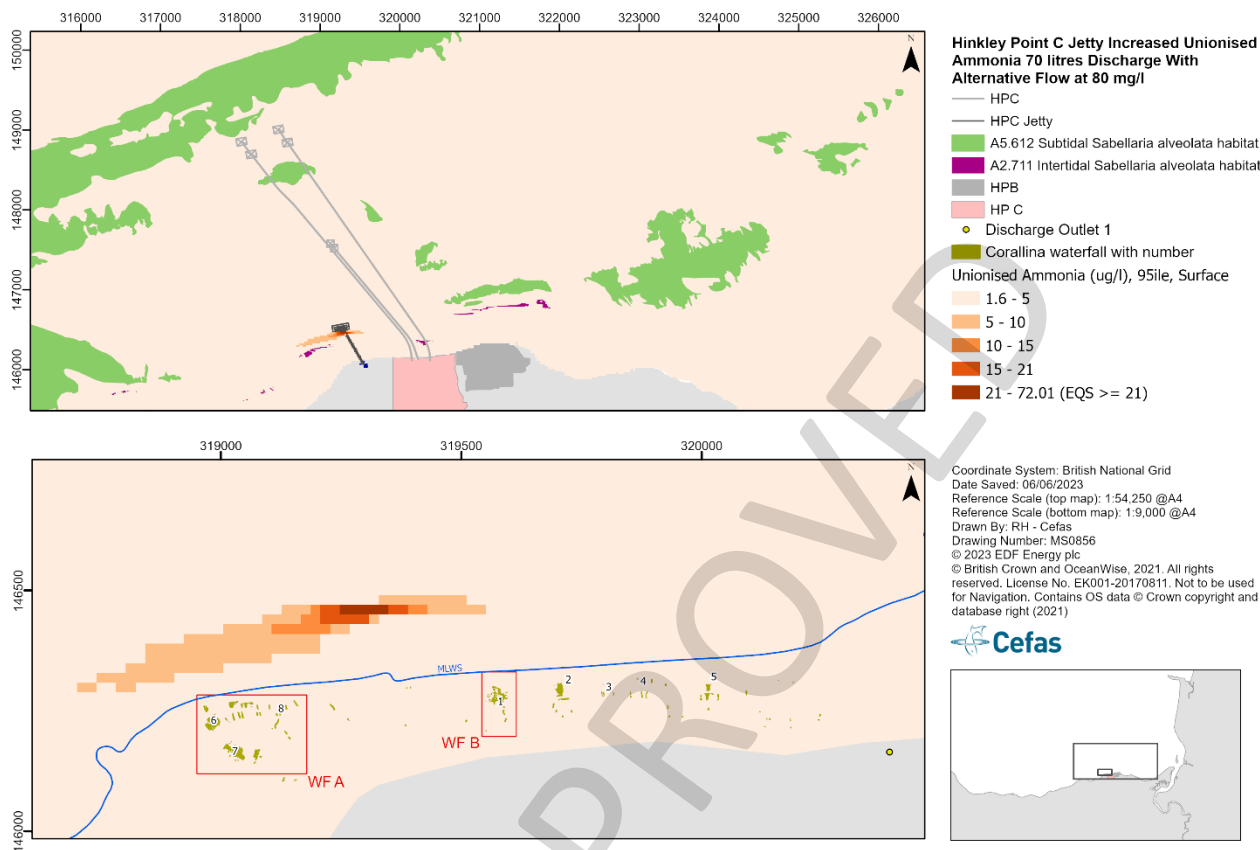


Figure 15: Surface 95<sup>th</sup> percentile un-ionised ammonia (38 l/s at 80 mg/l+ 70 l/s at 271 mg/l). The upper panel includes the intertidal and subtidal *Sabellaria*. The closest *Sabellaria* to the discharge is in the intertidal near station 8. The lower panel includes *Corallina* waterfalls.

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Table 13: Area of exceedance for un-ionised ammonia from GETM model.

Flows	Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
		Area > 21 µg/l Bed	Area > 21 µg/l Surface	Area > 21 µg/l Bed	Area > 21 µg/l Surface	Area > 21 µg/l Bed	Area > 21 µg/l Surface	Area > 21 µg/l Bed	Area > 21 µg/l Surface
Baseline	Construction (38 l/s) + Commissioning (70 l/s) Mean	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance
	Construction (38 l/s) + Commissioning (70 l/s) 95 <sup>th</sup> percentile	No exceedance	0.20 ha	No exceedance	0.20 ha	No exceedance	0.20 ha	No exceedance	0.20 ha
Alternative	Construction (38 l/s) + Commissioning (70 l/s) Mean	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance
	Construction (38 l/s) + Commissioning (70 l/s) 95 <sup>th</sup> percentile	No exceedance	0.20 ha	No exceedance	0.20 ha	No exceedance	0.20 ha	No exceedance	0.20 ha

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### 5.2.2 Total ammonia

For total ammonia, the PNEC based on the mean value is 1.1 mg/l, whilst the MAC based on the 95<sup>th</sup> percentile is 8 mg/l. The MAC was not exceeded at the surface or bed in any scenario, but the PNEC was exceeded at the surface but only for a maximum of 0.04 ha (equivalent to 1 grid cell in the model and the point of immediate discharge). In reality both the PNEC and MAC will be exceeded immediately at the point of discharge, but as the mixing would occur at a sub grid cell level, this is not seen in the GETM model. Figure 16 and Figure 17 show the spatial plots of the surface mean and 95<sup>th</sup> percentile total ammonia for the construction and commissioning discharges for the 80 mg/l scenario with alternative flows. Table 14 summarises the area of exceedance above the PNEC and MAC for total ammonia for all scenarios.

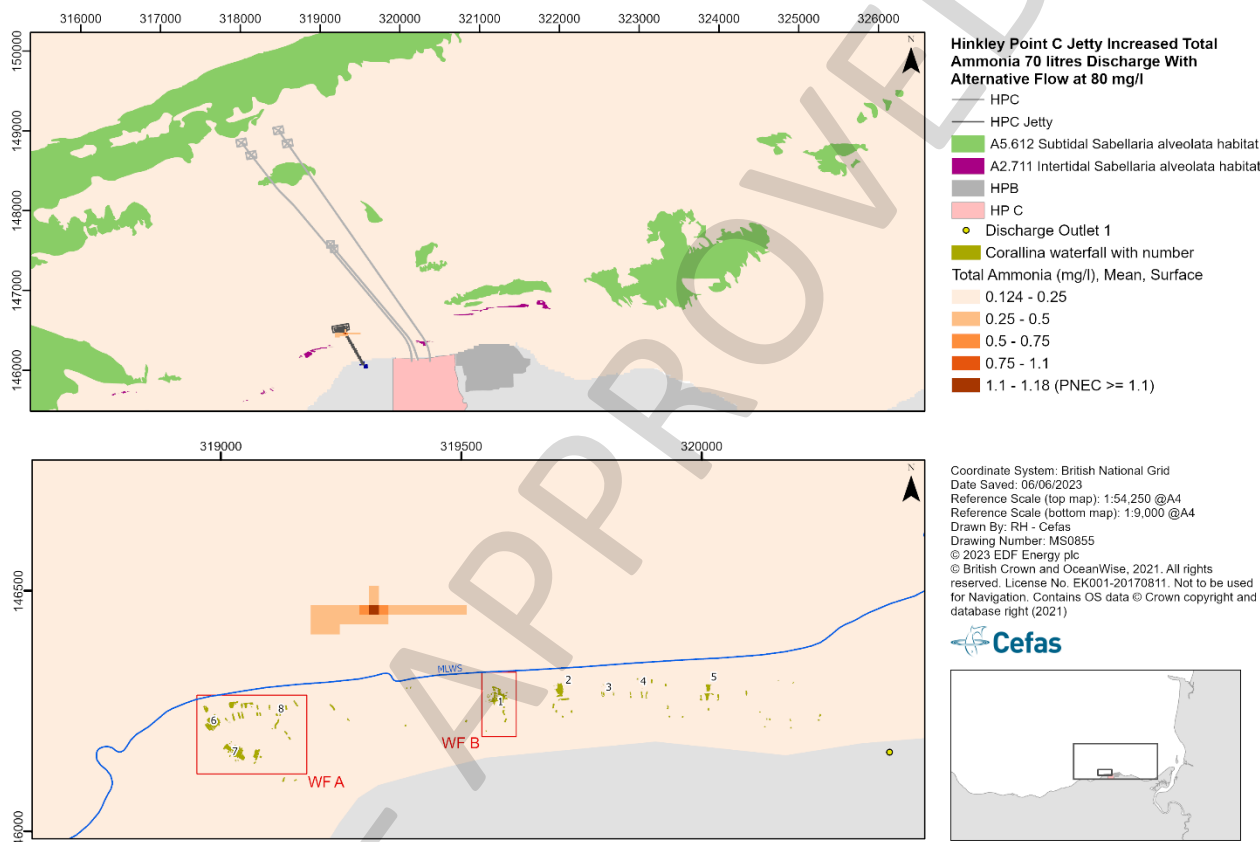


Figure 16: Surface mean ammonia concentration (mg/l) for the 80 mg/l at 70 l/s discharge simulation. The upper panel includes the intertidal and subtidal *Sabellaria*. The closest *Sabellaria* to the discharge is in the intertidal near station 8. The lower panel includes *Corallina* waterfalls.

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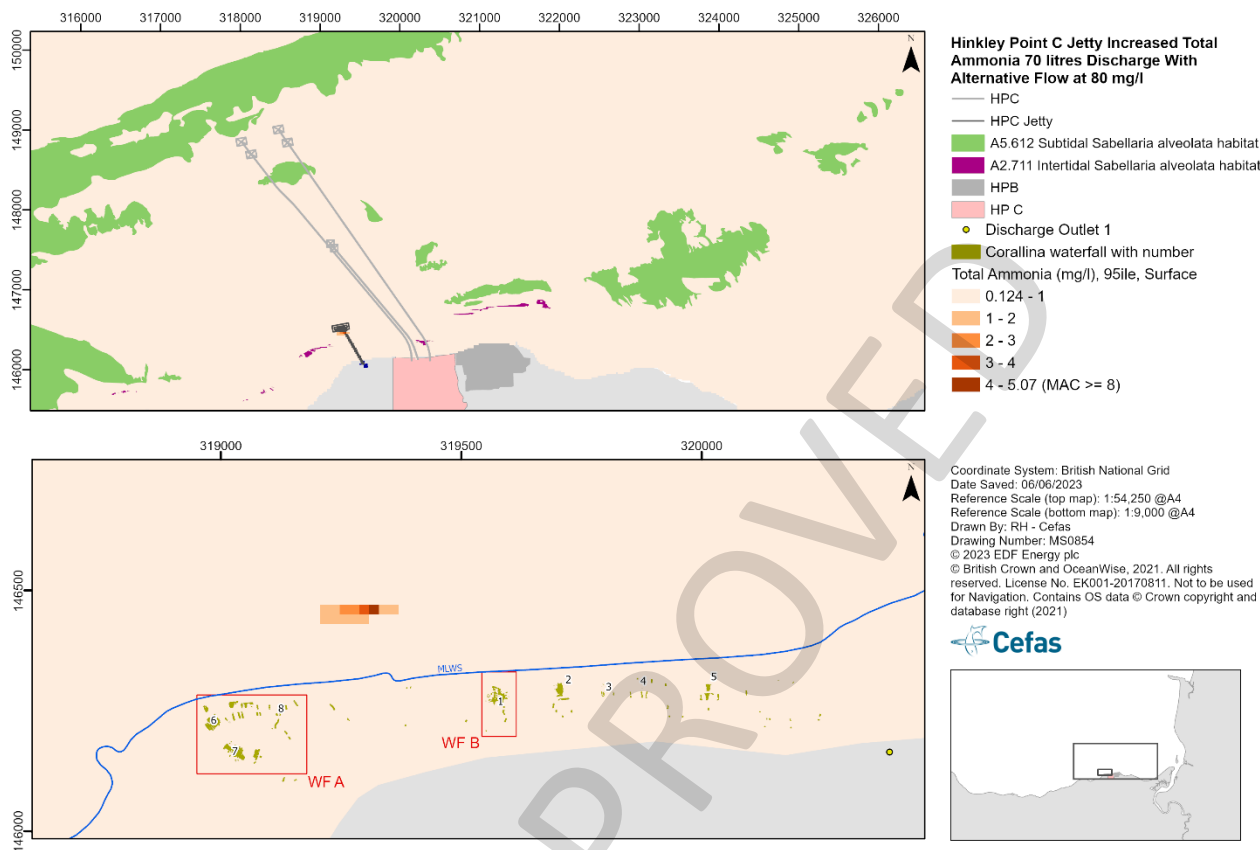


Figure 17: 95<sup>th</sup> percentile surface concentration (mg/l) of ammonia for 80 mg/l at 70 l/s. No value exceeds > 8000 µg/l MAC. The upper panel includes the intertidal and subtidal *Sabellaria*. The closest *Sabellaria* to the discharge is in the intertidal near station 8. The lower panel includes *Corallina* waterfalls.

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Table 14: Area of exceedance for total ammonia, above the PNEC (1.1 mg/l) and MAC (8 mg/l) from GETM model.

Flows	Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
		Area > 1.1 mg/l Bed	Area > 1.1 mg/l Surface	Area > 1.1 mg/l Bed	Area > 1.1 mg/l Surface	Area > 1.1 mg/l Bed	Area > 1.1 mg/l Surface	Area > 1.1 mg/l Bed	Area > 1.1 mg/l Surface
Baseline	Construction (38 l/s) + Commissioning (70 l/s) Mean	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	0.04 ha	No exceedance	0.04 ha
Alternative	Construction (38 l/s) + Commissioning (70 l/s) Mean	No exceedance	No exceedance	No exceedance	0.04 ha	No exceedance	0.04 ha	No exceedance	0.04 ha
Flows	Scenario	20 mg/l		40 mg/l		60 mg/l		80 mg/l	
		Area > 8 mg/l Bed	Area > 8 mg/l Surface	Area > 8 mg/l Bed	Area > 8 mg/l Surface	Area > 8 mg/l Bed	Area > 8 mg/l Surface	Area > 8 mg/l Bed	Area > 8 mg/l Surface
Baseline	Construction (38 l/s) + Commissioning (70 l/s) 95 <sup>th</sup> percentile	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance
Alternative	Construction (38 l/s) + Commissioning (70 l/s) 95 <sup>th</sup> percentile	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance	No exceedance

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## 6 Conclusion

Seven alternative discharge scenarios, from the HPC sewage treatment works, have been tested and compared to the original construction discharge scenario (treated sewage ammoniacal nitrogen at 20 mg/l at 13.3 l/s + ground water 4.7 mg/l at 25 l/s). The additional scenarios included increasing the treated sewage ammoniacal nitrogen concentration to 40, 60 and 80 mg/l, plus alternative flows by increasing the treated sewage flowrate by 10 l/s and decreasing the groundwater flow by 10 l/s. The assessments considered both the construction only discharge, plus the combined construction and commissioning discharges.

Applying the Environment Agency's Screening tests, the results of 'test 5' shows that when considering construction alone each scenario tested was within permissible limits. However, the partitioning of un-ionised ammonia is influenced by the physical conditions and this partitioning is not factored into the basic screening tests. Therefore, while the screening test was passed, further assessment of the discharges in terms of mixing calculations and nearfield modelling was conducted. When considering the combined construction and commissioning discharges, due to the considerable increase in ammonia from the commissioning phase, the screening tests were not passed. However, this is consistent with previous assessments (BEEMS Technical Report TR428) which required modelling to fully assess the potential implications of the commissioning discharges.

For the construction only discharge, nearfield modelling using CORMIX shows the concentrations of un-ionised ammonia fall below the EQS (21 µg/l) within <7.16 m for the original scenario (i.e. treated sewage at 20 mg/l ammoniacal nitrogen). This distance to the EQS increased to a maximum of 46.04 m for the 80 mg/l discharge scenario, with the original flows, and to 82.08 m for 80 mg/l discharge with the alternative flow rates. While the estimated mixing zone was considerably larger under the new scenarios compared to the baseline scenario (increasing from ~7m to over 80m), the mixing zone was still very small in respect to the scale of the receiving environment and therefore is not expected to cause any significant environmental effects.

Reanalysis of the GETM modelling results show that during the period where the construction and commissioning discharges overlap, the discharge scenarios will lead to an estimated additional 0.11 to 0.31 µg/l of un-ionised ammonia with the original flow rates and 0.06 to 0.61 µg/l of un-ionised ammonia with the alternative flow rates at the locations of the sensitive biological receptors. From the time series of instantaneous un-ionised ammonia concentrations at the eight *Corallina* locations and seven *Sabellaria* locations, the maximum instantaneous value (10.4 µg/l) was below the EQS of 21 µg/l. For all scenarios, the area of exceedance of un-ionised ammonia as a 95<sup>th</sup> percentile has a maximum value of 0.2 ha at the surface and was not exceeded at the bed. For context the receiving water body (Bridgwater Bay) has a surface area of 9,224.5 ha, and therefore the area of exceedance represents 0.002% of the water body.

For total ammonia, the MAC (8 mg/l as a 95<sup>th</sup> percentile) was not exceeded at the surface or bed in any scenario, but the PNEC (1.1 mg/l as a mean) was exceeded at the surface only, however only for a maximum of 0.04 ha (equivalent to 1 grid cell in the model and the point of immediate discharge).

The overall conclusion was that all of the scenarios considered would not lead to significant environmental effects.

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## Appendix A Additional Plots

### A.1 Time series of ammonia discharge

Figure 18 to Figure 25 show the individual time series of un-ionised ammonia at the *Corallina* locations C1-C8, as originally shown grouped in Figure 13. Figure 26 to Figure 32 show the individual time series of un-ionised ammonia at the *Sabellaria* locations A – G, as originally shown grouped in Figure 14.

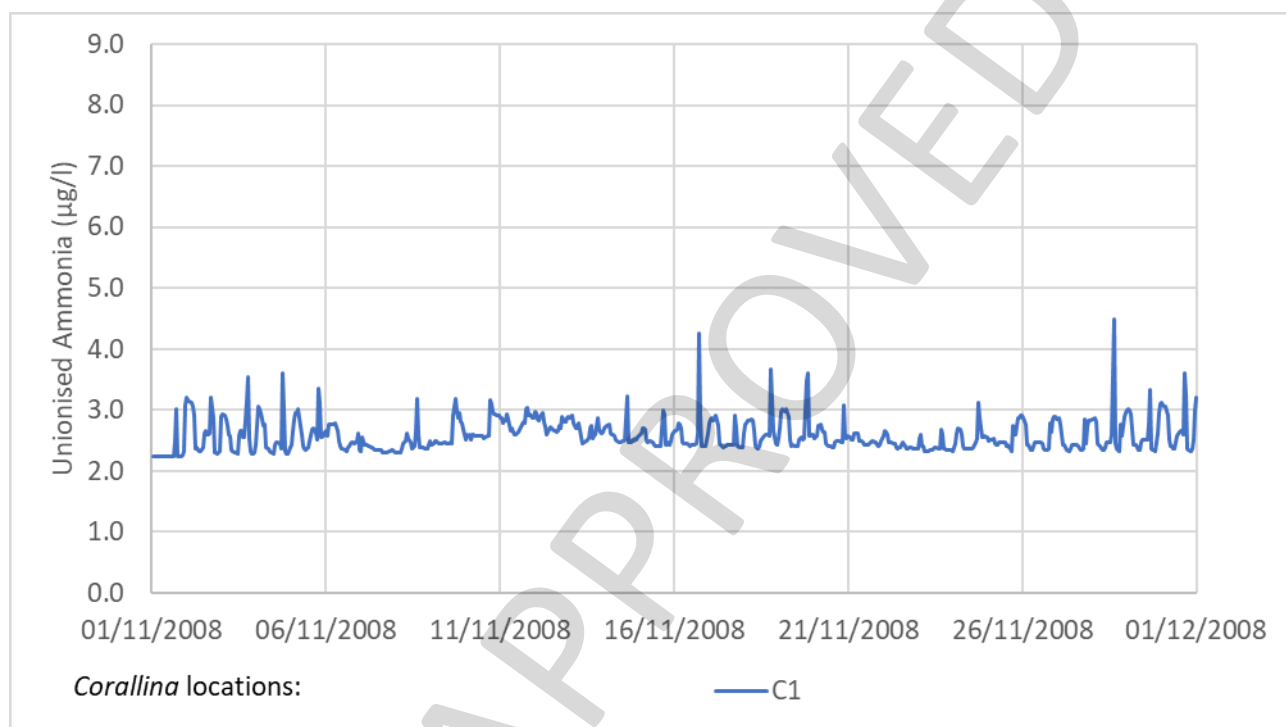


Figure 18: Time series of un-ionised ammonia at the *Corallina* location C1 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.



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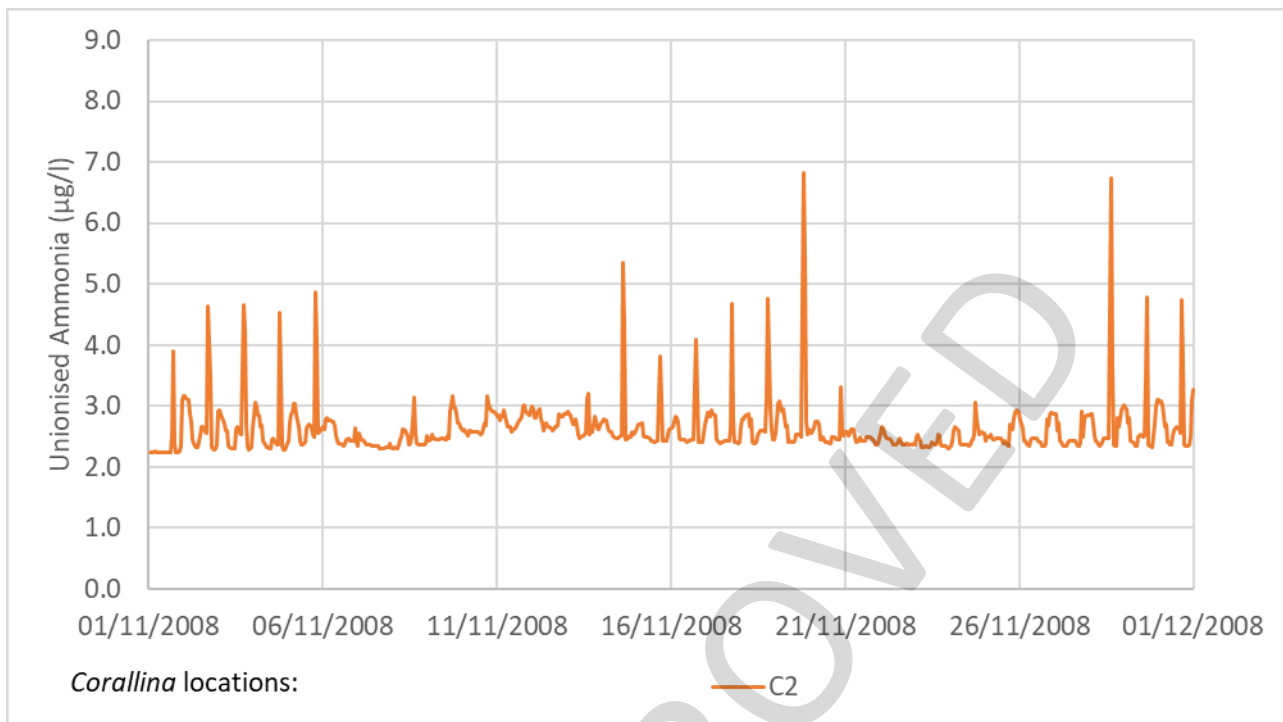


Figure 19: Time series of un-ionised ammonia at the *Corallina* location C2 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

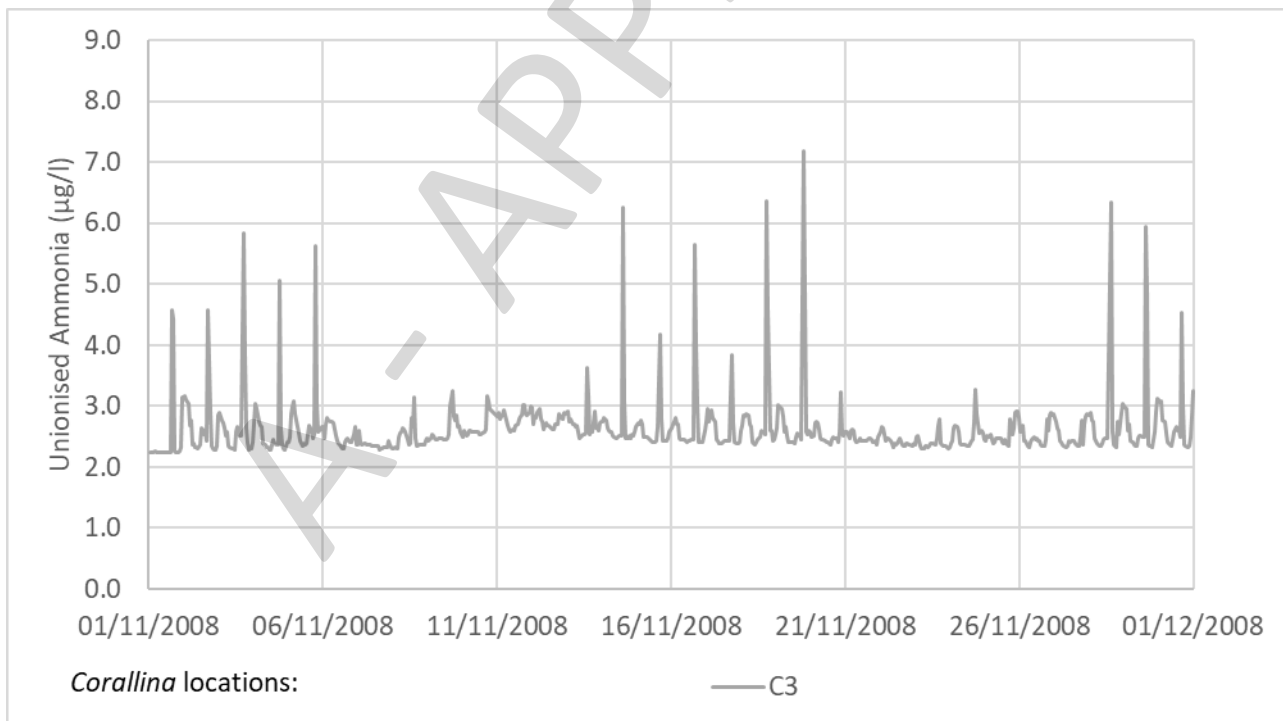


Figure 20: Time series of un-ionised ammonia at the *Corallina* location C3 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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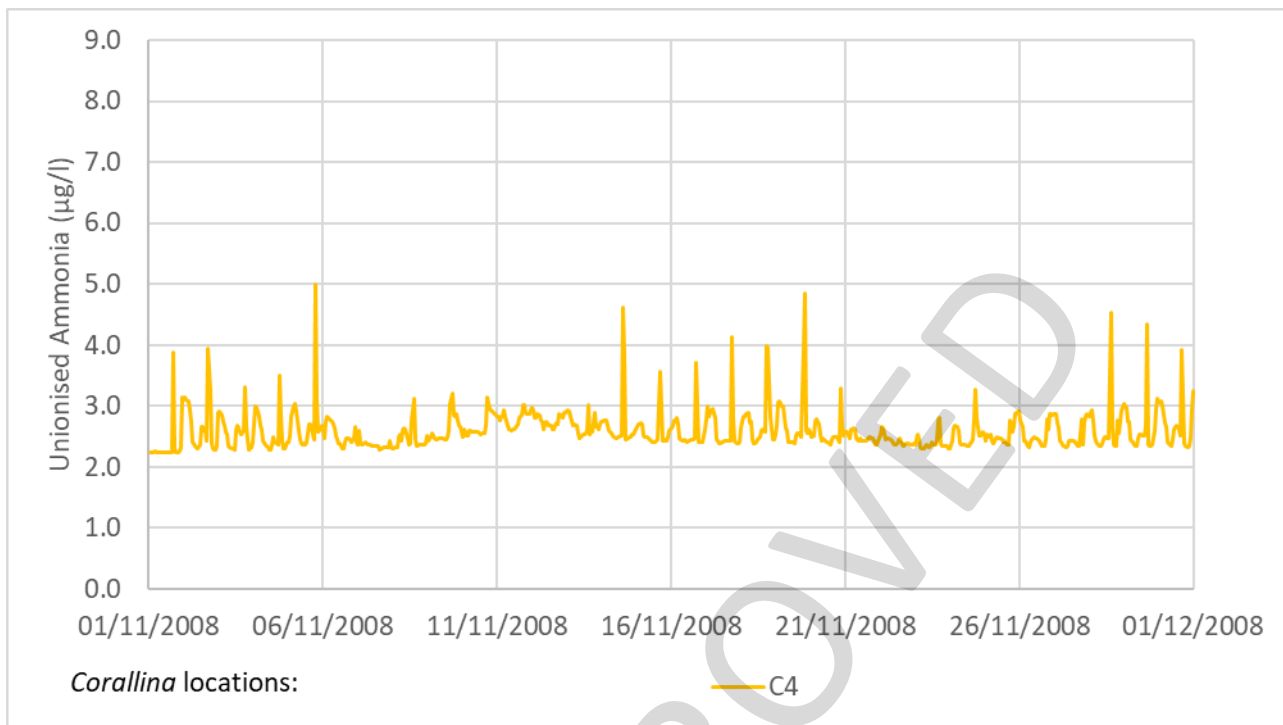


Figure 21: Time series of un-ionised ammonia at the *Corallina* location C4 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

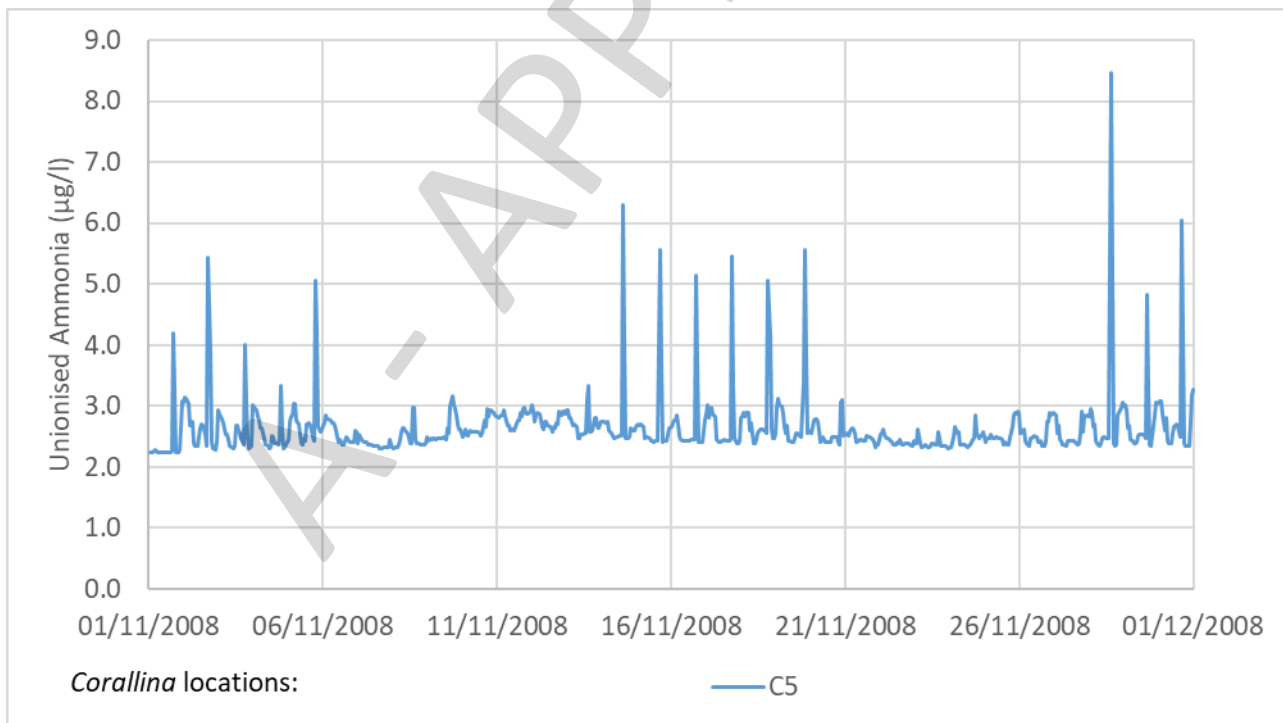


Figure 22: Time series of un-ionised ammonia at the *Corallina* location C5 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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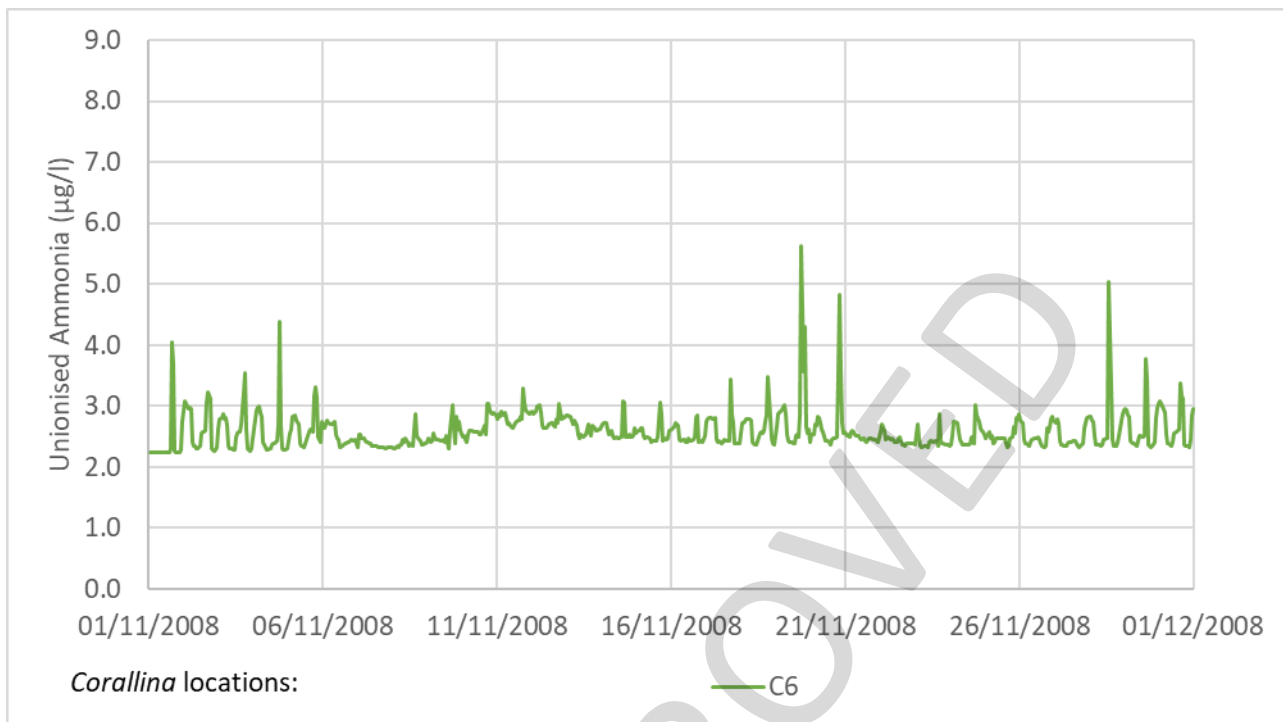


Figure 23: Time series of un-ionised ammonia at the *Corallina* location C6 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

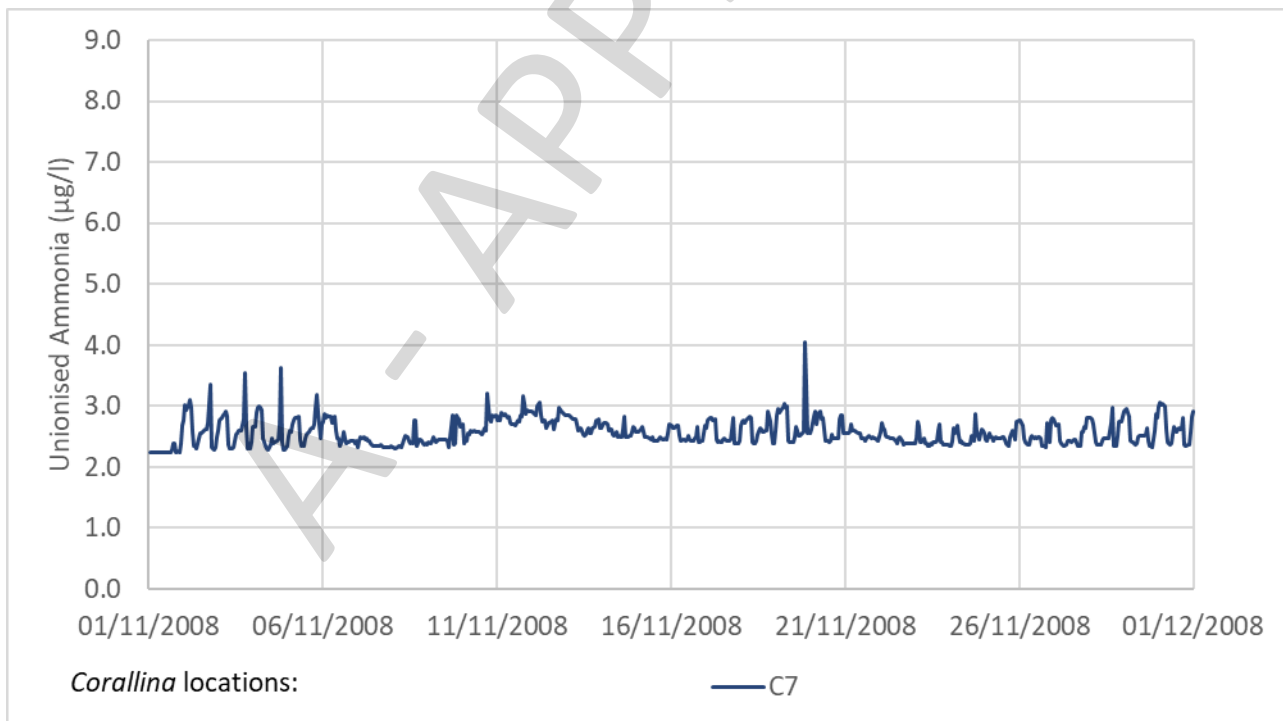


Figure 24: Time series of un-ionised ammonia at the *Corallina* location C7 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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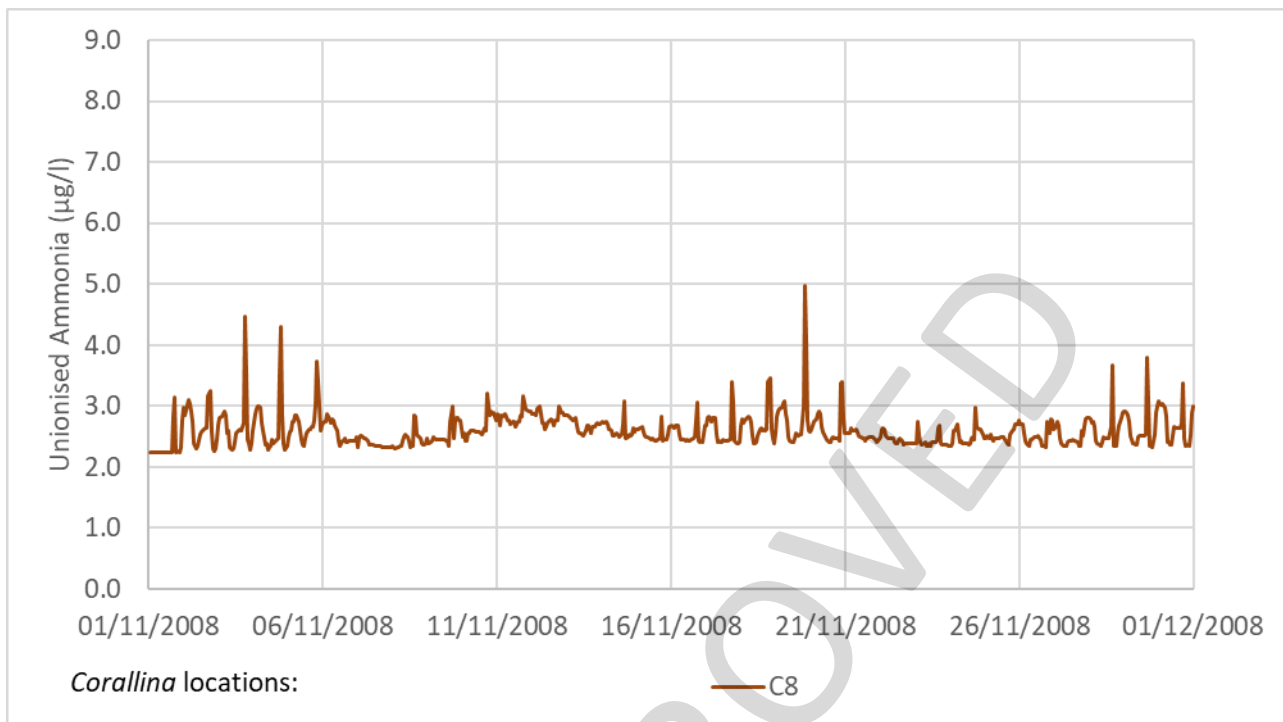


Figure 25: Time series of un-ionised ammonia at the *Corallina* location C8 for the alternative 38 l/s at 80 mg/l+70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

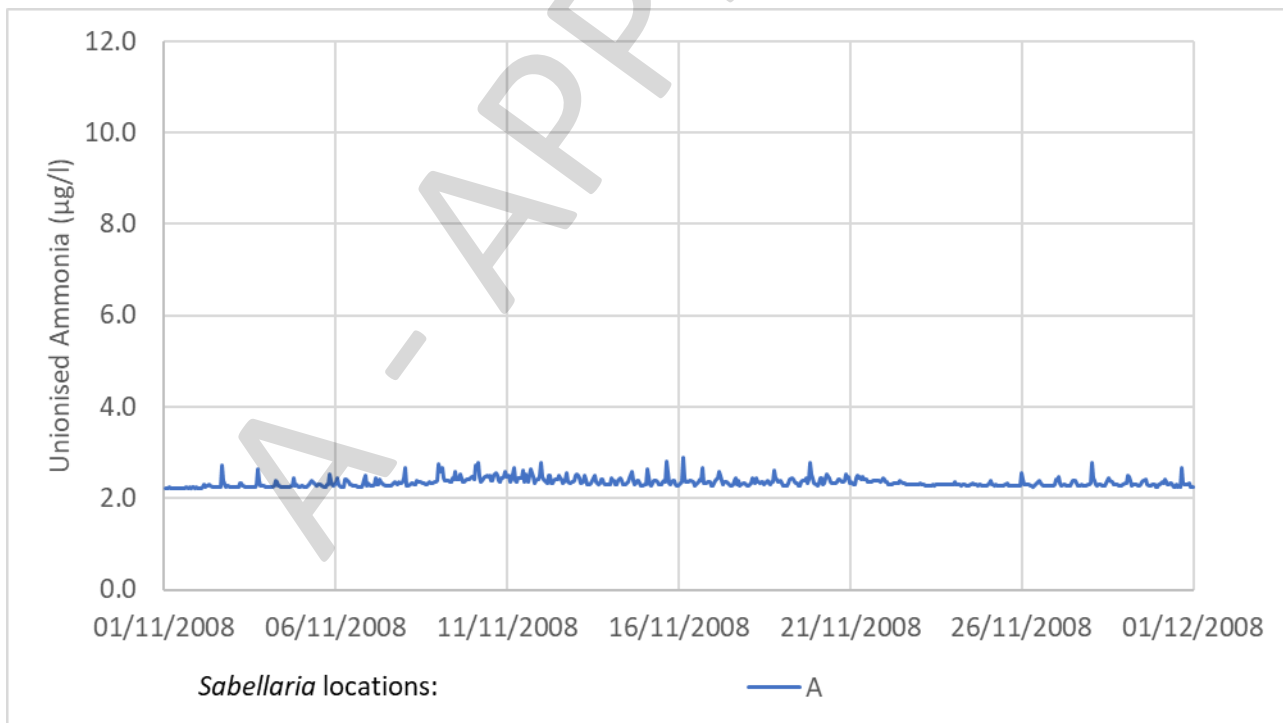


Figure 26: Time series of un-ionised ammonia at the *Sabellaria* location A for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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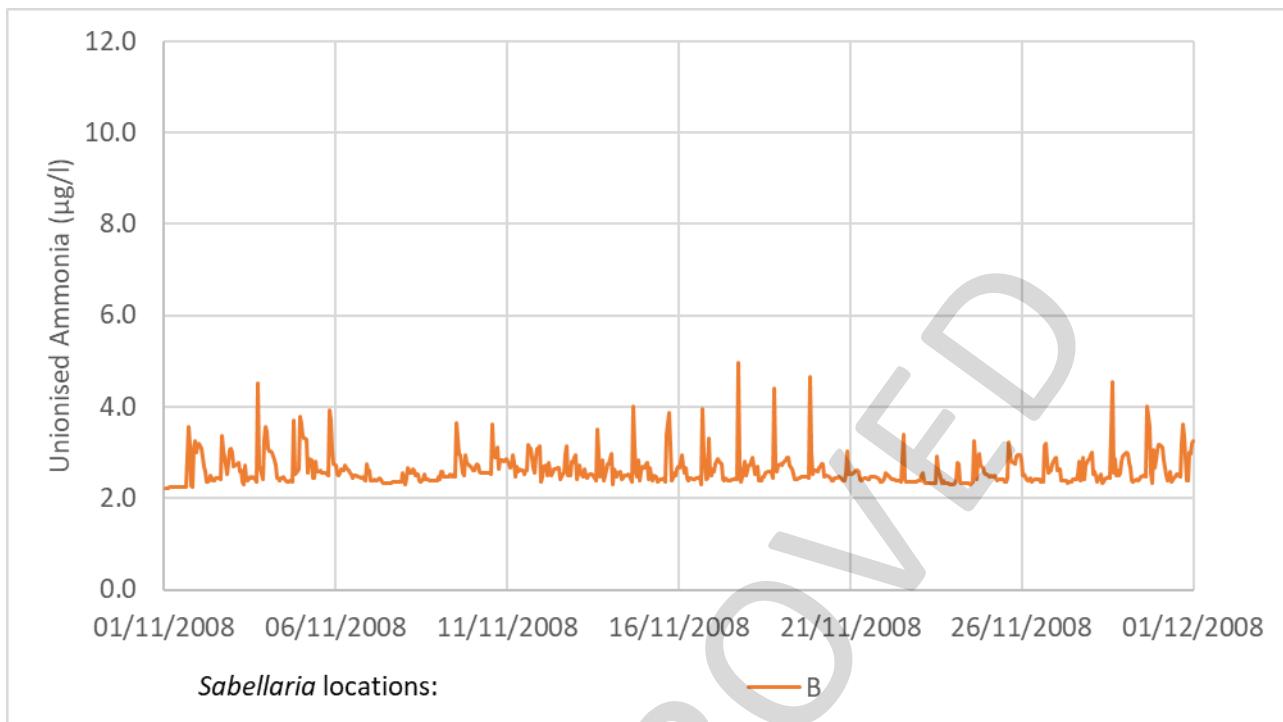


Figure 27: Time series of un-ionised ammonia at the Sabellaria location B for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

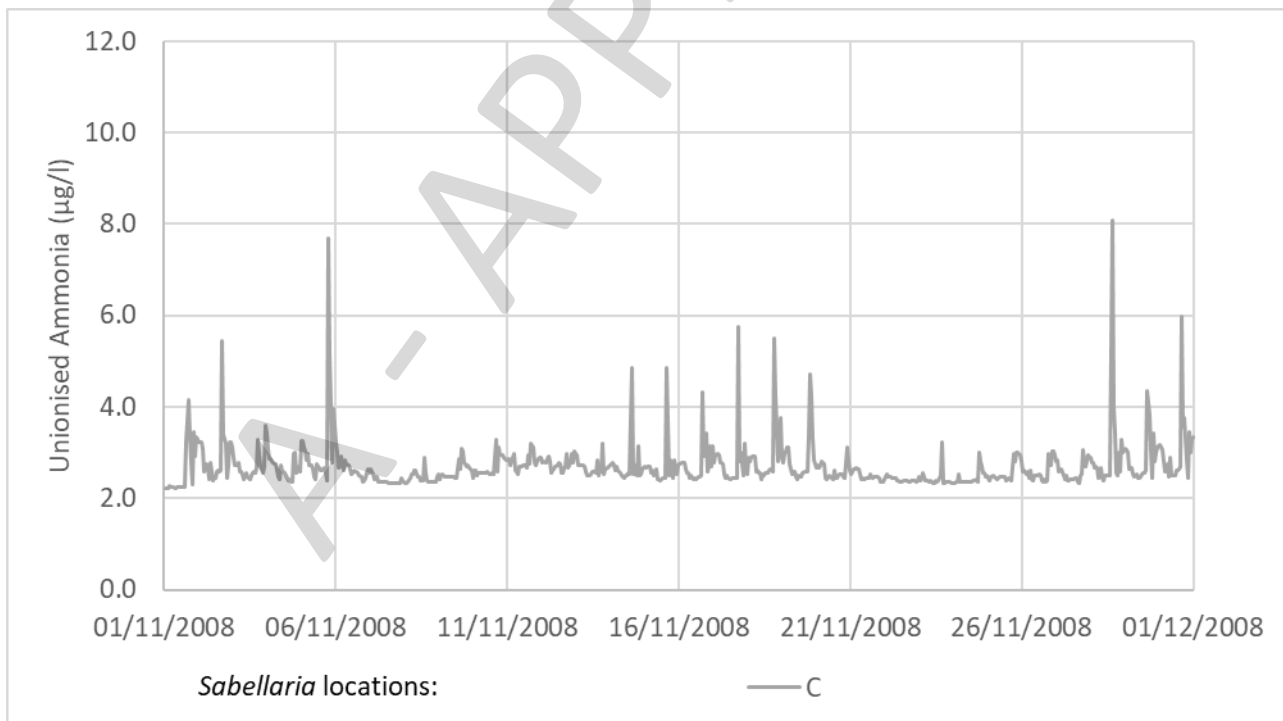


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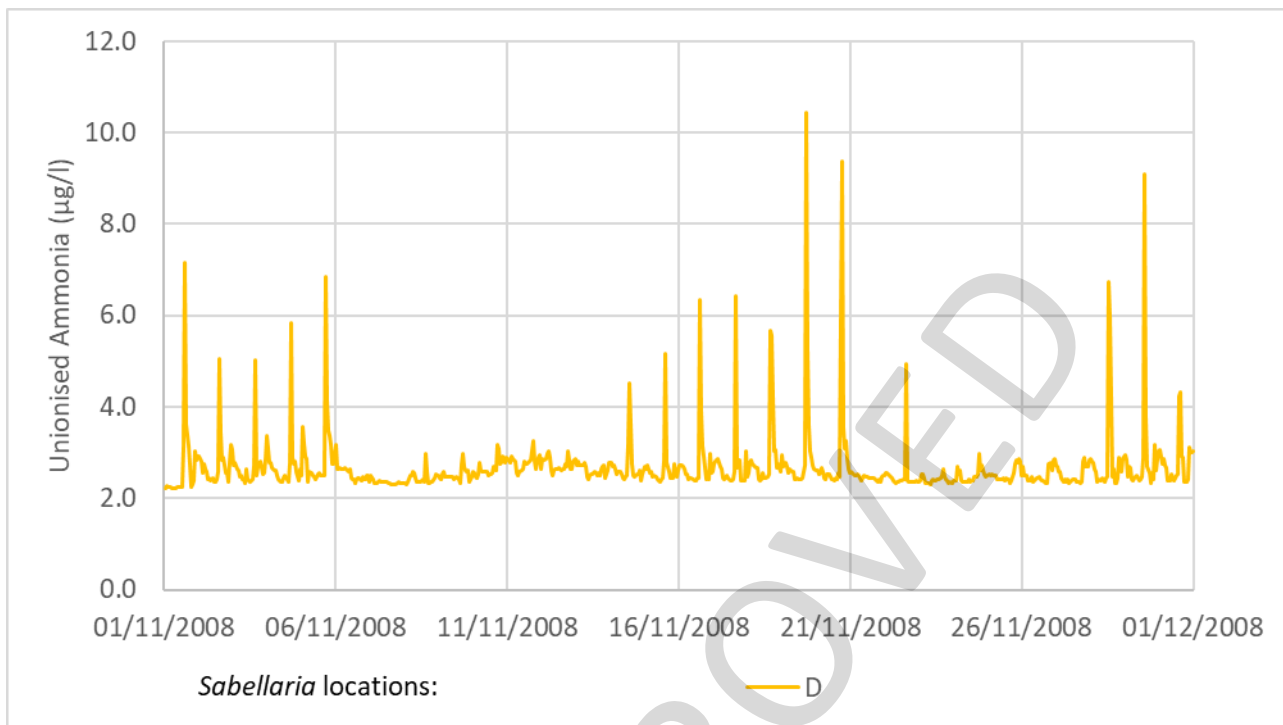


Figure 29: Time series of un-ionised ammonia at the *Sabellaria* location D for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

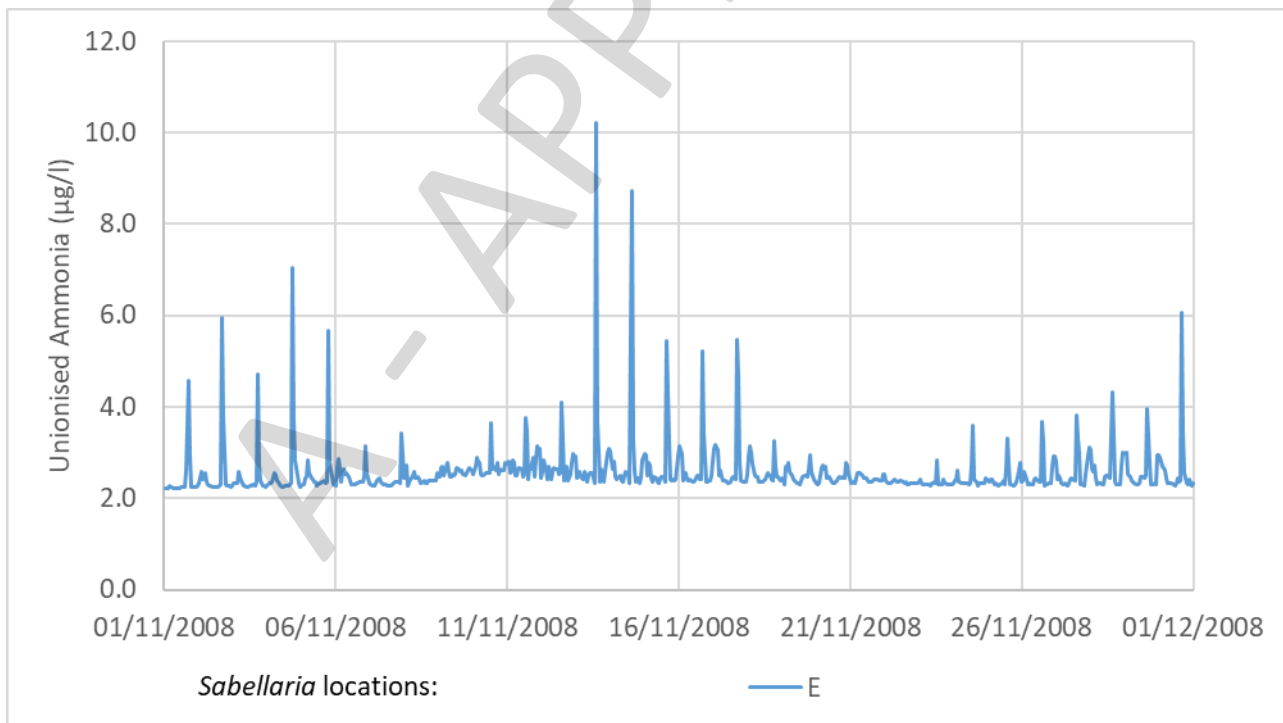


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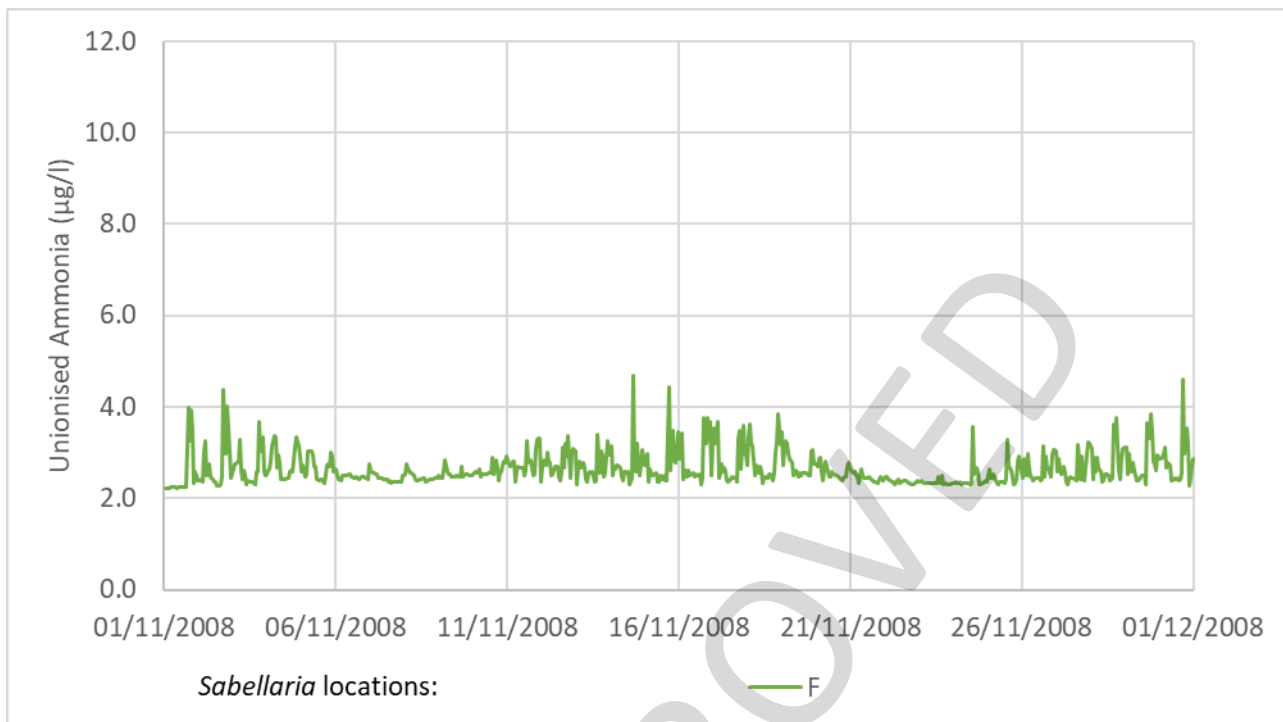


Figure 31: Time series of un-ionised ammonia at the *Sabellaria* location F for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

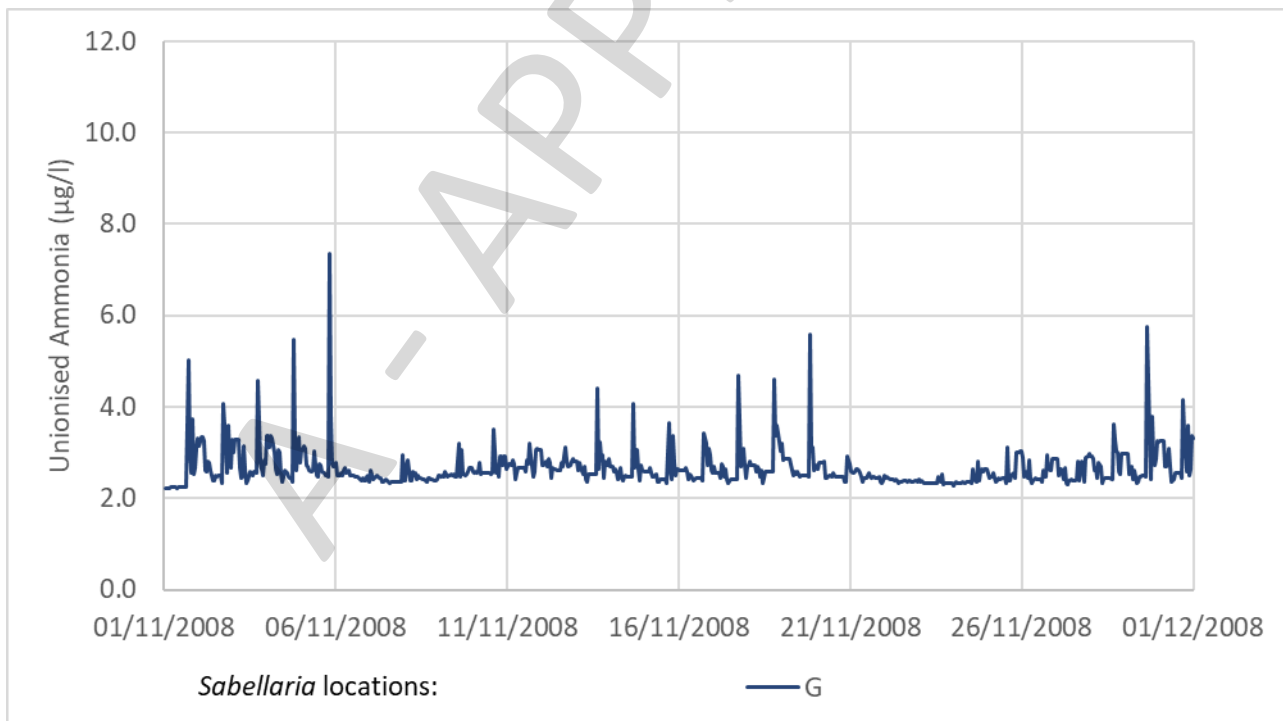


Figure 32: Time series of un-ionised ammonia at the *Sabellaria* location G for the alternative 38 l/s at 80 mg/l +70 l/s at 271 mg/l scenario using mean conditions of temperature, salinity, and pH.

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## Glossary

Term / acronym	Definition
AEVF	Allowable Effective Volume Flux
DCO	Development Consent Order
EQS	Environmental Quality Standard
EVF	Effective Volume Flux
HPC	Hinkley Point C
MAC	Maximum Allowable Concentration
PNEC	Predicted No Effect Concentration
WDA	Water Discharge Activity



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**APPENDIX B HINKLEY POINT C CONSTRUCTION DISCHARGE  
MODELLING ASSESSMENT AT THE TEMPORARY  
JETTY LOCATION**

A - APPROVED

**Cefas BEEMS Technical Report TR428; Hinkley Point C construction discharge modelling assessment at the temporary jetty location**

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<b>DOCUMENT TITLE</b>	Cefas BEEMS Technical Report TR428; Hinkley Point C construction discharge modelling assessment at the temporary jetty location.
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<b>ISSUE REASON</b>	P6 - For Construction
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<b>CONTRACTOR DOCUMENT NUMBER</b>	BEEMS Technical Report TR428	<b>CONTRACTOR REVISION</b>	14

		<b>ECS CODES</b>	

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01	14/08/2017	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Dean Foden	Hinkley Point lead
02	13/09/2017	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Brain Robinson	Programme director
03	15/09/2017	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Dean Foden	Hinkley Point Lead
04	19/10/2017	Dave Sheahan	Principal Scientist	Liam Fernand	Principal Physical Oceanographer	Liam Fernand	Principal Physical Oceanographer
05	25/10/2017	Dave Sheahan	Principal Scientist	Liam Fernand	Principal Physical Oceanographer	Brian Robinson	Programme Director
06	09/04/2018	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Dean Foden	Hinkley Point Lead
07	20/04/2018	Dean Foden	Hinkley Point Lead	Dave Sheahan	Principal Scientist	Dave Sheahan	Principal Scientist
08	08/06/2018	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Dean Foden	Hinkley Point Lead
09	26/01/2021	Liam Fernand	Principal Physical Oceanographer	Dave Sheahan	Principal Scientist	Dean Foden	Hinkley Point Lead
10	23/03/2021	Dave Sheahan	Principal Scientist	David Haverson	Modelling Lead	Dean Foden	Hinkley Point Lead
11	24/03/2021	Dave Sheahan	Principal Scientist	David Haverson	Modelling Lead	Dean Foden	Hinkley Point Lead
12	10/06/2021	Dave Sheahan	Principal Scientist	David Haverson	Modelling Lead	Dean Foden	Hinkley Point Lead
13	25/06/2021	Dave Sheahan	Principal Scientist	David Haverson	Modelling Lead	Andrew Griffith	Principle Investigator
14	24/11/2021	Dave Sheahan	Principal Scientist	David Haverson	Modelling Lead	Andrew Griffith	Principle Investigator

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Revision	Purpose	Amendment	By	Date
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02	Update	Revision following client comments	LF	13/09/2017
03	Update	Revised TBM chemicals source terms	LF	15/09/2017
04	Update	Revision following client comments	DS	19/10/2017
05	Update	Revision following regulator comments	DS	25/10/2017
06	Update	Revision following addition of sections on sewage discharge and coliforms	LF	9/04/2018
07	Update	Minor update in response to EDFE comments	DF	20/04/2018
08	Update	Update in response to comments from the Environment Agency	LF	08/06/2018
09	Update	Update to include cold commissioning	LF	26/01/2021
10	Update	Revision following client comments	DS	23/03/2021
11	Update	Revision following client comments	DS	24/03/2021
12	Update	Revision following EA and client comment	DS	10/06/2021
13	Update	Revision following EA and client comment	DS	25/06/2021
13	Update	Table correction following EA and client comment	DS	24/11/2021

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# Hinkley Point C construction discharge modelling assessment at the location of the temporary jetty Revision 14

Dave Sheahan, Liam Fernand, Amelia Araujo, Tiago Silva,  
Berrit Bredemeier, Lenka Fronkova, Jonathon Beecham,  
Mark Breckels, Gemma Kiff, Richard Harrod.

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temporary jetty location**

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	Version	Author	Date
Draft with source terms updated from Edition 1 and the inclusion of tunnel boring and sewage discharges	0.01	Liam Fernand	09/08/2016
Executive QC	0.02	Dean Foden	10/08/2017
Revision	0.03	Liam Fernand & Dave Sheahan	11/08/2017
Executive QC & Final Draft	0.04	Dean Foden	14/08/2017
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Revision following regulator comments	4.03	Liam Fernand	16/10/2017
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## Abbreviations and Glossary

Abbreviation / Term	Definition
AEVF	Allowable Effective Volume Flux
BOD	Biological oxygen demand
CETP	Commissioning Effluent Treatment Plant
CPM	Combined Phytoplankton and Macroalgal Model
CWDA	Construction Water Discharge Activity
CWW	Cementitious Washwater Water
DIN	Dissolved inorganic nitrogen
EQS	Environmental Quality Standard
EVF	Effective Volume Flux
CWW	Cementitious wastewater
GETM	General Estuarine Transport Model
HXA	KER, TER, SEK Tanks
KER	Liquid Radwaste Monitoring and Discharge System
MAC	Maximum Allowable Concentration
MSFD	Marine Strategy Framework Directive
NTU	Nephelometric Turbidity Units
PNEC	Predicted No Effect Concentration
PSU	Principal Salinity Units
SCL	Spray Concrete Lined
SEK	Conventional Island Liquid Waste Discharge System Tanks
TBM	Tunnel Boring Machine
TER	Additional holding tanks for return to liquid waste treatment
TraC	Transitional and Coastal
UV	Ultraviolet
WDA	Water Discharge Activity
WFD	Water Framework Directive

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This edition includes estimates of the effect of the additional nutrients and ammoniacal nitrogen due to the discharge of the breakdown products of hydrazine and other commissioning chemicals during the cold commissioning phase, during which drainage is expected from one or two HXA tanks per day. This has been included as a separate section (4.10). The methodology has three parts;

- i) To include the discharge in the GETM model so that the dilution and spreading of the ammonia plume and the potential for impact upon designated features can be considered.
- ii) Use of the CPM model to predict the impact upon phytoplankton production and macroalgae production in the wider estuary.
- iii) To consider the jetty discharges in the context of a Water Framework and habitats assessment.

**Changes made in Revision 10**

Following client feedback, the text was edited in several sections to clarify where changes have been made to introduce the commissioning discharge assessment. A section of abbreviations/glossary has also been added at the beginning this report.

**Changes made in Revision 11**

Minor sections of text were updated following client comments and some edits were made to clarify the keys in several Figures.

**Changes made in Revision 12**

Following feedback from the Environment Agency additional details have been added to the report to explain the different wastewater streams more fully for the cold commissioning phase and to include reference to the cementitious wastewater discharge. The different discharge scenarios were updated in Table 1 to include new wastewater streams. Data in Table 3 have also been updated to show calculations made by the Environment Agency in the stage 1 Habitats Regulations Assessment. The different discharge rates modelled for hydrazine and commissioning chemical discharges are explained in the context of the use of a hydrazine treatment plant and post treatment storage prior to discharge. Explanation is provided that a separate report BEEMS technical report TR550 provides a more comprehensive assessment of biological quality elements and designated features.

**Changes made in Revision 13**

Following feedback from the Environment Agency additional details have been added to the report: Corrections and clarification have been made to Table 1 and it is highlighted that Case D discharges during the construction period are those that most represent the situation now and including the period when CWW and commissioning discharges would also take place. Recalculations by the Environment Agency made to groundwater datasets resulted in reductions in nitrogen loading figures and these are shown where applicable. Some small increases in metals discharges also resulted and are indicated but these do not change the assessment. Some further detail was added to explain that the in-combination effects of the small discharge of CWW are unlikely to result in significant changes to the assessment made for in combination inputs from Case D construction activity and from commissioning wastewater.

**Changes made in Revision 14**

Following further feedback from the Environment Agency (23/11/21) additional details have been added to the report: Corrections and clarification have been made to Table 25 the heading and table values have been edited so that it now shows H1 tests for the combined construction wastewater and the commissioning wastewater discharges for total ammonia and unionised ammonia.

**Conclusions**

Early versions of this report provided an assessment of the construction discharge only. From version 7 the commissioning inputs of un-ionised ammonia, phosphorus, and nitrogen in combination with the construction

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bed, the relevant concentration was predicted to be below EQS within 5 metres of the discharge. Neither mean bed concentrations nor 95<sup>th</sup> percentile concentrations exceed the EQS, and benthic features should therefore remain unaffected.

Ammoniacal nitrogen discharge is at its maximum during the construction period when cold commissioning wastewater discharges occur. Assessment of combined discharges showed no areas of exceedance for either total ammonia concentrations or the mean un-ionised ammonia EQS at the surface or the bed. An area of only 0.2 ha at the surface was predicted to exceed the EQS for un-ionised ammonia as a 95<sup>th</sup> percentile. More detailed time series analysis, considering more extreme summer temperatures when the proportion of un-ionised ammonia is likely to be maximal, confirmed that concentrations were less than 25% of the EQS at the locations closest to *Corallina* and *Sabellaria* features. The same assessment would apply to lower sensitivity habitat close to the jetty discharge.

A habitats assessment provided in BEEMS TR443 established that there was either no pathway for effects or no likely significant effects arising from jetty discharges of construction chemical inputs during Case C and Case D, which are considered the most significant inputs during the construction period.

The predicted discharge concentrations of hydrazine used in cold commissioning were evaluated for toxicological effects in BEEM TR445. A discharge concentration of 15 µg l<sup>-1</sup> was sufficiently precautionary that the acute PNEC was never exceeded at the *Corallina* features and only at *Sabellaria* stations D and E. Furthermore, the plume was very short lived (1-2 hours) and concentrations were well below the acute PNEC (4 ng l<sup>-1</sup> as a 95<sup>th</sup> percentile) at all features.

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# 1 Background

Cefas has been commissioned by NNB Generation Company (HPC) Ltd (NNB GenCo) to assess the priority substances and specific pollutants present in various discharges, to be made under a proposed construction Water Discharge Activity (CWDA) permit application, at the location of the temporary jetty at Hinkley Point C (HPC) (to be known as Outlet 12). Dilution and dispersion of the substances in the marine environment have been investigated using a validated GETM (General Estuarine Transport Model) model of Hinkley Point (see BEEMS Technical Report TR267 Edition 2).

The flow rates used for the modelling construction and commissioning discharges are shown in Table 1. The contaminants of concern are:

1. Groundwater from the dewatering system which contains metals and dissolved inorganic nitrogen (DIN) and ammoniacal nitrogen.
2. Treated sewage discharge which contains DIN and ammoniacal nitrogen from three permanent treatment units.
3. Effluent from tunnel excavations containing small amounts of Tunnel Boring Machine (TBM) soil conditioning chemicals and variable quantities of groundwater containing metals and DIN. Input of tunnelling effluent is scheduled to stop in January 2022.
4. Cementitious wastewater discharge (CWW).
5. Commissioning discharge of hydrazine.
6. Commissioning discharge considering hydrazine, ethanolamine contribution to ammoniacal nitrogen,
7. Commissioning discharge considering hydrazine, ethanolamine contribution to nitrogen and trisodium phosphate contribution to phosphorus.

Dewatering of deep excavations is required during the construction of HPC. In this process, groundwater is pumped from a network of deep boreholes and discharged sub-tidally at a location near the seaward end of the HPC temporary jetty.

NNB GenCo has reviewed the data from the boreholes that will form the longer-term network (those along the northern, western, and eastern sides of the deep excavation), as well as wider data sets that are reflective of current conditions, including temporary boreholes installed to enhance the efficacy of local dewatering. In each case, the 95<sup>th</sup> percentile for each of the substances of concern has been considered as this excludes anomalously high values while still providing a robust assessment. To enable a robust assessment of the potential impacts of the proposed discharge on the marine environment and interest features to be completed, reasonable worst-case values have been selected from these datasets and from the March 2017 data upon which Edition 1 of this report was based. This report contains the results of modelling these updated worst-case values.

The output from the permanent sewage treatment plants is discharged via the HPC temporary jetty.

The main bulk of the tunnelling material (with associated soil conditioning chemicals) is returned with the spoil to the muck bay. The tunnelling spoil will be re-used on-site in accordance with the site materials management plan. Sources of water from the tunnelling operations will include groundwater entrained within the tunnelling spoil, groundwater from the shaft dewatering, very minor seepages of groundwater into the tunnel, water used for cleaning equipment and dust suppression, surface run-off from the muck bay and groundwater seepage into the launch pits and Spray Concrete Lined (SCL) tunnels.

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One of the issues when considering all three discharge streams is to consider the timescale of the likely discharges and potential maximum discharges and loads. This report considers when loads of a contaminant are at maximum levels or are likely to persist as discharges for a reasonable period.

### **1.1 Indicative construction discharge schedule**

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In August 2017 based on the best knowledge of the likely sequencing of different phases of the construction period, a series of discharge scenarios was developed taking account of the highest likely wastewater inputs from different construction sources. These Cases A to D were used to assess the maximal inputs of different contaminants of concern. Case E is omitted here but essentially covers the latter period of construction when tunnelling inputs are completed. This schedule is included to enable the plausible worst-case volume and contaminant concentrations to be considered for permitting. The schedule will inevitably change, but the summary of the worst-case conditions should cover the likely changes. The indicative sequence, duration and start point for different activities as envisaged in August 2017 is provided in Table 1 and Figure 1. For the assessment of the contaminant inputs from the cementitious waste water (CWW) and commissioning discharges the construction activities and discharges that are occurring in combination are best represented by those described for Case D. No seasonal dependence of the schedule has been considered therefore changes to the start or end times do not affect conclusions in the assessment: the assessment of impact is not dependent on the seasonality of the operations. The main seasonal factors affecting the discharge are wind variations and wave mixing. The modelling undertaken does not include wave mixing and so is conservative. Seasonal increases in wave height will increase mixing and reduce the areas of intersection (if any exist) between features and discharged waters above EQS concentrations. Even in the worst-case modelling condition no such intersection exists, and therefore we conclude that the areas of intersection will not be changed because of seasonal influences.

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Table 1. Indicative sequencing of the relevant discharges based upon August 2017 construction plans. (Recent data on the actual flow rates for groundwater and tunnel effluent indicate that the values used here provide precautionary assumed overlaps between different activities and contaminant source contributions.)

Main site Groundwater	Sewage	Week	Tunnelling wastes (and associated) discharges	Case
De-watering discharge at Jetty, 20 l s <sup>-1</sup>		1	NA	Case A 20 l s <sup>-1</sup> (jetty)
20 l s <sup>-1</sup>		17	Approximately 7 l s <sup>-1</sup>	N/A
20 l s <sup>-1</sup>	sewage treatment plant discharge (jetty) 13.3 l s <sup>-1</sup>	25	12 l s <sup>-1</sup> ramping up to 22 l s <sup>-1</sup> as SCL works ramp up. Tunnelling for intake 1 continues.	Case B 55 l s <sup>-1</sup> (jetty)
20 l s <sup>-1</sup>	13.3 l s <sup>-1</sup>	49	30 l s <sup>-1</sup> (ca. 26.7 l s <sup>-1</sup> groundwater also including ca. 3 l s <sup>-1</sup> soil conditioning chemicals from the use of 1 TBM).	<b>Case C</b> Peak Ca., 63 l s <sup>-1</sup> (jetty)
20 l s <sup>-1</sup>	30 l s <sup>-1</sup> . Rare but potentially maximum discharge.	49	30 l s <sup>-1</sup> (ca. 26.7 l s <sup>-1</sup> groundwater also including ca. 3 l s <sup>-1</sup> soil conditioning chemicals from the use of 1 TBM).	<b>Case C1max</b> Peak Ca., 80 l s <sup>-1</sup>
20 l s <sup>-1</sup>	13.3 l s <sup>-1</sup>	81	SCL works complete. Tunnelling continues HPC Intake 1, Outfall, and Intake 2. Maximum use of TBM soil conditioning chemicals corresponds to the output from 2 TBMs working simultaneously. 6 l s <sup>-1</sup>	<b>Case D</b> 40 l s <sup>-1</sup> (original tunnelling assessment) <sup>2</sup> 38.3 l s <sup>-1</sup> assessed for combined commissioning input at jetty <sup>3</sup>
(20 l s <sup>-1</sup> ) <sup>4</sup>	(13.3 l s <sup>-1</sup> ) <sup>4</sup>	NA <sup>5</sup>	Cementitious wastewater (CWW) plus other Case D inputs	<b>Case F</b> (0.6 l s <sup>-1</sup> CWW) <sup>6</sup>
(20 l s <sup>-1</sup> ) <sup>4</sup>	(13.3 l s <sup>-1</sup> ) <sup>4</sup>	NA <sup>5</sup>	Commissioning discharge – this input contributes nitrogen and ammoniacal nitrogen from addition of ammonia and breakdown of hydrazine, ethanolamine, and phosphorus from trisodium phosphate see section 3.5 and 4.10 plus other Case D inputs	<b>Case J</b> <sup>7</sup> (70 l s <sup>-1</sup> commissioning discharge)

<sup>1</sup> There has been no treated sewage discharge from the jetty as of 1<sup>st</sup> June 2021 but discharges are scheduled to start in the next few months; <sup>2</sup> For the original 2017 assessment of tunnelling chemicals a minimal groundwater dilution flow (20 l s<sup>-1</sup>) was assumed during Case D. This effectively produced a most conservative scenario for tunnelling chemicals as it minimises dilution (assuming 20 l s<sup>-1</sup> groundwater + 13.3 l s<sup>-1</sup> treated sewage + 6 l s<sup>-1</sup> tunnelling chemical which was rounded up to 40 l s<sup>-1</sup> discharge);

<sup>3</sup> The total volume for assessment of DIN during Case D 38.3 l s<sup>-1</sup> includes 13.3 l s<sup>-1</sup> sewage contribution + 20 l s<sup>-1</sup> general groundwater input + 5 l s<sup>-1</sup> groundwater from tunnelling. The additional 6 l s<sup>-1</sup> tunnelling chemical make-up water will not add DIN but will dilute the overall concentration so to provide the most conservative assessment this was not included in the flow rates for the DIN calculation.

<sup>4</sup> The total volume of groundwater (including 5 l s<sup>-1</sup> from tunnelling) and sewage contributions of chemicals of concern during Case D are considered in combination with additions of the same contaminants from CWW or commissioning inputs.

<sup>5</sup> NA - not applicable as start timing not identified in 2017 scheduling

<sup>6</sup> During Case F cementitious wastewater input contributions are evaluated in combination with those for Case D

<sup>7</sup> During Case J the construction discharge for DIN and ammoniacal nitrogen uses the Case D example at 25 l s<sup>-1</sup> groundwater with additional contributions from commissioning inputs.

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to conduct further detailed modelling to determine the extent and magnitude of the predicted exceedance of the EQS in the receiving waterbody.

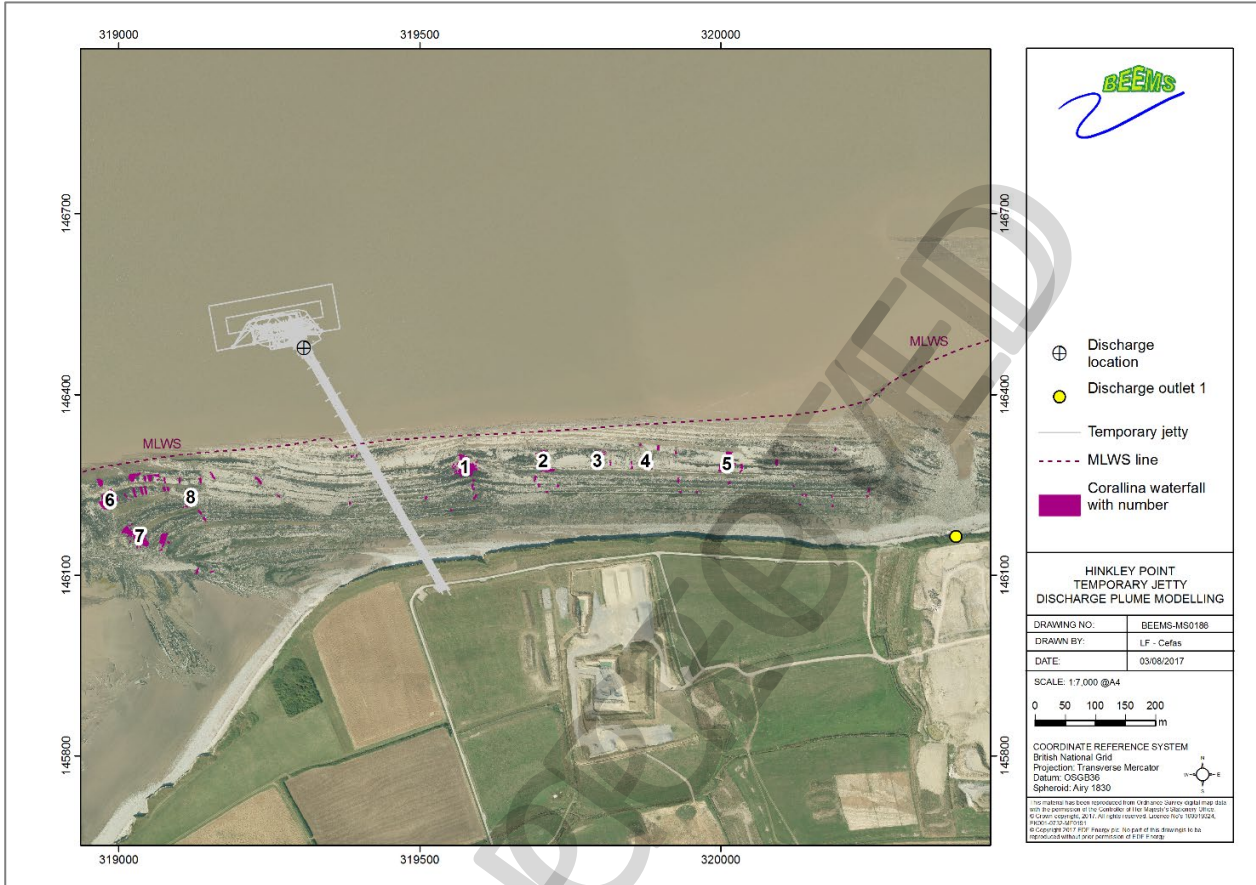


Figure 2. Location of the temporary jetty and proposed discharge point (shown by a cross within a circle). The main *Corallina* features of interest shown in purple and numbered for future reference in this report. The existing cross shore discharge point (Outlet 1) is shown by a yellow circle.

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## 2 Application of Environment Agency guidance for the assessment of the subtidal discharge.

The EA screening approach applies to the discharge from the jetty because the discharge is to the subtidal environment and beyond 50m from mean low water spring (MLWS) tidal level. The proposed construction discharge is a low volume of groundwater, sewage treatment effluent and tunnelling waste (see Table 1) with concentrations of some contaminants exceeding EQS levels. The properties of the proposed discharge are shown in Table 2. The commissioning discharge and cementitious water discharges are discussed in the construction and cold commissioning section 3.5.

Table 2. Proposed jetty discharge characteristics. The discharge location is shown in Figure 2.

Discharge Characteristics	Value
Location OSBG	319315E 146475N
Location WGS84	51° 12.7056' N 003° 9.3894' W (51.21176 N 3.15649 W)
Charted water depth (surface to bed) at discharge location	At least 3.0 m
Discharge flow	Varies with Case.
Discharge salinity	1 PSU

### Groundwater priority and specific contaminant data

When calculating summary statistics for all substances, any values below the method detection limit were adjusted to a value of half the detection limit. For metals, modelling tests use both total and dissolved concentrations to assess potential deterioration of surface water quality (Environment Agency, 2014). The total concentration of substances was used in the initial screen and in subsequent modelling to take account of uncertainty regarding the partitioning of substances into the dissolved phase as the groundwater mixes with the seawater. For several neutral hydrophobic chemicals and some metals, however, solubility would be expected to decrease under saline conditions (Turner, 2003). The assessment includes the screening of the source terms against the saltwater EQS values presented in the Water Framework Directive (Standards and Classification) Directions (England and Wales) (WFD, 2015). NNB GenCo has reviewed the data from the boreholes that will form the longer-term network (those along the northern, western, and eastern sides of the deep excavation) as well as wider data sets that are reflective of current arrangements, including temporary boreholes installed to enhance the efficacy of local dewatering. In each case, the 95<sup>th</sup> percentile for each of the substances of concern has been considered as this excludes anomalously high values while still providing a robust assessment. To enable a robust assessment of the potential impacts of the proposed discharge on the water environment and on the interest features to be made, the worst-case values have been selected from these datasets and from the March 2017 data. Summary statistics for the concentrations of substances measured in the site groundwater carried forward to the modelling assessment are shown in Table 3.

The updated guidance for surface water pollution (Environment Agency, 2016) recommends the application of an initial test (Test 1) for discharges to Transitional and Coastal (TraC) waters in which the discharge concentration is compared to the relevant quality standard or equivalent for that substance. Where the discharge concentration exceeds the standard concentration, further assessment is required. As this construction discharge will be subtidal a further test ("Test 5") is recommended, comparing the discharge specific Effective Volume Flux (EVF) with the location specific Allowable Effective Volume Flux (AEVF). If the EVF is not greater than the AEVF, then the discharge is considered insignificant and is screened out.

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Relative to chart datum the discharge depth for construction related effluents will be at least 3.0 metres therefore a maximum AEFV value of 3.0 is used for comparison in Table 3.

The grey shaded discharge concentrations in Table 3 are those used in the EVF calculation. Theoretically, the mean values could be used in the EVF calculation with the annual average EQS, however, this assumes that the mean discharge is an annual average. As the discharge concentration is determined by the dewatering process it is not appropriate to assume a random process contributing to the discharge concentration, and the discharge is intended to occur over several years. There could, for instance, be many months when values above the mean are present in the chemical discharge. As a precautionary approach, the 95<sup>th</sup> percentile discharge concentrations have been used for calculating the EVF values.

The Environment Agency considered the datasets submitted for the assessment of construction discharges in December 2017. They confirmed that most of the values used within the screening were conservative, however a few (shown in bold and underlined Table 3) had slightly higher values. This was not considered to be an issue as zinc was still the substance which had the highest EQS exceedance, and therefore was still the 'contaminant of concern' which was most relevant to be carried forward to the modelling stages. The slight discrepancies between the Zinc 95<sup>th</sup> percentile values were also not considered to be an issue because it was not expected that this slight increase (1.37%) to the input data would vary the outcome results of the modelling assessments.

As the suspended sediment concentration at a given location directly affects light penetration and the potential for increased phytoplankton growth, the reference concentration of dissolved inorganic nitrogen (DIN) for TraC waters for the Good/Moderate boundary also references the suspended sediment concentration. The average turbidity concentration measured at Hinkley Point (Amec, 2009) was 214 NTU. This defines Hinkley as turbid with associated 99<sup>th</sup> percentile winter DIN values for transitional and coastal waters of 2520  $\mu\text{g l}^{-1}$  and 3780  $\mu\text{g l}^{-1}$  thresholds for Good and Moderate respectively (Water Framework Directive Standards and Classification Directions, 2015, Appendix B). It should be noted that a portion of the DIN in groundwater is nitrate/nitrite which may not all readily convert to ammonia, but total conversion to ammonia was assumed to ensure that the assessment made was conservative.

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Table 3. Groundwater contaminants and concentrations likely to be present in the construction dewatering discharge and comparison to EQS for three cases. AA refers annual average concentration and MAC refers to the maximum allowable concentration. EVF (m<sup>3</sup> s<sup>-1</sup>) has been derived using 95<sup>th</sup> percentile discharge concentrations and the AA EQS (except for mercury where the MAC EQS has been used). The shaded values indicate those used in the screening test assessment. These data are based on Environment Agency calculation from NNB GenCo data sources. Underlined updated values had non-significant increases relative to original Cefas calculations.

Contaminant	Assessed discharged concentration µg l <sup>-1</sup>		Saltwater AA EQS µg l <sup>-1</sup>	Saltwater MAC EQS (as 95%ile) (µg l <sup>-1</sup> )	Back-ground concentration (µg l <sup>-1</sup> )	(EVF) Case A and Case D	EVF Case C	TraC Water test 5 EVF < 3.0 Pass/Fail
	Mean	95%ile (used in EA Screening test)						
Un-ionised ammonia (N)	258.75	123.5	21	-	<u>4.6</u>	<u>0.15</u>	<u>0.352</u>	<u>Pass</u>
DIN groundwater	1860.92	4073	2520 <sup>1</sup>		1050	0.06	0.129	Pass
Cyanide	0.025	50	1	-	0	1.00	2.34	Pass
Total cadmium	0.09	0.460	0.2	-	<u>0</u>	<u>0.05</u>	<u>0.12</u>	<u>Pass</u>
Total chromium	4.58	24	0.6 <sup>2</sup>	32	0.02	0.83	1.93	Pass
Total lead	0.85	3	1.3	14	0.02	0.05	0.11	Pass
Total copper	31.7	221	4.76	-	3.95	<u>5.46</u>	<u>12.17</u>	<u>Fail</u>
Total zinc	427.2	1642.15	6.8	-	3.035	<u>8.72</u>	<u>20.37</u>	<u>Fail</u>
Total mercury	0.2	0.49	-	0.07 <sup>3</sup>	0.02	0.2	0.46	Pass
DIN Sewage sources		20,000 <sup>4</sup>	2520		1050	0.19	0.41	Pass

<sup>1</sup> 99<sup>th</sup> percentile (180 µmol) standard for period 1<sup>st</sup> November – 28<sup>th</sup> February for dissolved inorganic nitrogen for Good status, Appendix B, Table 17.

<sup>2</sup> The EQS in seawater is set for dissolved hexavalent chromium only but this is dissolved total chromium (all species).

<sup>3</sup> The EQS for mercury is only set as a 95<sup>th</sup> percentile.

<sup>4</sup> A max value not 95<sup>th</sup> percentile, ammoniacal nitrogen as a proxy for total nitrogen from sewage treatment (µg l<sup>-1</sup>) as other contributions e.g. NO<sub>2</sub>, NO<sub>3</sub> are expected to be small.

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The Effective Volume Flux of the discharge (EVF) is defined as:

$$EVF = (EFR \times RC) / (EQS - BC) \text{ m}^3 \text{ s}^{-1}$$

Where:

*EFR* = the effluent discharge rate ( $\text{m}^3 \text{ s}^{-1}$ )

*RC* = release concentration of the priority substance of concern ( $\mu\text{g l}^{-1}$ )

*EQS* = EQS (AA) of the substance of concern ( $\mu\text{g l}^{-1}$ )

*BC* = mean background concentration at the discharge location ( $\mu\text{g l}^{-1}$ )

For Case A and Case D, which together represent most of the total tunnelling time, both copper and zinc fail the screening tests. During peak ground water load (Case C) chromium also fails this test, although only marginally and for a period of only approximately 8 weeks when the flow is predicted to be at a maximum. If the annual average is used, only zinc would be of potential concern (the copper EVF is substantially below the threshold). As zinc is the substance of greatest exceedance then this report considers this discharge further, with detailed modelling in a real-world simulation described in section 3. Calculation of EVF values as shown in Table 3 are provided in more detail in Appendix C, Table 22..

**2.1 Total loads for Cadmium and Mercury.**

There are specific requirements for annual loads of cadmium and mercury compounds. Figure 3 shows that the criteria not to exceed 5kg and 1kg (respectively) are met, for both cadmium and mercury respectively.

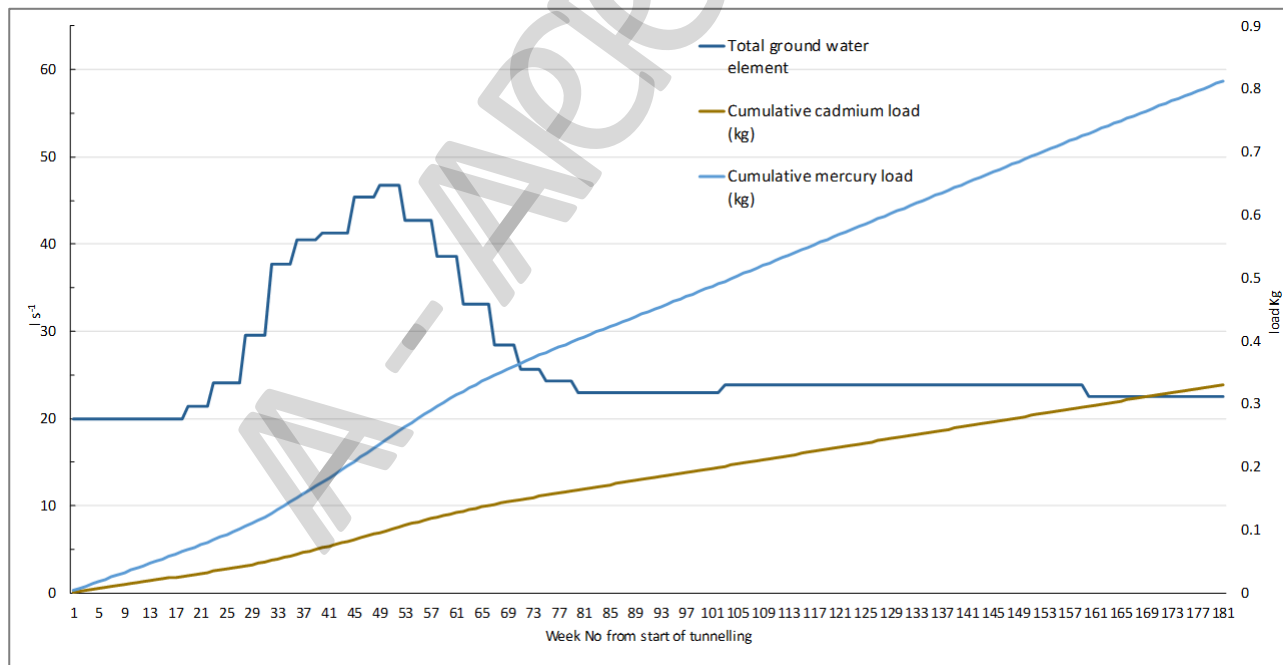


Figure 3. Three-year timeline of groundwater discharge ( $\text{l s}^{-1}$  left axis) and resulting cumulative metal load for Mercury and Cadmium (kg right axis).

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## 3 Discharge Assessment Methodology

### 3.1 Modelling approach.

The release and mixing of zinc in the construction discharge was modelled using the validated Hinkley Point 25 m resolution GETM model. This is a 3D hydrodynamic model with an inbuilt passive tracer to represent zinc. As a worst case, it was assumed that there was no loss of dissolved zinc due to sediment absorption or biological uptake. Using these assumptions allowed concentrations to be scaled, as the modelled concentration was simply a function of dilution. The model setup, calibration and validation are described in British Energy Estuarine & Marine Studies (BEEMS) Technical Report TR267 Edition 2. As with the 100m resolution Hinkley Point GETM model (BEEMS Technical Report TR177) the surface is forced with reanalysed data from a meteorological model (ERA40 interim from ECMWF). The boundary conditions were forced by a broader 3D GETM domain, described in BEEMS Technical Report TR177.

The construction discharge characteristics are shown in Table 2. The discharge outfall is attached to a jetty pile and located approximately 1 m above the seabed (approximately 2 m below lowest astronomical tide (LAT)). CORMIX modelling (shown in Appendix D of this report) indicates that the plume will be buoyant and form a surface pool (or pond) at slack water which will become increasingly elongated as the tidal flow increases, forming a long thin streak at peak tidal flow. CORMIX is unable to replicate many of the features simulated by the GETM model, and GETM is therefore a better model to use away from the near field (further than 10s of metres from the outfall). Specifically, GETM can replicate wind driven behaviour and has precise bathymetry so that interactions with the tidal flow (e.g. eddies) are well replicated. Neither the CORMIX nor the GETM model includes the effects of waves which enhance vertical mixing and increase dilution. The modelling predictions of plume areas above the EQS are therefore conservative: the actual discharge will be subject to more mixing and dilution (caused by wave action) than the models are able to replicate and so the actual concentrations in the environment will be lower than those predicted.

The mean background concentration of zinc in the environment is  $3.03 \mu\text{g l}^{-1}$  (See Appendix A) whilst the EQS is  $6.8 \mu\text{g l}^{-1}$ . When comparing the model results against the EQS, an adjusted value of  $3.77 \mu\text{g l}^{-1}$  was used as a threshold to account for the background concentration of zinc, calculated by simply subtracting the background concentration from the EQS concentration.

### 3.2 Discussion of initial mixing conditions

The greatest challenge in modelling a small volume, buoyant flow is to sufficiently replicate the initial mixing whilst retaining the ability to simulate real wind and bathymetric features.

In this study, the GETM model domain used a discrete grid with dimensions of 25 m by 25 m and 15 vertical layers in a sigma co-ordinate system in which the layer thickness changed with water depth. The discharge flow for Case D ( $25 \text{ l s}^{-1}$ ) was small compared with the total volume in the model grid cell, so to avoid excessive initial dilution, the discharge was made into the model surface layer, which is consistent with the results of the near field CORMIX modelling of a buoyant plume.

It should be noted that in a buoyant plume with a discharge in an offshore location, unless mixing occurs, there will be no impact on seabed features. Consideration of the tidal cycle is useful in understanding the likely modes of impact. When the flood tide is at its strongest (with flow to the east), the discharge plume will initially be buoyant, and will then be advected in a narrow surface streak and mixed down. As mixing occurs the concentration within the streak will rapidly drop. At high water, around slack tide, a pool of the discharged water will form at the surface which will be advected westwards as the ebb tide increases. As the tidal range is large in the Severn Estuary, this surface layer of water will be separated vertically from the bed, and the discharged water will not meet sensitive features such as *Sabellaria* or *Corallina* patches. As the tidal flow velocity increases, the strong tidal flows and rough topography of the Severn Estuary generate



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strong vertical mixing which ensures a large reduction in the concentrations of contaminants in the discharged water.

The period around low water slack tide is the time of greatest *potential* concern. It would be expected that the slack water period at low tide would also result in ponding, and that this ponded water would then be advected as the flood tide increases. As the water depth at this time is low, it has the *potential* for interaction with the bed and to be advected onto the sensitive areas of the rock platform. As the flow increases after low water slack tide, the water depth increases and the potential for interaction with the bed at concentrations of concern decreases. It is therefore the period around low water slack tide that needs the best simulation from the model. The CORMIX model system was used to understand the initial mixing condition (Appendix D). It indicated that at 25m distance from the discharge the dilution was approximately 22-fold. CORMIX modelling also showed that the plume rapidly comes to the surface (because of its buoyancy) so that only a very small footprint of exposure (radius of up to 5 m or 78 m<sup>2</sup>) occurs at the bed.

The discharge varies with time. During Case A and Case D it is small compared to the model grid size (approximately 20 – 25 l s<sup>-1</sup> when considering groundwater alone) and therefore initial dilution due to mixing in the model is potentially overestimated. This was overcome by simulating discharge into the upper grid cell of the model only, successfully replicating the near-field mixing suggested by the CORMIX simulation. At low water slack tide, the vertical cell size at the surface in the GETM model at the outfall location is 0.2 m and the total volume in the upper grid cell approximately 125 m<sup>3</sup>. During Case B and Case C conditions the initial mixing condition is less of a concern where volumes of discharge peak at 63 l s<sup>-1</sup>.

As the Cormix modelling suggested that initial dilution was 22-fold at a distance of 25 m from the discharge (i.e. the same size as a single grid cell) then the discharge volume of 20 l s<sup>-1</sup> met this dilution criterion within 284 seconds or approximately 5 minutes. For the larger Case C discharge, 22-fold dilution was achieved in 95 seconds.

The period of near slack water (but not zero velocity) in the model is typically around 30 minutes, much longer than the worst case 5 minutes given above, thus the GETM model will correctly represent the concentrations of zinc around low water and thus replicate the low water ponding situation well. The ponded water is then advected by the tides. The model is therefore able to replicate the period of concern (low water slack tide) accurately. The advection of the ponded water is shown in Appendix E.

The maximum concentration at the point of discharge (within 25 m) may be underestimated, but away from that grid cell (25 m by 25 m) the concentrations are well represented.

While the tide advects water along the coast, with a small cross-shore component, it is the wind direction that gives the greatest variability in the cross-shore component and possible impact on to the shore and sensitive habitat.

### 3.3 Analysis of wind scenarios.

The tide will move the plume along the coast, but it is expected that the winds from the northern quadrant will have the greatest potential to push the plume onto the intertidal areas where *Corallina officinalis* and *Sabellaria* sp. are found. The year 2008 has been used as the representative year for all the Hinkley Point C thermal and chemical modelling (BEEMS Technical Report TR177) and hydrodynamic data collected in that year was used to validate the models. To maintain consistency with previous modelling work, 2008 was, therefore used as the modelling year in this study. Analysis of the wind speed and direction for the year 2008 (see Figure 4) shows that the month of November exhibited both the highest percentage of days with northerly winds and highest percentage of days with average wind speed in the 5 -15 m s<sup>-1</sup> range from N and NW directions. Choosing the month of November to perform the simulation ensures the worst-case scenario for impact and a realistic variability in weather forcing.

The current operational Hinkley Point B discharge was included in the simulation (equivalent to Run A in BEEMS Technical Report TR267 Ed.2) for the period of 21/10/2008 to 30/10/2008 to spin up the





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**3.4 Tunnelling materials and chemicals.**

Tunnel boring machines (TBMs) will be used to excavate two tunnels required for the cooling water intakes and one for the cooling water discharge. Tunnels will be constructed in sections or rings. One ring is equivalent to 1.5 metres of tunnel length and an estimated maximum of 24 rings per intake tunnel per day and 16 rings for the outfall tunnel per day will be completed.

By far the largest volume of wastewater produced by tunnelling operations comprises groundwater from the deepest excavations completed during early stages of the SCL works. This groundwater discharge is considered alongside the main dewatering discharge, as it will be of similar composition and therefore could also contain levels of zinc of potential concern. There are also much smaller quantities of water which contain chemicals from the tunnelling operations, and those chemicals are considered here.

To obtain optimum performance with TBMs, ground-conditioning chemicals are used at the cutter head. These chemicals improve ground properties for cutting and for the initial removal using a screw conveyor. During the subsequent transport of removed materials from the cutting face on a conveyor belt, some residual fluids associated with the conditioned ground material will leach out and be captured in the pit at the bottom of the tunnel. These fluids, along with small amounts of natural groundwater from the cutting face, will then be pumped out and discharged at the jetty location.

Chemical use in tunnelling is associated with three broad functions which are:

- (i) Fuelling and lubrication of the TBM
- (ii) TBM protection greases / sealants
- (iii) Ground conditioning

Table 4 provides a description of these main chemical applications in tunnelling, the most likely chemical types and their properties and indicates the fate of residual wastes.

Table 4. General chemical use, treatment and disposal associated with tunnelling operations

Chemical function	Chemical type	Description of use	Disposal route
Fuelling and lubrication	Hydraulic oils	Various uses on TBM	Spills when filling or seal leaks treated with absorbent granules, granules disposed of by licenced waste disposal
	Other oils	Various uses on TBM	As above
	Diesel	Backup generators	As above
Sealant	Grease	Approx. 2.5 kg per ring used in positive loss protection	Returned to muck bay as contained within excavated spoil. Remainder in barrel returned to surface, washed and waste disposed of by licenced waste disposal
	Tail skin grease	1.5 kg m <sup>2</sup> left on tunnel wall lining	In tunnel encased on outer surface of ring. Remainder in barrel returned to surface, washed and waste disposed of by licenced waste disposal
Ground conditioning	Various	circa 50l per ring if system running at 100 %	Spoil returned to muck bay, residual fluids lost to pit bottom are recovered and pumped to jetty

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Table 5. Example products for use in ground conditioning, their properties and percentage of key component substances and associated Predicted No Effect Concentrations for each substance or surrogate value for a group of similar substances. Details of calculations in Appendix C, Table 23.

Chemical function	Product	Main active substance(s)	Active mass (kg) per day assuming 100% use for 1 intake tunnel and 1 outfall tunnel.	Predicted no effect concentration (PNEC) for aquatic environment ( $\mu\text{g l}^{-1}$ )
Anti-clogging agent	BASF Rheosoil 143	Sodium lauryl ether sulfate (<30%)	68.5 kg <sup>1</sup> (based on 40 rings per day)	40 <sup>2</sup>
Soil conditioning-additive	CLB F5 M	2,4-Pentanediol, 2-methyl- ( $\leq 10\%$ )	22.8kg <sup>1</sup> total (based on 40 rings per day).	4300 <sup>3</sup>
		Alcohols, C10-16, ethoxylated, sulfates, sodium salts – ( $\leq 10\%$ )		35 <sup>2</sup>
		Mono-C10-16-alkyl, Sodium sulfate ( $\leq 10\%$ )		4.5 <sup>4</sup>

<sup>1</sup> This value takes account of substance density (1.05), % active substance, and assumes 90% associated to spoil (see later discussion); <sup>2</sup>see Table 15 HERA 2004; <sup>3</sup>see SIDS, 2001, <sup>4</sup>see Table 13 HERA, 2002

The PNEC values shown in Table 5 for each active substance are either taken directly from relevant risk assessment reports i.e. for 2-methyl-2-4 pentanediol (SIDS initial assessment report, 2001), or use the lowest PNEC from a substance group assessment i.e. PNEC values calculated for other alcohol ethoxylate sulphates are derived for representative carbon chain length substance or worst case if not known (Table 15 in HERA, 2004,) and for mono-C10-16-alkyl sodium sulphate (Table 13 HERA 2002). In the case of mono-C10-16-alkyl sodium sulphate we assessed the C14 toxicity (as this generated the most conservative PNEC) whereas the substance will be composed of a range of carbon chain lengths.

**3.4.1 Screening methodology assessment.**

Theoretically, a maximum of 24 rings could be installed per intake tunnel per day and 16 rings for the outfall tunnel. There is overlap in time of construction between the HPC cooling water Intake 1 and the cooling water outfall and between the outfall and Intake 2. The current drilling programme (Figure 1) shows a short overlap between the drilling of all 3 tunnels. However, for operational reasons including power availability, all three TBMs will not be operating at full capacity simultaneously. Using a realistic total construction estimate of 40 rings per day gives a total mass of 68.5 kg per day for BASF Rheosoil (Table 5). This assumes that overall, 10% of the active substance of the product used leaches out of the soil and is then discharged via the jetty. This is considered a conservative estimate of the level of adsorption to the mineral material removed from the tunnel for each ring.

Various literature sources show that at surfactant solution concentrations of several hundred mg l<sup>-1</sup> there is adsorption of between 3 – 19 mg of anionic surfactants per gram of mineral (i.e. kaolinite) associated with the solution (Lv *et al.*, 2011, Yekeen *et al.*, 2017). Based on the predicted surfactant concentration in the

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conditioning fluids and the large quantity of mineral material removed per ring it is likely that all but a few percent of surfactant will be adsorbed to the mineral waste but a conservative 90% is assumed here. Case D is the most likely time when peak ring installation rates (and hence peak usage of soil conditioning chemicals) will occur.

Table 6. Environment Agency screening assessment of surfactant components of products. Example chemicals for use in ground conditioning, their properties and fate (for details of calculations see Appendix C, Table 24).

Conditioning product	Estimated Discharge concentration mg l <sup>-1</sup> of active substance. Case D	Saltwater AA EQS <sup>1</sup> µg l <sup>-1</sup>	Background concentration µg l <sup>-1</sup>	Effective volume flux (Case D) Total flow 40 l/s (m <sup>3</sup> s <sup>-1</sup> )	TraC Water test 5 EVF < 3.0 (Pass/Fail)
BASF Rheosoil 143	19.8	40	0	19.80	Fail
CLB F5 M Ethoxylated sulphates	6.6	35	0	7.54	Fail
CLB F5 M Mono- alkyl sodium sulphate	6.6	4.5	0	58.67	Fail

<sup>1</sup> these EQS values derived from HERA 2004 for both BASF Rheosoil 143 (sodium lauryl ether sulfate) and for CLB 5M (Alcohols, C10-16, ethoxylated, sulfates, sodium salts (≤10%) Mono-C10-16-alkyl, Sodium sulfate (≤10%))

As these chemicals fail the TRAC 5 screening test they are considered further in the next section.

**3.5 Assessment of construction and cold commissioning inputs.**

Edition 6 of this report considered the construction discharge inputs. During the latter phase of the construction period (best represented by Case D construction discharge inputs) cold commissioning of the reactors and associated pipework will take place. During this process, a range of tests will be conducted, and conditioning will be undertaken with demineralised water (potable water may be used in some cases) and various chemical additives. The discharge of commissioning wastewater will contribute to intermittent discharges of commissioning chemicals and their breakdown products. During cold commissioning there is no available cooling water system therefore discharge is planned via the jetty. The commissioning discharge has been assessed for inputs of hydrazine using a discharge rate of 83.3 l s<sup>-1</sup> and this assessment is described in BEEMS technical report TR445. Here the breakdown products of that hydrazine and other commissioning chemicals are assessed in combination with construction inputs for Case D (see Table 1).

Testing of the primary and secondary circuits requires them to be filled and flushed several times each with demineralised water and treatment chemicals. As a precautionary assessment the maximum daily discharge volume is taken to be 1500 m<sup>3</sup>d<sup>-1</sup>, equivalent to the contents of the two 750 m<sup>3</sup> HXA tanks that serve this waste stream. The discharge rate is expected to be 37 l s<sup>-1</sup> per tank or 70 l s<sup>-1</sup> for discharge of both. The discharge is expected to last for a period of 5.63 hours. The modelled discharge rate is lower than that modelled for the hydrazine discharge modelling which used a rate of 83.3 l s<sup>-1</sup> over a 5 hour period (BEEMS TR445). The higher discharge rate was based on information available at the time of modelling and the lower discharge rate is considered more accurate for the HXA tanks. In terms of the hydrazine modelling for commissioning, as the discharge concentration would be the same for either discharge rate, the higher rate of 83.3 l s<sup>-1</sup> is considered to provide a slightly more conservative assessment. However, for the hydrazine and other commissioning chemical breakdown products modelling the 70 l s<sup>-1</sup> has been used.

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# 4 Results

## 4.1 Modelling of the discharge for Zinc in relation to *Corallina*

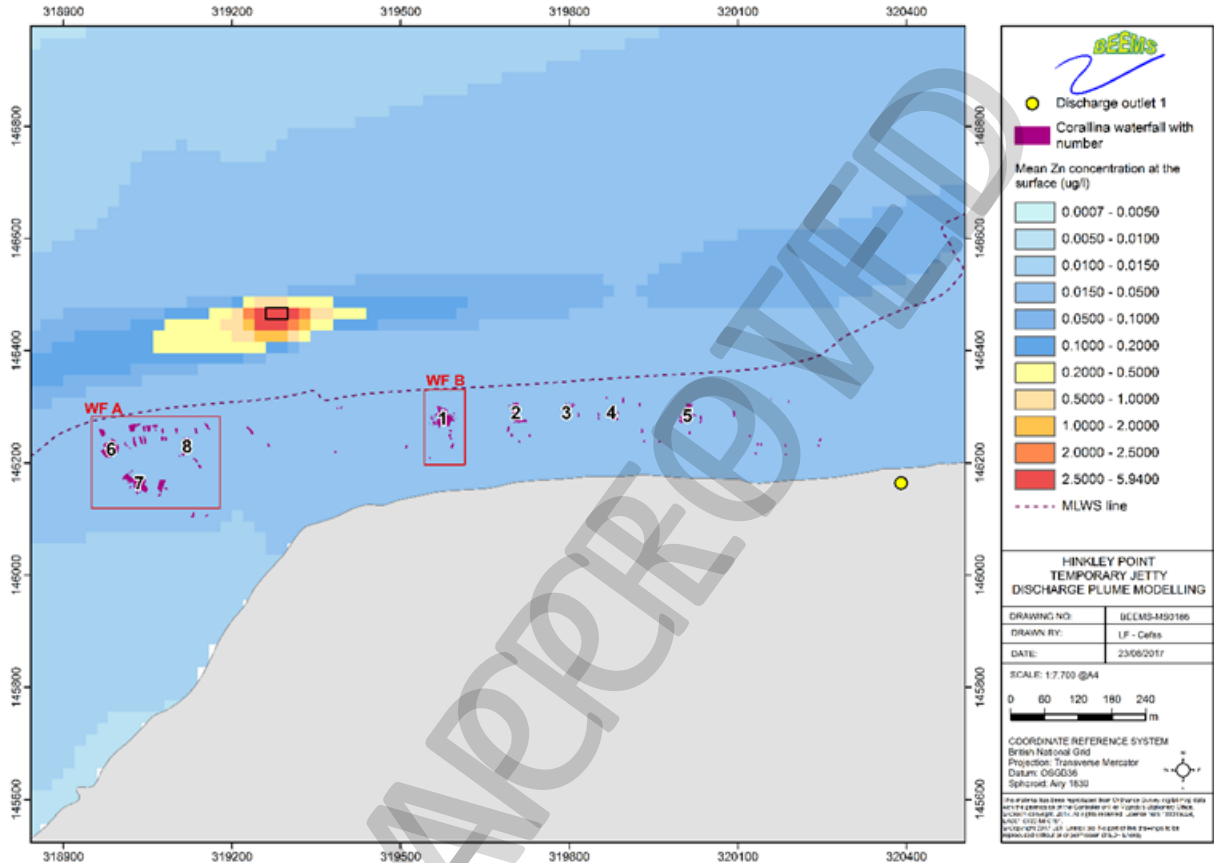


Figure 5. Distribution of average (monthly mean) surface concentrations of zinc for Case D in relation to the *Corallina* features. The EQS is exceeded for the small area by the discharge itself. Features labelled WF are the *Corallina* waterfalls referred to in the HPC jetty monitoring reports (BEEMS TR256). The comparative EQS is 3.77  $\mu\text{g l}^{-1}$ .

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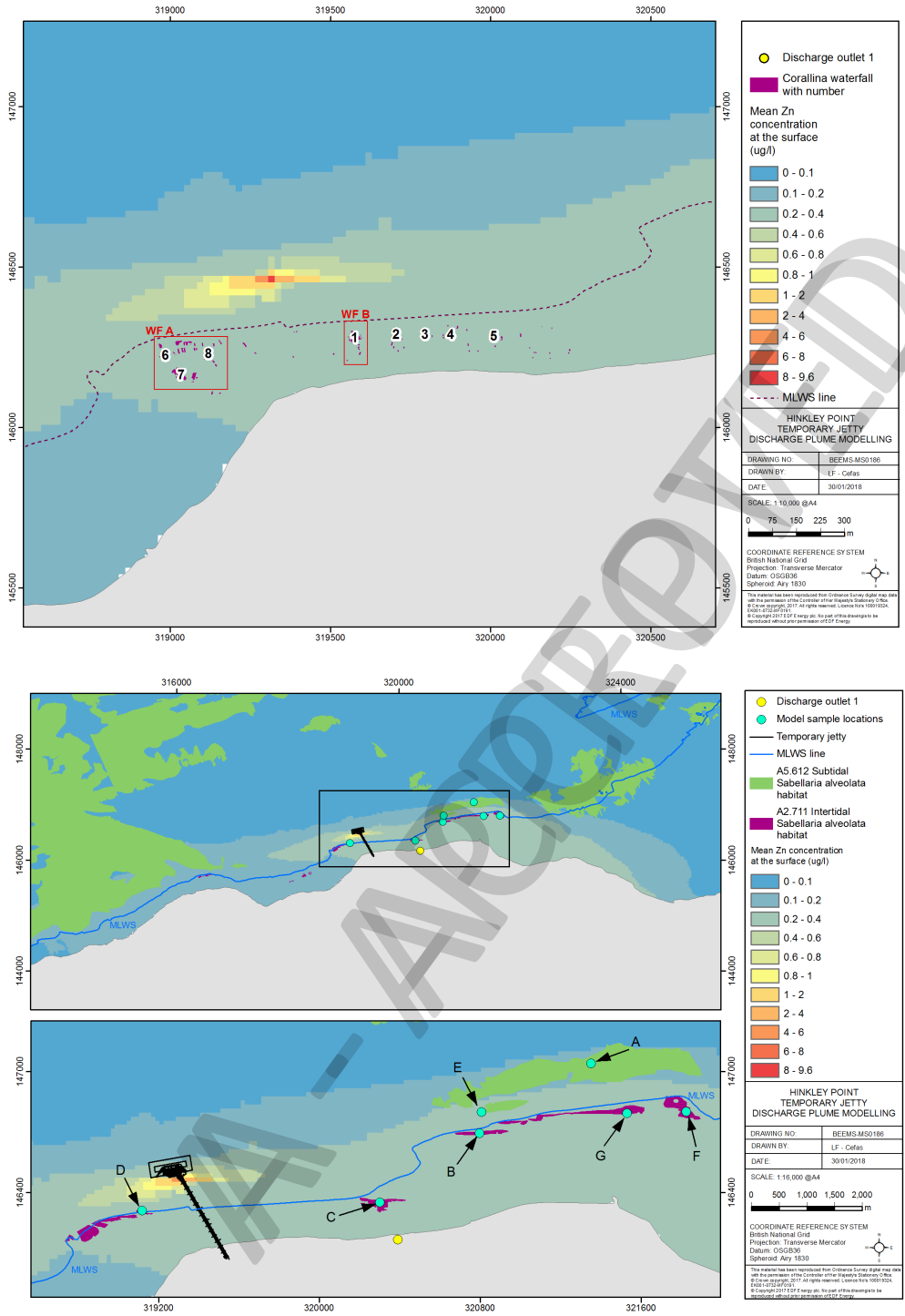


Figure 6. Distribution of average (monthly mean) surface concentrations of zinc for Case C in relation to the *Corallina* features. The EQS is exceeded for the small area by the discharge itself. Features labelled WF are the *Corallina* waterfalls referred to in the HPC jetty monitoring report (BEEMS TR256). The comparative EQS is 3.77  $\mu\text{g l}^{-1}$ .

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The predicted exposure of *Corallina* to zinc for Case D and Case C are shown Figure 5 and Figure 6 respectively, together with locations where *Corallina* features are present. For zinc, the EQS is defined as an annual average. As described in Section 3.1, the modelling is performed above the background, and all tables and plots show the surplus concentration above background and refer to the EQS concentration above background levels. Zinc has a background concentration of  $3.03 \mu\text{g l}^{-1}$  meaning that the threshold value for exceeding the EQS is  $3.77 \mu\text{g l}^{-1}$  (Table 3). For Case C, the mean seabed concentration at each *Corallina* position increased by approximately 1% of the EQS (Table 7).

Importantly, dilution is significant across the main tidal excursion axis, i.e. there is a very rapid reduction in concentration to the north and south from the discharge plume.

The areas above the EQS for the surface are 0.125 Ha for Case D and 0.3 Ha for Case C.

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Table 7. Zinc concentration ( $\mu\text{g l}^{-1}$ ) at *Corallina* feature locations (Figure 5) for total zinc discharges corresponding to  $22 \text{ l s}^{-1}$  at  $1620 \mu\text{g l}^{-1}$  Zn (Case D) and  $46 \text{ l s}^{-1}$  at  $1620 \mu\text{g l}^{-1}$  Zn (Case C). The threshold for discharges to exceed the EQS is  $3.77 \mu\text{g l}^{-1}$ , based on the background concentration.

Feature No. (see Figure 5)	OSGB Easting	OSGB Northing	Latitude N ( $^{\circ}$ )	Longitude E ( $^{\circ}$ )	Mean Case D ( $\mu\text{g l}^{-1}$ )		Max Case D ( $\mu\text{g l}^{-1}$ )		Mean Case C ( $\mu\text{g l}^{-1}$ )		Max Case C ( $\mu\text{g l}^{-1}$ )	
					Surface	Bed	Surface	Bed	Surface	Bed	Surface	Bed
1	319575	146280	51.2100	3.1527	0.10	0.10	0.37	0.37	0.24	0.24	0.87	0.87
2	319705	146290	51.2101	3.1509	0.10	0.10	0.64	0.64	0.24	0.24	1.50	1.50
3	319795	146290	51.2102	3.1496	0.11	0.10	0.61	0.61	0.26	0.24	1.44	1.15
4	319875	146290	51.2102	3.1484	0.12	0.12	0.39	0.39	0.28	0.28	0.92	0.92
5	320010	146285	51.2101	3.1465	0.12	0.11	0.49	0.49	0.29	0.26	1.15	1.15
6	318985	146225	51.2095	3.1612	0.10	0.10	0.59	0.59	0.24	0.22	1.38	1.38
7	319035	146165	51.2089	3.1604	0.11	0.10	0.29	0.29	0.25	0.23	0.69	0.69
8	319120	146230	51.2095	3.1592	0.11	0.10	0.29	0.29	0.25	0.23	0.69	0.69

Note, there is no exceedance of the EQS. Feature 5 has the highest mean concentration but feature 2 the highest maximum bed concentrations, however maximums are significantly below the EQS.

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**4.2 Modelling of the discharge for Zinc in relation to *Sabellaria***

On a larger spatial scale than the *Corallina* features, there are intertidal and subtidal patches of *Sabellaria* reef which may be exposed to the total discharge. The EQS for zinc is defined as a mean value and there is no intersection of discharge water above the annual average EQS (adjusted to 3.77 µg l<sup>-1</sup>) with patches of *Sabellaria* (Figure 7 to Figure 10). The concentrations of zinc at *Sabellaria* features are summarised in Table 8. In all cases the mean EQS is not exceeded and the 95<sup>th</sup> percentile exposure is below the annual average EQS.

Table 8. Zinc concentrations at *Sabellaria* patches A and E (subtidal) and B, C, D, F and G (intertidal). For locations see Figure 8.

Feature	Mean seabed µg l <sup>-1</sup>		Seabed µg l <sup>-1</sup> (95 <sup>th</sup> percentile)	
	Case D	Case C	Case D	Case C
Subtidal <i>Sabellaria</i> A (Easting 321350 Northing 147040)	0.03	0.14	0.09	0.20
Intertidal <i>Sabellaria</i> B (Easting 320800 Northing 146694)	0.10	0.24	0.23	0.54
Intertidal <i>Sabellaria</i> C (Easting 320300 Northing 146351)	0.10	0.24	0.20	0.47
Intertidal <i>Sabellaria</i> D (Easting 319118 Northing 16309)	0.10	0.23	0.22	0.53
Subtidal <i>Sabellaria</i> E (Easting 320800 Northing 146800)	0.10	0.22	0.28	0.65
Intertidal <i>Sabellaria</i> F (Easting 321824 Northing 146800)	0.11	0.25	0.23	0.55
Intertidal <i>Sabellaria</i> G (Easting 321529 Northing 146793)	0.11	0.27	0.24	0.56

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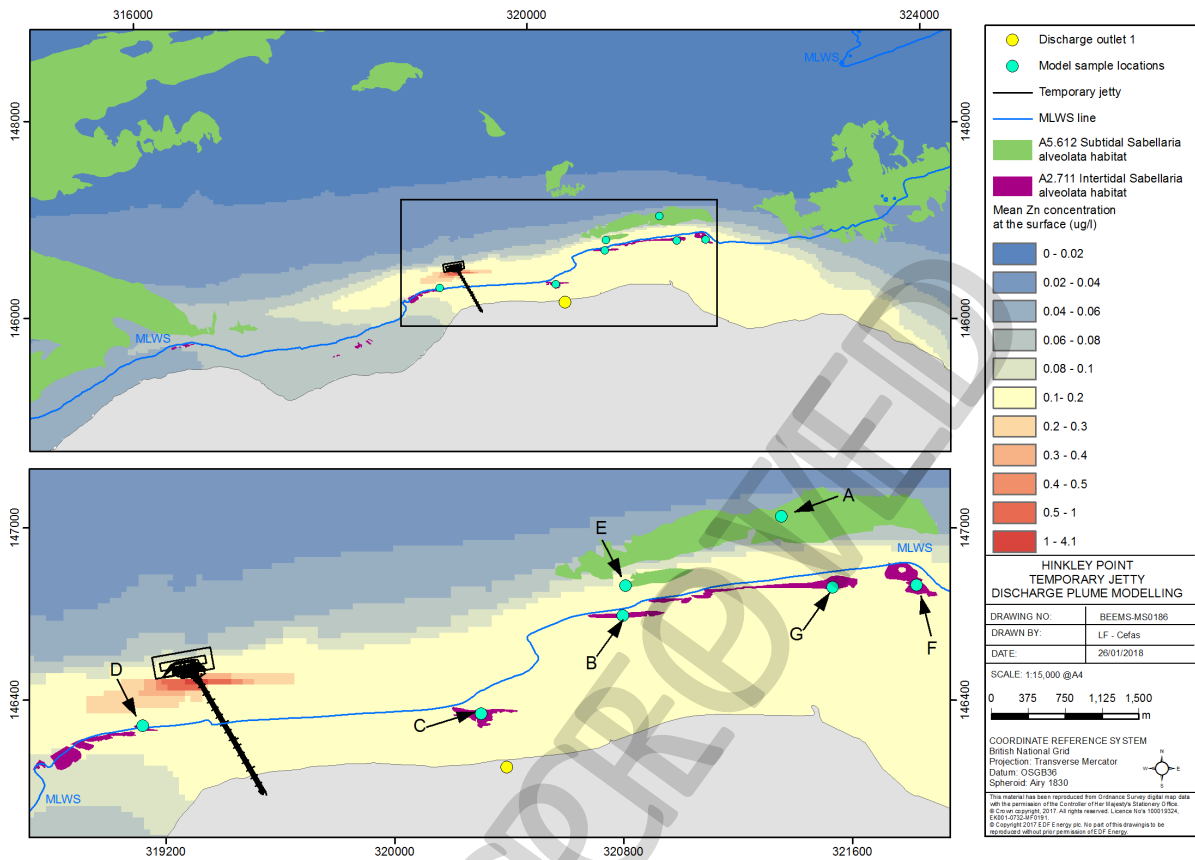


Figure 7. Mean surface discharge concentration of zinc in  $\mu\text{g l}^{-1}$  for case D with the location of *Sabellaria* shown (upper), and subtidal *Sabellaria* patch A and intertidal *Sabellaria* patch B, C, D, F and G marked. The EQS for zinc is  $3.77 \mu\text{g l}^{-1}$  above background concentration. The cyan dots mark the *Sabellaria* positions that are listed in Table 8.

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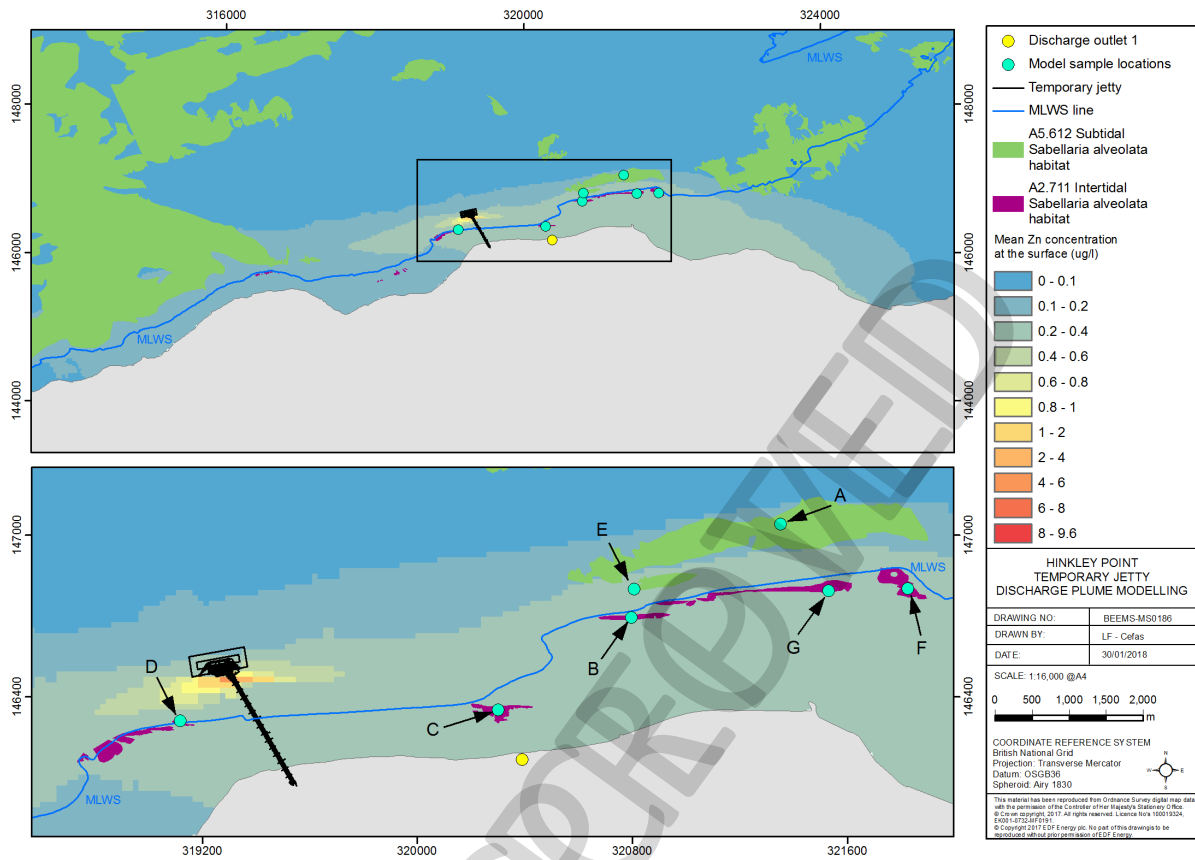


Figure 8. Mean surface discharge concentration of zinc in  $\mu\text{g l}^{-1}$  for case C with the location of *Sabellaria* shown (upper), and subtidal *Sabellaria* patches A and E, intertidal *Sabellaria* patches B, C, D F and G. The EQS for zinc is  $3.77 \mu\text{g l}^{-1}$  above background concentration. The cyan dots mark the *Sabellaria* positions that are listed in Table 8.



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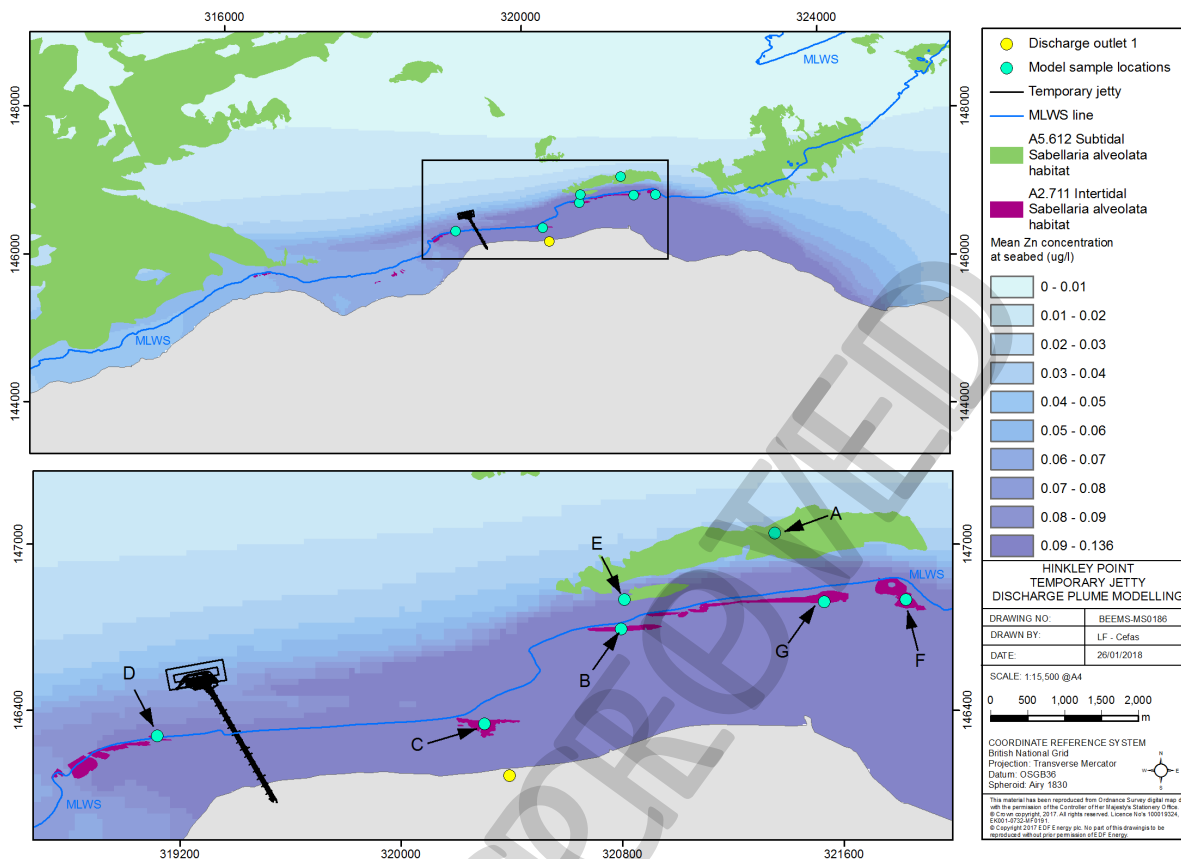


Figure 9. Mean bed discharge concentration of zinc in  $\mu\text{g l}^{-1}$  for case D with the location of *Sabellaria* shown (upper), and subtidal *Sabellaria* patches A and E, and intertidal *Sabellaria* patches B, C, D, G, F. The EQS for zinc is  $3.77 \mu\text{g l}^{-1}$  above background concentration. The cyan dots mark the *Sabellaria* positions that are listed in Table 8.

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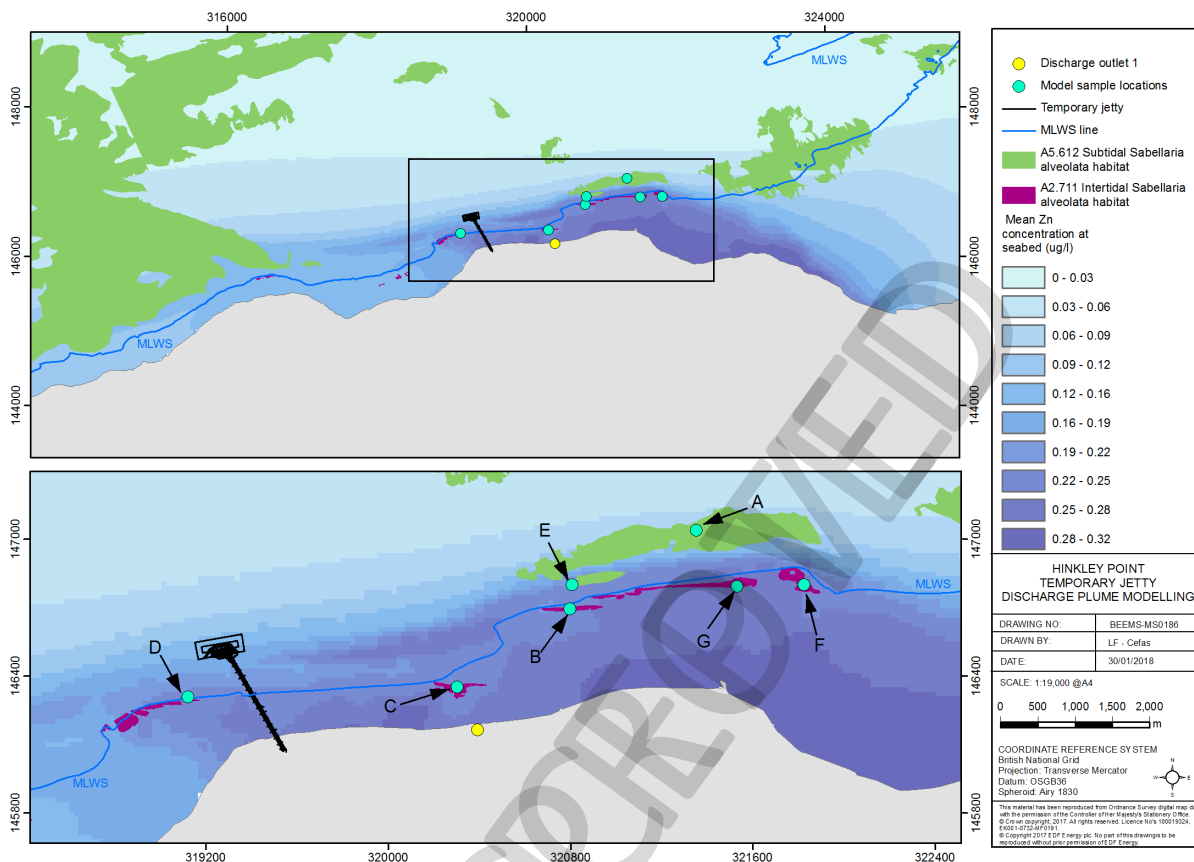


Figure 10. Mean bed discharge concentration of zinc in  $\mu\text{g l}^{-1}$  for Case C with the location of *Sabellaria* shown (upper), and subtidal *Sabellaria* patches A and E, and intertidal *Sabellaria* patches B, C, D, E, F and G marked. The EQS for zinc is  $3.77 \mu\text{g l}^{-1}$  above background concentration. The cyan dots mark the *Sabellaria* positions that are listed in Table 8.

### 4.3 Modelling of conditioning chemical BASF Rheosol 143 in relation to *Sabellaria*.

Having failed the screening test, this compound is modelled in an identical way to zinc. As the modelling of zinc does not assume any substance decay, and predicted concentrations come only from dilution, these results have been scaled from the model simulations undertaken for zinc by using a multiplier to correctly simulate the mass of discharged chemical. The exact chemical to be used may change depending on the tunnelling machine employed and substrata encountered. This modelling is included to show the likely spatial extent of a discharge of  $40 \text{ l s}^{-1}$  at concentration of  $19.83 \text{ mg l}^{-1}$  with an EQS of  $40 \mu\text{g l}^{-1}$ . The tunnelling operations which use this chemical are likely to occur during the Case D period ( $40 \text{ l s}^{-1}$ ) however the results are insensitive to this flow volume as it is the total mass of material that is discharged that is the primary consideration.

The modelling results for BASF Rheosol 143 are shown in Figure 11 and Figure 12 which show that there is no exceedance of mean PNEC (surrogate EQS) at the bed; there is a small area at the surface where the EQS is exceeded. The 95<sup>th</sup> percentile concentrations at the bed are shown in Figure 13.

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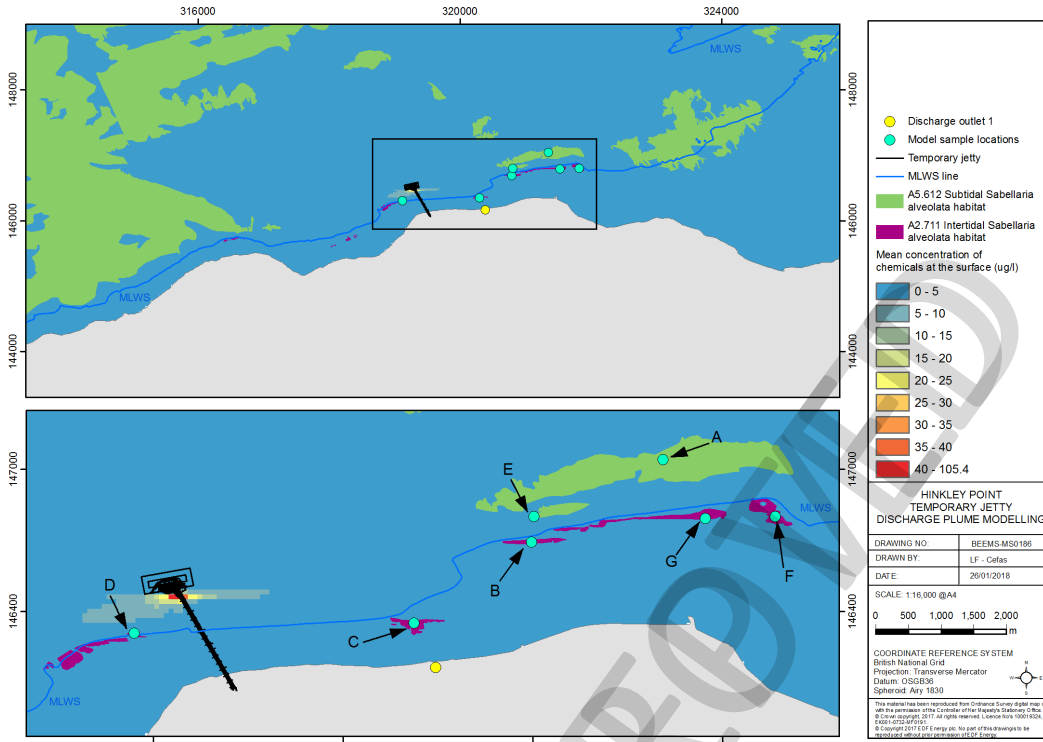


Figure 11. Mean surface concentration of BASF Rheosoil 143 in  $\mu\text{g l}^{-1}$ . The PNEC (surrogate EQS) is  $40 \mu\text{g l}^{-1}$ . Subtidal *Sabellaria* patches A and E and intertidal patches B, C, D, E, F and G are marked.

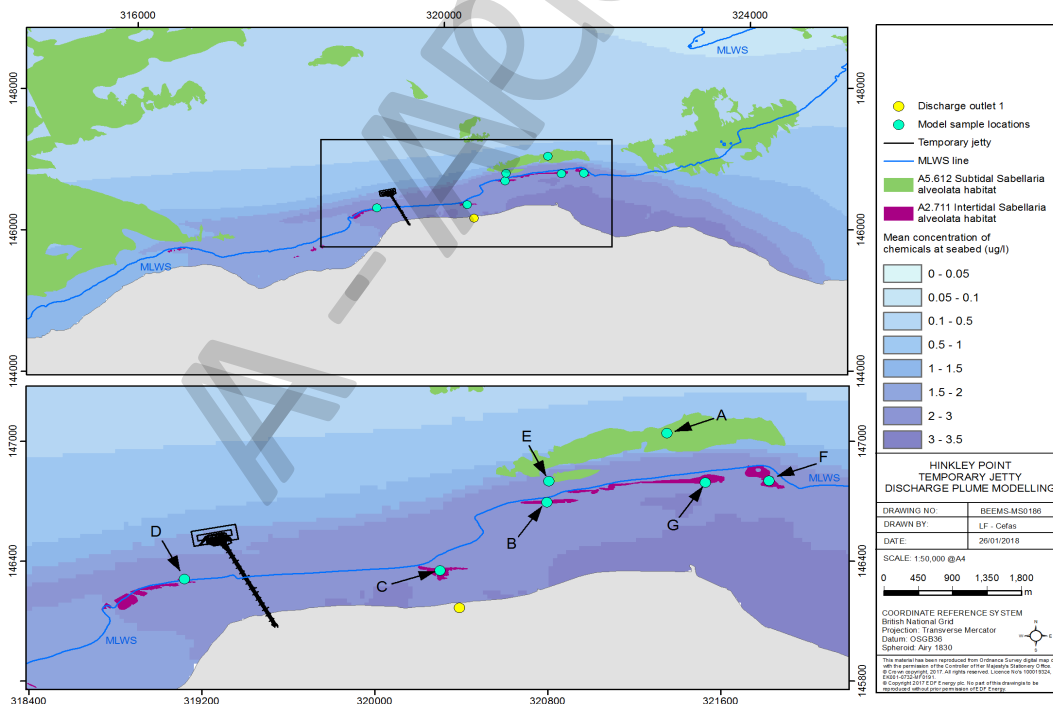


Figure 12. Mean bed concentration of BASF Rheosoil 143 in  $\mu\text{g l}^{-1}$ . The PNEC (surrogate EQS) is  $40 \mu\text{g l}^{-1}$ . Subtidal *Sabellaria* patches A and E and intertidal patches B, C, D, F and G are marked.

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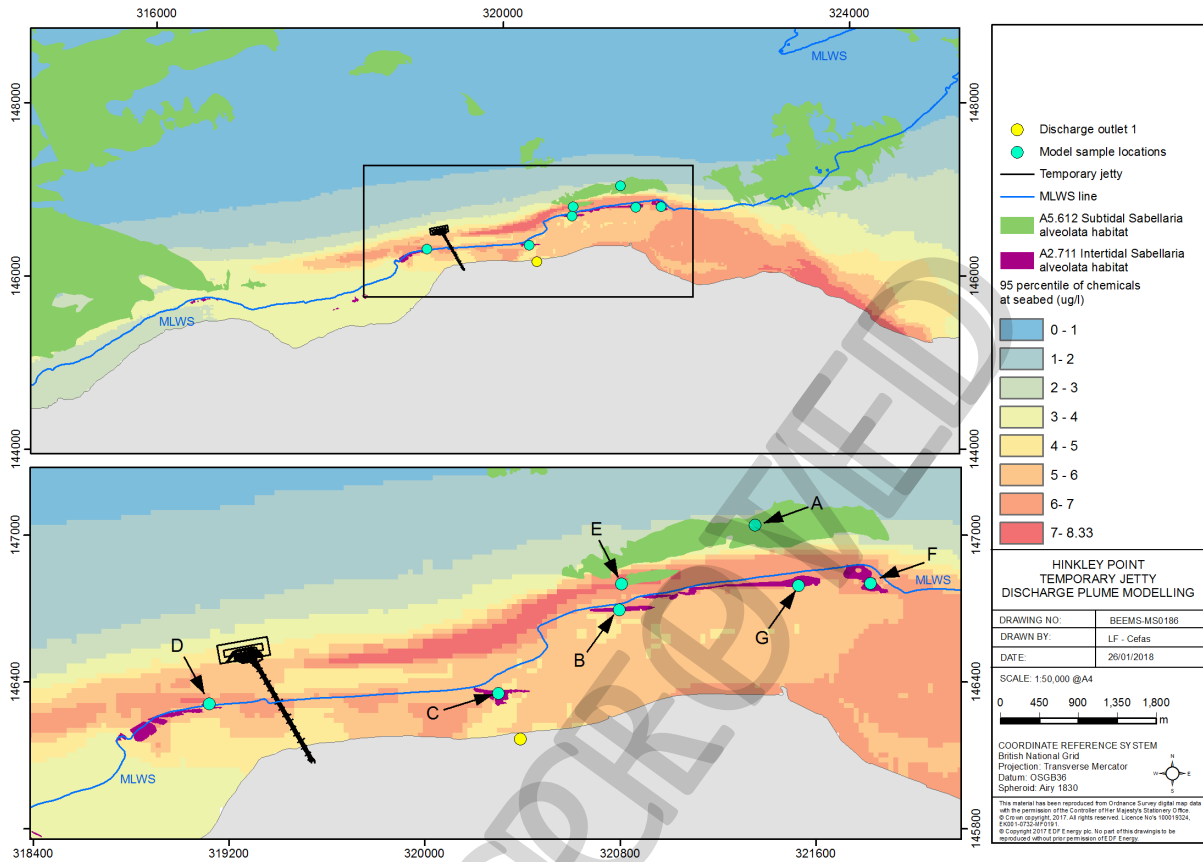


Figure 13. 95<sup>th</sup> percentile bed concentration of BASF Rheosoil 143 in  $\mu\text{g l}^{-1}$ . The PNEC (surrogate EQS) is  $40 \mu\text{g l}^{-1}$ . Subtidal *Sabellaria* patches A and E and intertidal patches B, C, D, F and G are marked.

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**4.4 Modelling of conditioning chemical Condat CLB F5/M in relation to Sabellaria**

Results of Condat CLB F5/M modelling are shown in Figure 14 and Figure 15. This modelling shows the likely spatial extent of a discharge of 40 l s<sup>-1</sup> with a concentration of 6.6 mg l<sup>-1</sup> and an EQS of 4.5 µg l<sup>-1</sup>. No exceedance of the EQS concentration is predicted to occur at the bed, though a small area of exceedance (0.96 ha) is predicted at the surface. Note the scales are different between surface and bottom plots. 95<sup>th</sup> percentile concentrations at the seabed are shown in Figure 16.

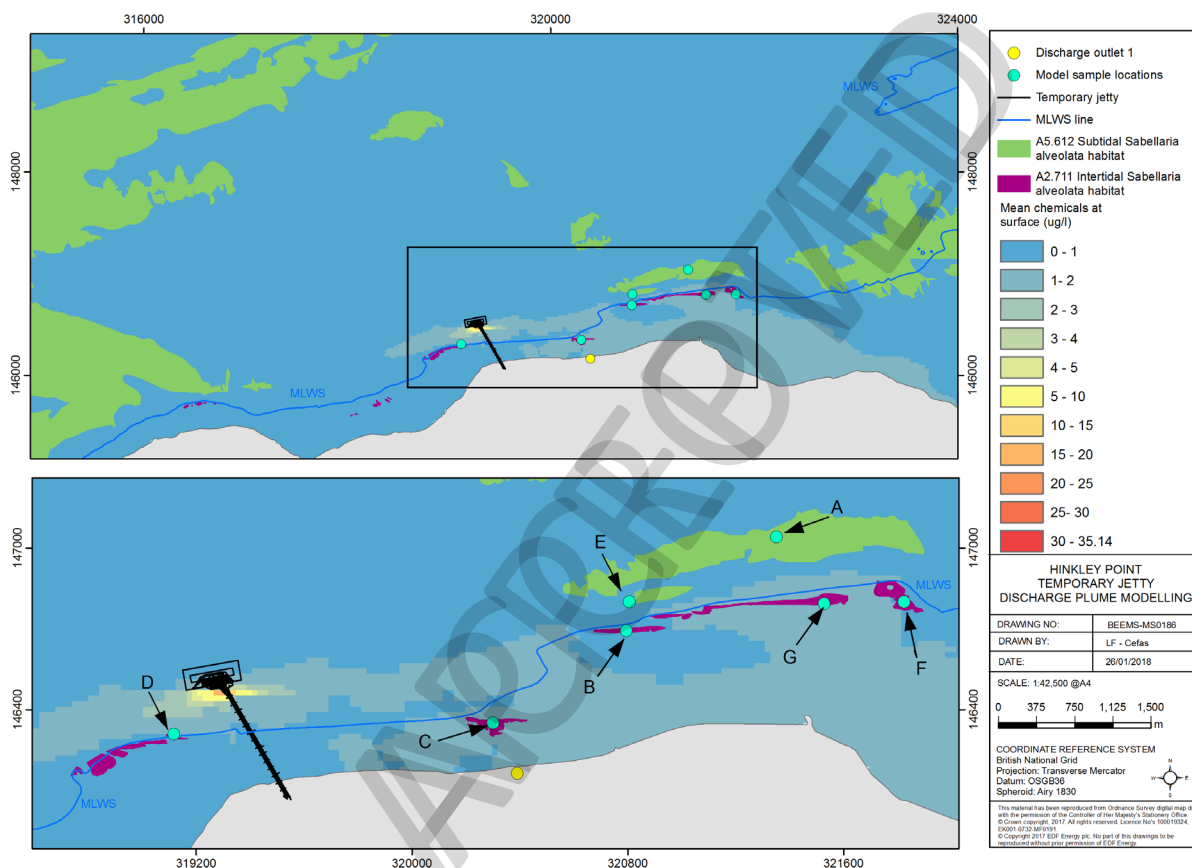


Figure 14. Mean surface concentration of CLB 5 in µg l<sup>-1</sup>. The PNEC (surrogate EQS is 4.5 µg l<sup>-1</sup>) with the location of Sabellaria delineated. Subtidal Sabellaria patch A, E and intertidal Sabellaria patches B, C, D, F and G marked.

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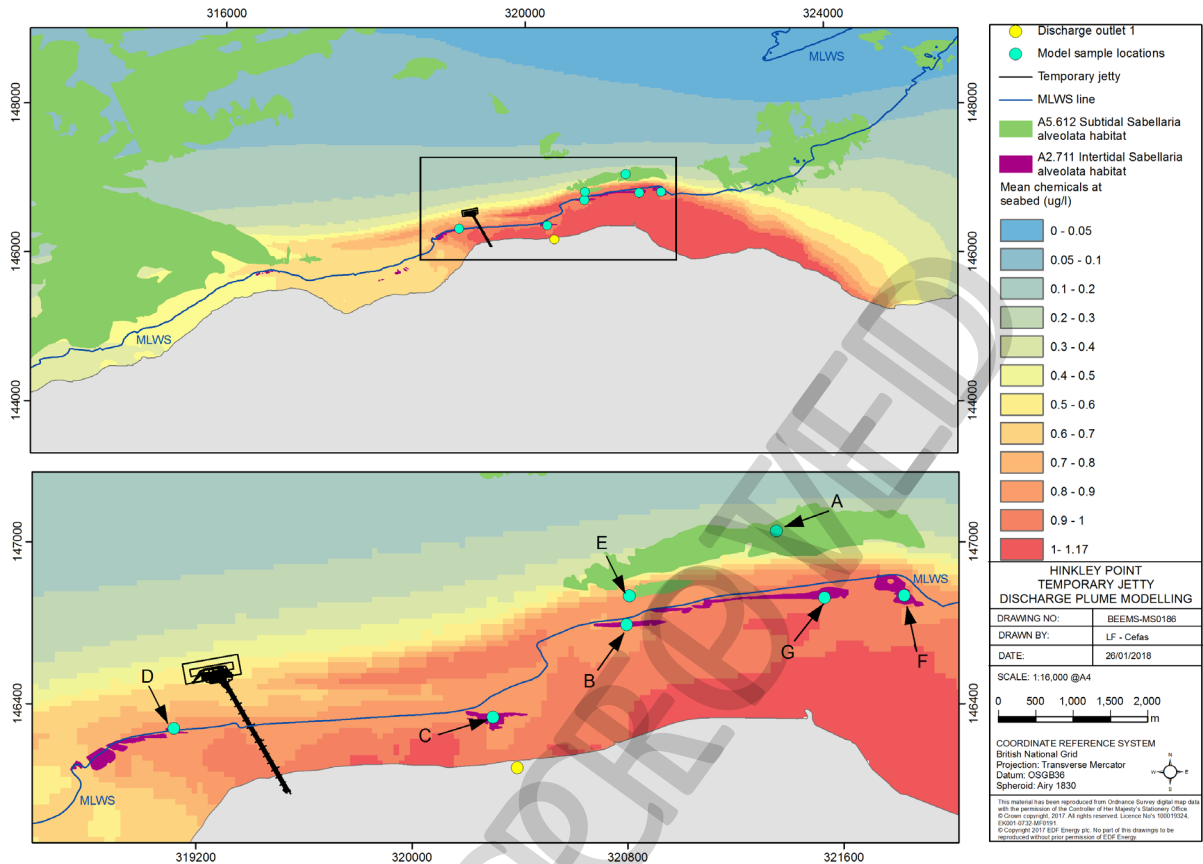


Figure 15. Mean bed concentration of CLB 5 in  $\mu\text{g l}^{-1}$ . The PNEC (surrogate EQS) is  $4.5 \mu\text{g l}^{-1}$  with the location of *Sabellaria* delineated. Subtidal *Sabellaria* patch A, E and intertidal *Sabellaria* patches B, C, D, E and G marked. No exceedance of the PNEC is predicted at the bed.

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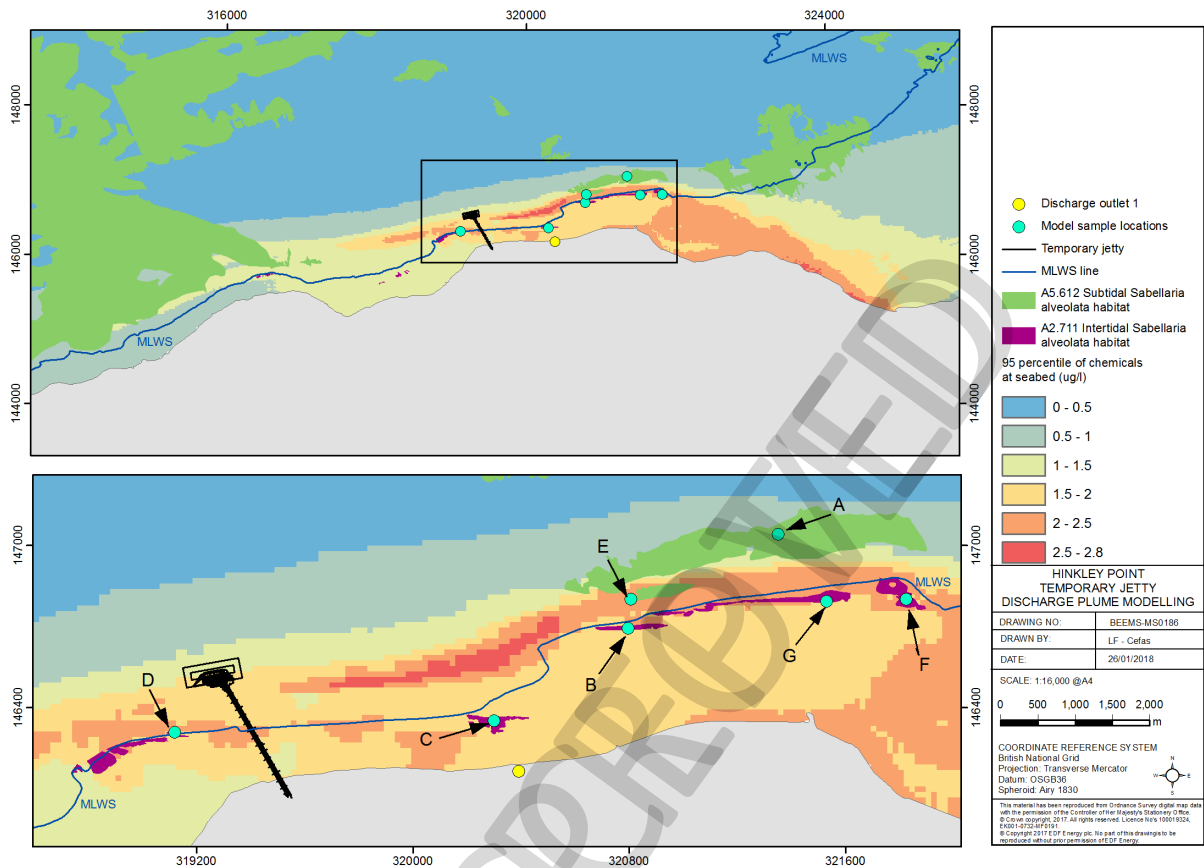


Figure 16. 95<sup>th</sup> percentile concentration of CLB 5 in  $\mu\text{g l}^{-1}$  at the seabed. The PNEC (surrogate EQS) is  $4.5 \mu\text{g l}^{-1}$ . Subtidal *Sabellaria* patches A, E and intertidal *Sabellaria* patches B, C, D, E and G are marked.

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Table 9. Concentrations of active substances of conditioning products, occurring at *Sabellaria* patches A, E (subtidal) B, C, D, F and G (intertidal). Feature locations are shown in Figure 16.

Feature	Mean seabed concentration (µg l <sup>-1</sup> )		95th percentile seabed concentration (µg l <sup>-1</sup> )	
	CLB 5 (PNEC/EQS 4.5 µg l <sup>-1</sup> ).	BASF Rheosoil 143 (PNEC/EQS 40 µg l <sup>-1</sup> )	CLB 5 (PNEC/EQS 4.5 µg l <sup>-1</sup> ).	BASF Rheosoil 143 (PNEC/EQS 40 µg l <sup>-1</sup> )
Subtidal <i>Sabellaria</i> A Easting 321350 Northing 147040	0.53	1.58	0.74	2.21
Intertidal <i>Sabellaria</i> B Easting 320800 Northing 146694	0.87	2.60	1.96	5.87
Intertidal <i>Sabellaria</i> C Easting 320300 Northing 146351	0.86	2.57	1.70	5.10
Intertidal <i>Sabellaria</i> D Easting 319118 Northing 16309	0.84	2.52	1.93	5.79
Subtidal <i>Sabellaria</i> E Easting 320800 Northing 146800	0.79	2.37	2.37	7.12
Intertidal <i>Sabellaria</i> F Easting 321824 Northing 146800	0.91	2.73	1.99	5.96
Intertidal <i>Sabellaria</i> G Easting 321529 Northing 146793	0.97	2.90	2.03	6.09
<i>Corallina</i> Position 5 Easting 320010 Northing 146285	0.94	2.84	2.01	6.01

It can be seen from the figures and table above is that neither mean bed concentrations nor 95<sup>th</sup> percentile concentrations exceed the EQS, and benthic features should therefore remain unaffected. There is a small area of exceedance at the surface near the discharge (Table 10).

Table 10. Summary of exceedance areas for BASF Rheosoil 143 and CLB F5

Discharged chemical	Area of exceedance at surface	Area of exceedance at bed
BASF Rheosoil 143 (Sodium lauryl ether sulfate. )	1875 m <sup>2</sup> (0.19 ha)	0
CLB F5 (Mono-C10-16-alkyl, Sodium sulfate (≤10%))	10,000 m <sup>2</sup> (1 ha)	0

Location G has the highest mean concentrations of conditioning products (Table 9). A time series of CLB 5 concentration at this location is therefore shown in Figure 17 to demonstrate the nature of the exposure. The PNEC for CLB 5 is 4.5.

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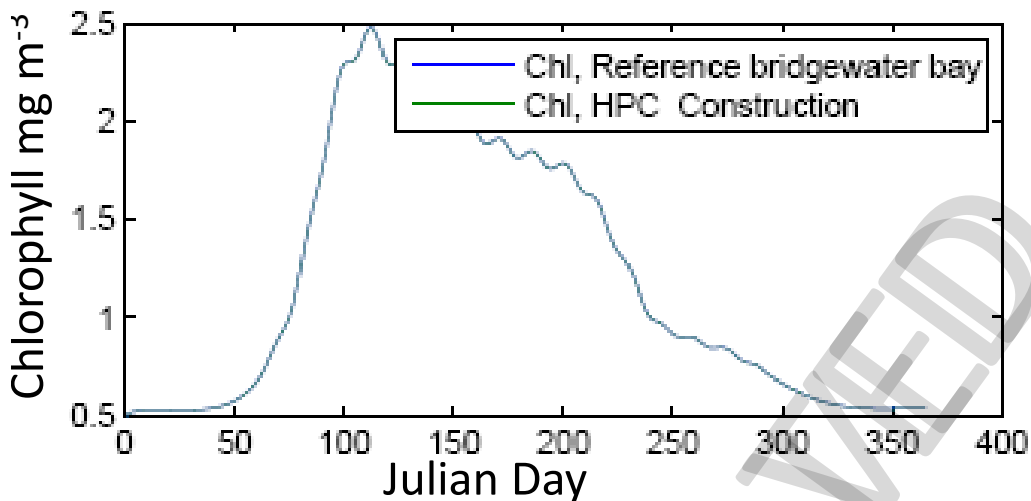


Figure 19 : Instantaneous phytoplankton levels (mg Chlorophyll m<sup>-3</sup>), for Bridgwater Bay with no power station discharge, and HPC construction. Note that additional nutrient discharges from HPC have no effect on background chlorophyll concentrations (and the reference and construction lines are the same).

Table 13 Phytoplankton and macroalgae production

Scenario	Phyto Annual Gross Production, (g C m <sup>-2</sup> y <sup>-1</sup> )	Macro Annual Gross Production, (g C m <sup>-2</sup> y <sup>-1</sup> )
Bridgwater Bay	11.05	18.43
HPC Construction	11.05	18.43

#### 4.10.2 Ammoniacal Nitrogen

Due to the breakdown of chemicals added during the commissioning process some ammoniacal nitrogen will be generated. This is estimated to have a concentration of 271 mg l<sup>-1</sup> (Calculation of this value is shown Appendix C Table 28) which is discharged over 5.63 hrs at either 37 l/s or 70 l/s depending on whether there is drainage from one or two HXA tanks per day.

This cold commissioning discharge needs to be considered alongside the construction discharge from groundwater and sewage. As this will occur late in the construction process, Case D flow rate (38 l/s) is most appropriate. Thus, the cases with maximum load of total ammonia to consider are:

1. A continuous discharge (38.3 l/s, at 10.03 mg l<sup>-1</sup>) + a pulse discharge at midday (37 l/s, 271 mg l<sup>-1</sup>) for 5.63 h.
2. A continuous discharge (38.3 l/s, at 10.03 mg l<sup>-1</sup>) + a pulse discharge at midday (70 l/s, 271 mg l<sup>-1</sup>) for 5.95 h.

These two scenarios were therefore modelled in GETM and treated as passive tracers, in a similar manner to the approach adopted for the conditioning chemicals, using a month-long simulation of the likely behaviour over a spring-neap cycle.

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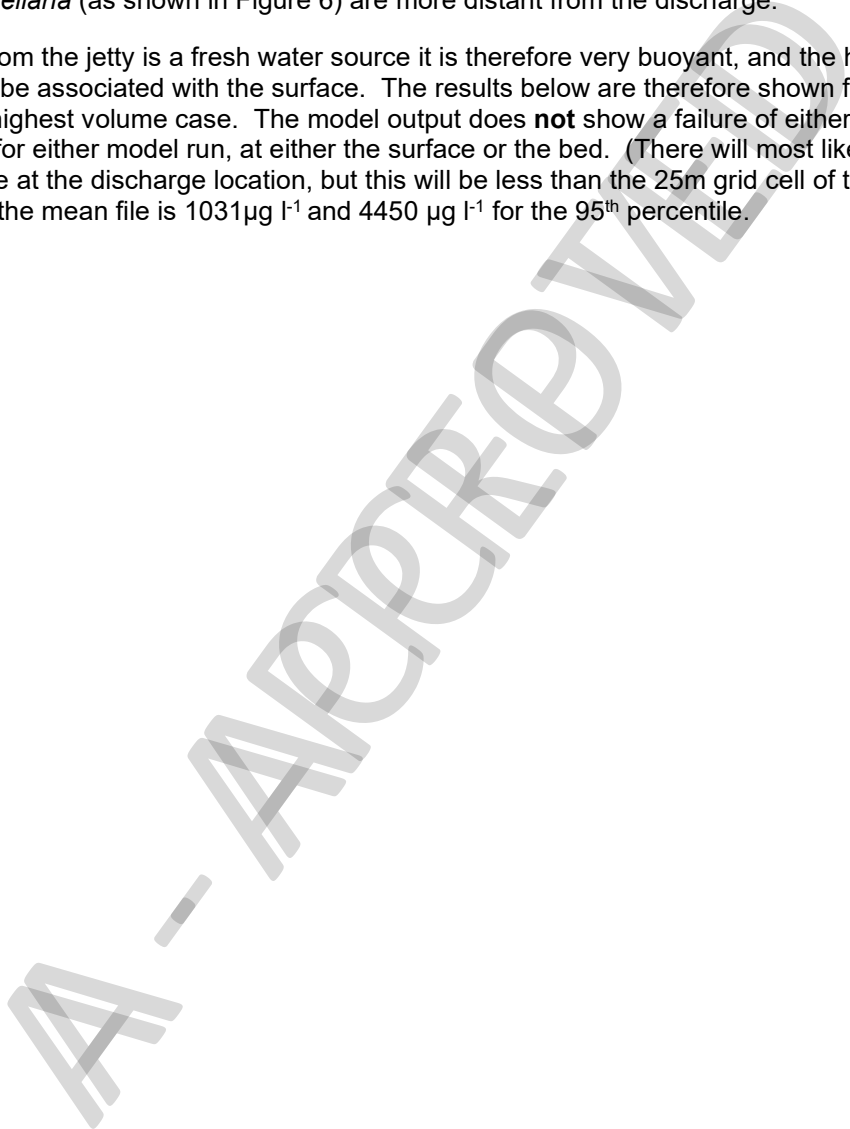
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There are also standards, for total ammonia, for which the concentration should not be exceeded:

- a) 1100  $\mu\text{g l}^{-1}\text{-N}$  annual average (AA)
- b) 8000  $\mu\text{g l}^{-1}\text{-N}$  maximum acceptable concentration (MAC) (interpreted as 95<sup>th</sup> percentile).

The mean background ammoniacal Nitrogen ( $\text{NH}_4\text{-N}$ ) concentration is 124  $\mu\text{g l}^{-1}$  measured in an annual survey at Hinkley Point (Amec, 2009). This has been included in the plots below (Figure 20 and Figure 21) which show the total ammonia discharge plume prediction in relation to the Corallina feature. For *Sabellaria* the nearest habitat to the discharge is in the intertidal area close to the *Corallina* at station 8. Other areas of *Sabellaria* (as shown in Figure 6) are more distant from the discharge.

As the discharge from the jetty is a fresh water source it is therefore very buoyant, and the highest concentrations will be associated with the surface. The results below are therefore shown for the surface and also from the highest volume case. The model output does **not** show a failure of either the mean or the 95<sup>th</sup> percentile for either model run, at either the surface or the bed. (There will most likely be a small area of exceedance at the discharge location, but this will be less than the 25m grid cell of the model). The maximum value in the mean file is 1031 $\mu\text{g l}^{-1}$  and 4450  $\mu\text{g l}^{-1}$  for the 95<sup>th</sup> percentile.



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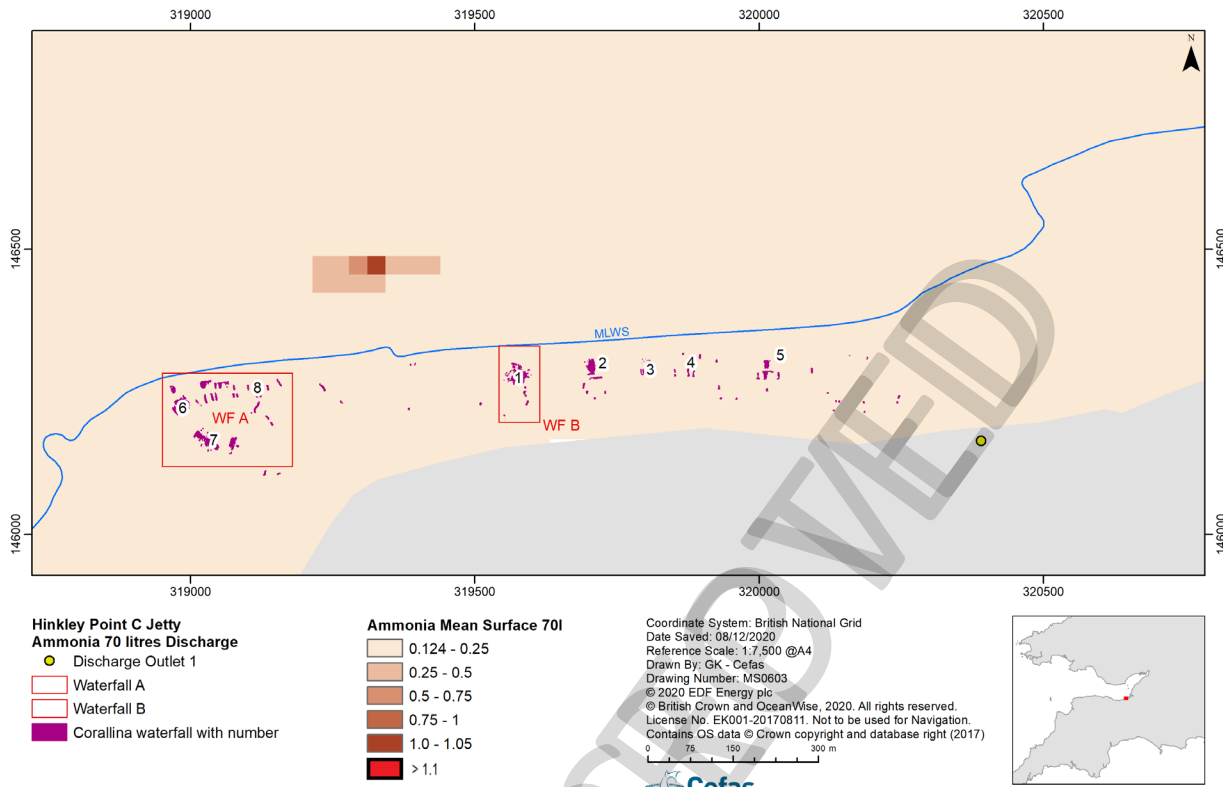


Figure 20 Surface mean ammonia concentration (mg l<sup>-1</sup>) for the 70 l/s discharge simulation. No values > 1100 µg l<sup>-1</sup> (PNEC). The figure includes *Corallina* waterfalls. The closest *Sabellaria* to the discharge is in the intertidal near station 8.

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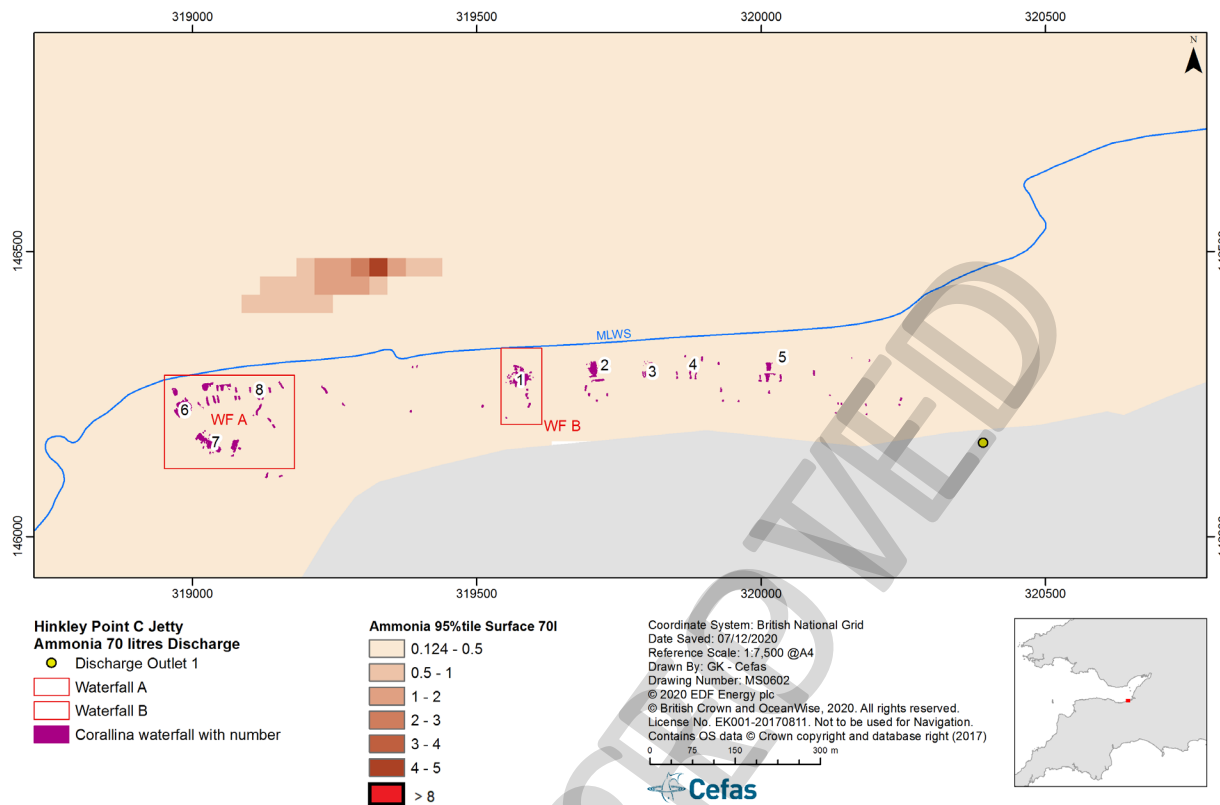


Figure 21 95<sup>th</sup> percentile surface concentration (mg l<sup>-1</sup>) of ammonia for 70 l/s. No value exceeds > 8000 µg l<sup>-1</sup> MAC. The figure includes Corallina waterfalls. The closest *Sabellaria* to the discharge is in the intertidal near station 8.

**4.10.3 Consideration of un-ionised ammonia concentration**

The concentration of un-ionised ammonia can be derived from knowledge of the total ammoniacal nitrogen concentration (i.e. NH<sub>4</sub> as N), the salinity, the pH and temperature using the EA calculator.

The EQS for un-ionised ammonia is 21 µg l<sup>-1</sup> expressed as an annual average, however being consistent with the previous screening, this value is compared with the 95<sup>th</sup> percentile source contributions. The annual mean values were temperature 12.5 °C, pH 7.86 and salinity 31.5 g/kg. The values have been calculated by taking the GETM output, adding the total ammonia background (0.124 mg l<sup>-1</sup>) and then using the EA calculator to generate the proportion of un-ionised ammonia.

**4.10.4 Consideration of combined inputs of concrete washwater**

During the period when commissioning chemicals and construction wastewater (as described for Case D) are being discharged at the jetty a maximum daily discharge of treated concrete wash water of 50 m<sup>3</sup>/day may also occur. The discharge rate for the concrete wash water (CWW) would be equivalent to a very low continuous daily discharge of 0.57 l/s<sup>-1</sup>. Preliminary characterisation of untreated concrete wash water indicates the presence of retarder and accelerator chemicals but also trace contaminant metals and ammoniacal and dissolved inorganic nitrogen. The CWW discharge represents just over 2% of the Case D groundwater discharge (25 l/s<sup>-1</sup>). Because of the very low CWW discharge rate and its low relative percentage contribution compared to groundwater inputs there are likely to be some small but non-significant elevations in the overall discharge concentrations of selected metals. However, as the combined discharge rate of e.g. groundwater and CWW would still be very low ca. 26 l/s<sup>-1</sup>, an increase of a few

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following treatment. As the areas of concern are the designated features of *Corallina* and *Sabellaria*, more detailed time series were assessed from the *Corallina* marked in Figure 22 and for the *Sabellaria* Figure 16 and are shown below. The values of un-ionised ammonia have been derived using mean temperature, salinity, and pH.

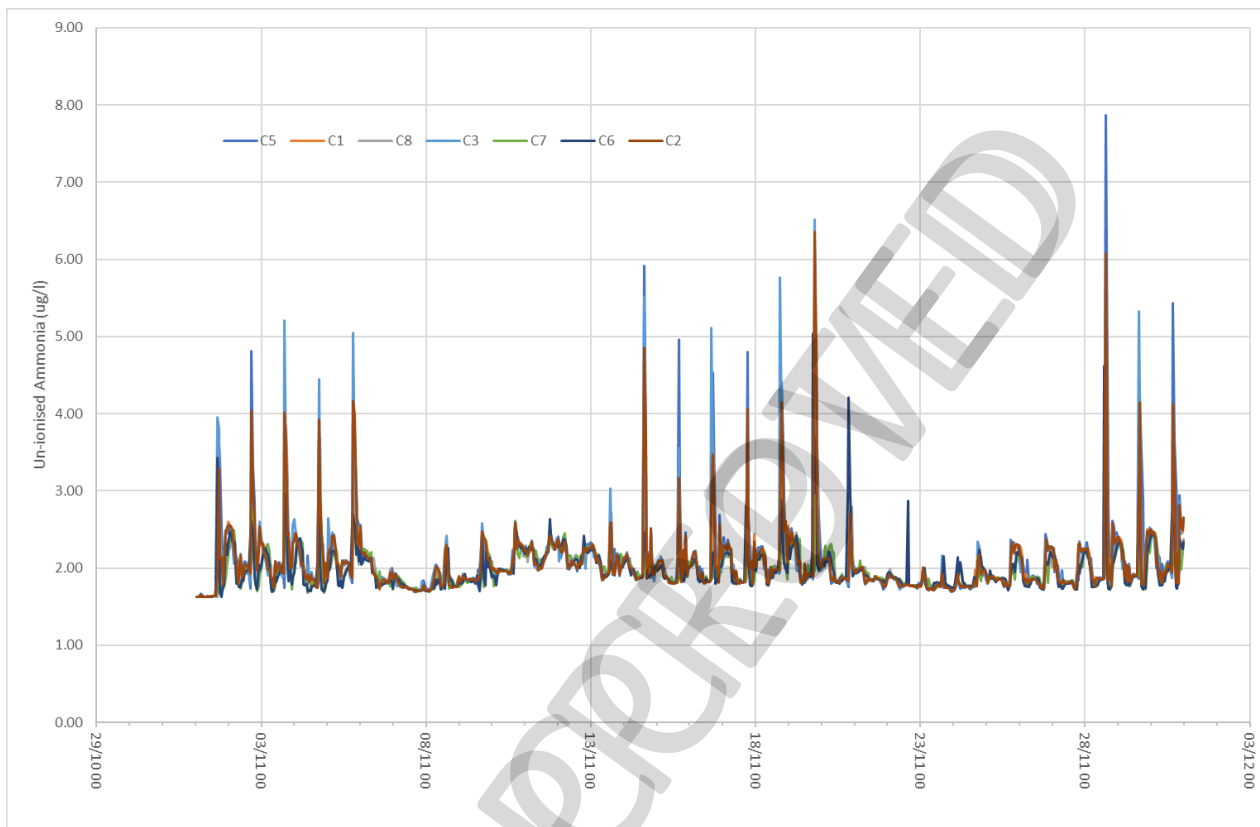


Figure 24 Time series of un-ionised ammonia at the locations of *Corallina* for the 38 l/second at 10 mg l<sup>-1</sup> + 70 l/second at 271 mg l<sup>-1</sup> scenario.

Evident from Figure 24 is that no *Corallina* features are exposed to high level of un-ionised ammonia, using annual means (as is the standard) however during summer the temperature will be significantly elevated. Therefore, mean and 95<sup>th</sup> percentile values at this location have been derived for summertime when temperatures will be much higher, using the 98<sup>th</sup> percentile temperature of 20.4 °C. Apparent, from the table below is that even in summer mean values are still low <4 µg l<sup>-1</sup>.

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Table 16 Summary of un-ionised ammonia ( $\mu\text{g l}^{-1}$ ) at *Sabellaria* features (A – G) for mean and elevated summer temperatures (letters correspond to the locations on Figure 16).

Feature	Mean seabed concentration ( $\mu\text{g l}^{-1}$ )		95th percentile concentration ( $\mu\text{g l}^{-1}$ )	
	Annual	Summer	Using mean values	Summer
Subtidal <i>Sabellaria</i> A Easting 321350 Northing 147040	1.74	3.21	1.90	3.46
Intertidal <i>Sabellaria</i> B Easting 320800 Northing 146694	2.01	3.71	2.60	4.77
Intertidal <i>Sabellaria</i> C Easting 320300 Northing 146351	2.08	3.85	2.68	4.91
Intertidal <i>Sabellaria</i> D Easting 319118 Northing 16309	2.07	3.83	2.56	4.67
Subtidal <i>Sabellaria</i> E Easting 320800 Northing 146800	1.95	3.61	2.54	4.67
Intertidal <i>Sabellaria</i> F Easting 321824 Northing 146800	2.03	3.75	2.72	4.94
Intertidal <i>Sabellaria</i> G Easting 321529 Northing 146793	2.05	3.79	2.71	4.94

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February temperatures are 6.6°C and August 19.4°C (BEEMS Technical Report 187). The typical inter-annual variation in monthly mean temperatures is 1.1°C.

It is not anticipated that this temperature change would affect the chemistry or toxicity of metals in the jetty discharge. The mean temperature uplift at *Sabellaria* locations near HPC and HPB are shown in Table 17.

Table 17. Mean temperature uplift due to HPB at *Sabellaria* locations at the bed with positions as those previously e.g. Figure 16.

Location	Mean temperature uplift (°C)
A	0.41
B	1.18
C	0.78
D	0.68
E	0.94
F	1.27
G	4.17

## 5.2 Discharge of waste by Hinkley B and Hinkley A

There is permitted discharge of groundwater of 50 m<sup>3</sup> d<sup>-1</sup> until March 2018 from Hinkley Point A (permit EPR/EB3392VY). The discharge is confined to two hours before and two hours after high tide.

In addition to the thermal plume discharge (see above), Hinkley B has a permit (HPB Consent no 070408) to discharge up to 1000 m<sup>3</sup> d<sup>-1</sup> of treated sewage with ammoniacal nitrogen concentrations up to 30 mg l<sup>-1</sup> and suspended solids up to 60 mg l<sup>-1</sup>. For DIN, this equates to an annual load of 10950 kg. These discharges are released at a discharge point close to the sea wall.

There is an east west separation of approximately 2.4 km between the jetty discharge and HPB/HPA outlet channel.

From a DIN perspective it is unlikely that the total discharge from the jetty would be detectable beyond a short distance (<50 m) from the jetty. Similarly, the discharges from HPB and HPA are small and will have undergone significant dilution by the time they have been advected to the small area where the jetty discharge may be detectable. The physical separation of 2.4 km between the jetty discharge and the HPA/HPB discharge channel is therefore considered sufficient to ensure there is no interaction between the discharges.

For WFD purposes, the HPC sewage discharge(s) will increase the total loading of DIN in the two local waterbodies in addition to the uplift already caused by the HPB discharge. HPB discharges into the Parrett waterbody, and the permitted discharge of 10,950 kg annually is calculated to uplift the Parrett waterbody concentration by 3.49 µmol l<sup>-1</sup> (if the discharge is completely released into the Parrett water body alone). As the background DIN concentration is high this does not affect the WFD status classification. If the jetty discharge is added to the HPB DIN discharge, the uplift would increase to 5.05 µmol l<sup>-1</sup>. The long-term fate of the DIN discharge from the temporary jetty is likely to be shared between the two WFD waterbodies (Bridgwater Bay and Parrett), and this is also true of the HPB discharge because the outfall is near the junction of these two waterbodies. Thus, using a shared equal split between the two bodies the combined effect of HPC (construction discharge at the jetty) and HPB is calculated to uplift the Bridgwater Bay waterbody by 0.58 µmol l<sup>-1</sup> and the Parrett waterbody by 2.52 µmol l<sup>-1</sup>. The WFD classification of these waterbodies would be unaffected. Considering the additional inputs of nutrients during the commissioning

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period the results from the CPM model show that that there is no difference between the Bridgwater bay reference case or the HPC construction run for either phytoplankton production or for macroalgae.

**5.2.1 Coliforms from HPB**

CORMIX dilution rates (see Appendix D) have been used to determine the maximum distance from the discharge at which bathing water standards could be exceeded. The HPB discharge permit specifies that the discharge can only take place either side of high water when water depth is similar to that of the HPC discharge. The highly conservative Cormix estimates of mixing and the exceedance distances calculated are therefore a useful conservative guide.

Table 18 Coliforms discharge from HPB

Species	Standard cells/100ml	Maximum discharge concentration cells/100ml	2 <sup>nd</sup> treatment. 2 log reduction.	Dilution factor to meet standard	Extent of exceedance
<i>E.coli</i>	500	240,000,000	2,400,000	4800	~ 1.8 km
Enterococci	200	13,600,000	136,000	680	<200m

It is not known what the actual microbiological discharge concentration is from Hinkley Point B, however assuming the same standard of secondary treatment as Hinkley C would imply a maximum potential extent of exceedance for *E.coli* of approximately 1.8 km (Table 18). This theoretical exceedance could only occur in very calm conditions. Under such calm conditions the plume would be long and thin and would not interact with the temporary jetty discharge, as the tidal stream lines are separate. In practice most of the time, wave mixing will mix the discharge rapidly so that no interaction could occur.

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Table 19 Tests to determine if habitats areas are affected by the combined construction and cold commissioning discharges.

Test	Predicted activity footprint	Result
i. 0.5 km <sup>2</sup> or larger	Heavy metals, Tunnelling chemicals, dissolved inorganic nitrogen and phosphorus, total ammonia and un-ionised ammonia, biological oxygen demand, suspended solids	Areas affected are below test value
ii. 1% or more of the water body's area	Heavy metals, Tunnelling chemicals, dissolved inorganic nitrogen and phosphorus, total ammonia and un-ionised ammonia, biological oxygen demand, suspended solids	Areas affected are below test value
iii. within 500 m of any higher sensitivity habitat	Heavy metals, Tunnelling chemicals, dissolved inorganic nitrogen and phosphorus, total ammonia and un-ionised ammonia, biological oxygen demand, suspended solids	The jetty discharge point is less than 500 m from <i>Sabellaria</i> and <i>Corallina</i> features
iv. 1% or more of any lower sensitivity habitat	Heavy metals, Tunnelling chemicals, dissolved inorganic nitrogen and phosphorus, total ammonia and un-ionised ammonia, biological oxygen demand, suspended solids	Is below test value

Tests i., ii. and iv. are met but the jetty discharge is within 500 metres of *Sabellaria* and *Corallina* habitat.

**Potential effects on higher and lower sensitivity WFD habitats**

The discharge from the jetty is within 500 m of higher sensitivity habitat polychaete reef and with *Corallina* habitat. However, the predicted plume discharge from the jetty is a fresh water source it is therefore very buoyant, the highest values are associated with the surface. The highest areas of exceedance of standards for all parameters of relevance to a WFD assessment was for one of the tunnelling chemicals Condat CLB F5/M for which an area of 1 ha at the surface exceeds the relevant EQS. At the bed, the relevant concentration was predicted to be below EQS within 5 metres of the discharge. Neither mean bed concentrations nor 95<sup>th</sup> percentile concentrations exceed the EQS, and benthic features should therefore remain unaffected. There is a small area of exceedance at the surface near the point of discharge.

For the other discharges considered the area above EQS was much more limited. The assessment of the ammoniacal nitrogen discharge when at maximum levels with combined construction and cold commissioning inputs showed no areas of exceedance for total ammonia concentrations nor at the mean un-ionised ammonia EQS at the surface or bed and an area of only 0.2 ha at the surface for the un-ionised ammonia as a 95<sup>th</sup> percentile. More detailed time series analysis considering more extreme summer temperatures when the proportion of un-ionised ammonia is likely to be maximal confirmed that concentrations were less than 25% of the EQS at the closest locations of *Corallina* and *Sabellaria* features. The same assessment would apply to lower sensitivity habitat close to the jetty discharge.

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## 7 Summary for construction and commissioning

For the construction discharge there is a small (1 ha) mixing zone (the area where the relevant EQSs are exceeded) around the jetty point of discharge itself. The mixing zone will have EQS exceedances for concentrations of zinc, copper and TBM ground conditioning chemicals. There will also be localised increases in DIN. The area of exceedance is largest for zinc and conditioning chemicals and the modelling has therefore focused on these substances for the combined commissioning inputs and for those from CWW discharge is:

- Case D, comprising 20 l s<sup>-1</sup> groundwater, 13.3 l s<sup>-1</sup> of treated sewage and ca., 5 l s<sup>-1</sup> of tunnelling groundwater discharge).

Where discharges during the construction period contribute the highest loadings of a given contaminant, the summary text remains unchanged from earlier versions of this report. However, updates are provided for the assessment of ammoniacal nitrogen inputs as these receive contributions from both construction discharges and from the breakdown of commissioning chemicals and are assessed both in terms of the total ammonia and of the proportion of the input that would form un-ionised ammonia. Breakdown of commissioning chemicals will also contribute additional inputs to the nitrogen and phosphorus loading, and these are assessed using a combined phytoplankton and macroalgal box model.

### Heavy metals

For Case D, both copper and zinc fail the Environment Agency screening tests. During peak ground water load (Case C) chromium also fails this test, although only marginally and for a period of approximately eight weeks when the flow is predicted to be at a maximum. If the annual average were used, then only zinc would be of potential concern as the copper Effective Volume Flux (EVF) is substantially below the threshold. As zinc was the substance of greatest exceedance this discharge was considered further by detailed modelling. The areas of exceedance for zinc at the surface were 0.3 Ha and 0.125 Ha for Cases C and D, respectively. As the discharge is buoyant, exceedance at the bed was only expected within a very short distance (less than 5 m) of the discharge itself. Some small additional metals inputs occur via the CWW discharge, but the discharge rate and concentrations are so low that this is not expected to change the present assessment.

There is no predicted exposure of designated bed features above the EQS at any time.

### TBM soil conditioning chemicals

Chemical constituents of TBM ground conditioning products BASF Rheosol 143 and Condat CLB F5/M failed the initial EQS screening and were investigated further using modelling approaches. With the worst-case chemical constituent (i.e., with the most toxic chemical group) there was no exceedance of the PNEC at the bed and the areas of exceedance at the surface were very small (0.19 ha for Rheosol 143 and 1 ha for Condat CLB F5/M). This assessment used examples of typical soil conditioning chemicals (primarily different types of surfactants) with particularly low (i.e., the most conservative) PNEC values. Providing the chemical components of any other products selected for soil conditioning have an Effective Volume Flux value at or below 58.7, then areas of exceedance will be the same or less than those shown here for CLB F5 mono- alkyl sodium sulphate.

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### DIN and phosphorus inputs during construction and commissioning

The jetty discharge will release dissolved inorganic nitrogen (DIN) into the estuary. Under the Water Framework Directive Standards, the Bridgwater Bay waterbody has 'Moderate' status for DIN. The jetty discharges result in a very localised elevation in DIN in the receiving waterbody and the initial screening test was passed (Table 3).

The average annual uplift from the jetty discharge during year 1 was estimated at  $0.36 \mu\text{mol l}^{-1}$  relative to a mean annual concentration of  $75 \mu\text{mol l}^{-1}$  within Bridgwater Bay and status is unaffected. Due to the high turbidity environment, productivity in the Severn is light-limited (Underwood, 2010) and the effects of minor DIN loading on the designated Severn Estuary features are deemed insignificant and not assessed further. In-combination effects of discharges from HPB are considered in Section 5 and it is concluded that there is no direct intersection between the HPB discharge and the jetty discharge. Based on the results of a CPM model this assessment would also apply during the period when the breakdown of cold commissioning discharge inputs makes a further contribution to nitrogen and phosphorus loadings. Some small additional nitrogen inputs occur via the CWW discharge, but the discharge rate and concentrations are so low that this is not expected to change the present assessment.

### Total and un-ionised ammonia during construction and commissioning

Using the EA calculator, the EQS for un-ionised ammonia ( $21 \mu\text{g l}^{-1}$ ) was exceeded in Case  $C_{\text{max}}$  and  $D_{\text{max}}$ , but only in the immediate vicinity of the discharge (within less than 10 m). Rapid dilution rates mean that the EQS was only exceeded when groundwater discharges and sewage discharges were at their maximum. The total area of EQS exceedance was 0.005 ha and, even during maximum discharges, the initial screening test was passed (Table 3). When combined construction and cold commissioning inputs of un-ionised ammonia are considered the area above the  $21 \mu\text{g l}^{-1}$  threshold, when using the 95<sup>th</sup> percentile of ammoniacal nitrogen is small (Maximum 0.2 hectares). For the actual EQS when using the annual average there are no areas of exceedance and the un-ionised ammonia concentrations associated with *Corallina* and *Sabellaria* features are less than 25% of the EQS. An additional assessment of the in-combination effects of concurrent sewage discharges from the temporary jetty and HPB are considered below. Some small additional ammoniacal nitrogen inputs occur via the CWW discharge, but the discharge rate and concentrations are so low that this is not expected to change the present assessment.

For total ammonia, the modelling shows that at the 25m resolution of the model for the construction and commissioning phase there is no exceedance of either the mean  $1100 \mu\text{g l}^{-1}$  or of the MAC  $8000 \mu\text{g l}^{-1}$ .

### Biological oxygen demand

The sewage treatment works is expected to achieve a maximum concentration of Biological Oxygen Demand (BOD) of  $40 \text{ mg l}^{-1}$  (i.e., draw down over 5 days) and the indicative Maximum Allowable Concentration (MAC) to be applied in the permit is therefore  $40 \text{ mg l}^{-1}$ . Using the  $13.3 \text{ l s}^{-1}$  discharge and a BOD of  $40 \text{ mg l}^{-1}$ , a daily BOD of 46 kg was calculated. This amount of oxygen would be transferred across  $14364 \text{ m}^2$  of the water surface in a day. The tidal excursion (how far a particle is advected) at Hinkley Point, even on the weakest (neap) tides, is many kilometres, thus there is ample resupply of oxygen from the atmosphere so that no change in oxygen concentration would be observed.

### Suspended solids

The background suspended solids concentration in the receiving water is relatively high (with a mean of  $264 \text{ mg l}^{-1}$  and a minimum of  $33 \text{ mg l}^{-1}$ ). Commissioning activities such as hydrostatic testing and flushing will result in variable suspended solids loadings within resultant effluents. The primary objective of the Commissioning Effluent Treatment Plant (CETP) is to reduce the hydrazine concentration in the final effluent discharge. However, the CETP will also incorporate methods to reduce suspended solids to permitted levels prior to discharge.

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### Coliforms – bathing water standards and shell fisheries

The discharge point is not in designated bathing waters. Model predictions (which do not consider wave-driven mixing) indicate that treatment from the plant is sufficient to ensure that microbial concentrations in discharged waters comply with bathing water standards within a maximum of 2.8 km from the discharge point (without UV treatment) and within 10 m (with UV treatment). The nearest designated bathing waters are 12 km distant from the jetty discharge and the closest shell fishery is 32 km distant and so no effects on these features is predicted.

### Potential in combination effects with the HPB discharge

This report has considered the potential interaction of the jetty discharges and the sewage discharge from HPB (2.4 km distant). There is no overlap of the plume mixing zone and the HPB discharge, and no interaction occurs because of the physical separation and the small discharge volume from the jetty.

During the main construction period the total annual loading of DIN has been considered for the two impacted Water Framework Directive designated waterbodies (Bridgwater Bay and River Parrett). The combined effect of HPC (construction discharge at the jetty) plus HPB is to uplift the DIN concentration in the Bridgwater Bay water body by  $0.58 \mu\text{mol l}^{-1}$  and the Parrett waterbody by  $2.52 \mu\text{mol l}^{-1}$  (when all the discharge goes into one body). There would therefore be no change of status: the present mean is  $75 \mu\text{mol l}^{-1}$  and the 99<sup>th</sup> percentile concentration for Good status in turbid waters is  $180 \mu\text{mol l}^{-1}$ . These results have also been confirmed including additional nutrient inputs during commissioning using a CPM model with no difference shown between the Bridgwater bay reference case or the HPC construction and cold commissioning run for either phytoplankton production or for macroalgae.

It is not known what the actual discharge concentration of microbial discharge is from Hinkley Point B, however assuming the same standard of secondary treatment as Hinkley Point C would imply an extent of exceedance of approximately 1.8km. This theoretical exceedance could only occur in very calm conditions. Under such calm conditions the plume would be long and thin and would not interact with the temporary jetty discharge, as the tidal stream lines are physically separate. In practice for most of the time, wave mixing will mix the discharge rapidly so that no interaction could occur.

If UV treatment is applied at HPC no microbial interaction with HPB is likely.

The thermal plume discharge from HPB has been considered and is expected to raise the mean background sea temperature at the jetty discharge location (where exceedance of the EQS's occurs) by approximately  $1^\circ\text{C}$ , this small temperature rise compared to the annual seasonal variation is considered unlikely to have any effect on the toxicity of any of the chemicals or metals considered.

### Test for inclusion of habitats in the WFD assessment

The tests for inclusion of habitats in a WFD assessment are if the footprint of the FRR discharge is any of the following:

- i.  $0.5\text{km}^2$  or larger
- ii. 1% or more of the water body's area
- iii. within 500m of any higher sensitivity habitat
- iv. 1% or more of any lower sensitivity habitat

For tests i., ii. and iv there is no exceedance of these areas, but the jetty discharge is within 500 metres of *Sabellaria* and *Corallina* habitat.

### Potential effects on WFD habitat

Higher sensitivity habitats:





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Table 21. Background values for contaminants in the Severn Estuary (from Amec 2009 report)

Analyte	Units	Concentration
Cyanide as CN	mg l <sup>-1</sup>	<0.500
Ammoniacal Nitrogen as N	mg l <sup>-1</sup>	<0.01
Nitrite as N	mg l <sup>-1</sup>	<0.004
Nitrogen: Total Oxidised as N	mg l <sup>-1</sup>	1.43
Orthophosphate, reactive as P	mg l <sup>-1</sup>	0.08
Fluoride	mg l <sup>-1</sup>	0.857
Sulphide as S	mg l <sup>-1</sup>	<0.01
Solids, Dissolved at 105 C	mg l <sup>-1</sup>	615
pH	pH Units	8.09
Bromide	mg l <sup>-1</sup>	43.4
Arsenic	g l <sup>-1</sup>	1.99
Selenium	µg l <sup>-1</sup>	<1
Beryllium	µg l <sup>-1</sup>	<10
Cobalt	µg l <sup>-1</sup>	<10
Molybdenum	µg l <sup>-1</sup>	<30
Silver	µg l <sup>-1</sup>	<1
Cadmium	µg l <sup>-1</sup>	0.08
Copper	µg l <sup>-1</sup>	4.17
Lead	µg l <sup>-1</sup>	0.5
Nickel	µg l <sup>-1</sup>	0.974
Zinc	µg l <sup>-1</sup>	4.94
Boron, Dissolved	µg l <sup>-1</sup>	2980
Calcium, Dissolved	mg l <sup>-1</sup>	299
Iron, Dissolved	µg l <sup>-1</sup>	<100
Magnesium, Dissolved	mg l <sup>-1</sup>	873
Manganese, Dissolved	µg l <sup>-1</sup>	<20
Potassium, Dissolved	mg l <sup>-1</sup>	265
Sodium, Dissolved	mg l <sup>-1</sup>	6990
Strontium, Dissolved	µg l <sup>-1</sup>	5060
Sulphate, Dissolved as SO4	mg l <sup>-1</sup>	1800
Boron	µg l <sup>-1</sup>	2940
Calcium	mg l <sup>-1</sup>	292
Iron	µg l <sup>-1</sup>	153
Magnesium	mg l <sup>-1</sup>	841
Manganese	µg l <sup>-1</sup>	<20
Potassium	mg l <sup>-1</sup>	255
Sodium	mg l <sup>-1</sup>	6810
Strontium	µg l <sup>-1</sup>	5000
Sulphate as SO4	mg l <sup>-1</sup>	1750
Mercury	µg l <sup>-1</sup>	<0.01
Nitrate as N	mg l <sup>-1</sup>	<1.43
Carbon, Organic: Total as C :- {TOC}	mg l <sup>-1</sup>	2.3





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**Table 17**

<b>Dissolved inorganic nitrogen standards for transitional water (salinity 25), or part of such water, (transitional waters categorised by type in accordance with paragraph 3 of Schedule 2)</b>				
<i>Mean dissolved inorganic nitrogen concentration (micromoles per litre) during the period 1<sup>st</sup> November to 28<sup>th</sup> February</i>				
	<i>Dissolved inorganic nitrogen concentration (micromoles per litre)</i>			
<i>Type</i>	<i>High</i>	<i>Good</i>	<i>Moderate</i>	<i>Poor</i>
	Mean for the period 1 <sup>st</sup> Nov to 28 <sup>th</sup> Feb			
Clear	20 <sup>(i)</sup>	30 <sup>(i)</sup>	45 <sup>(i)</sup>	67.5 <sup>(i)</sup>
	99 percentile standard for the period 1 <sup>st</sup> Nov to 28 <sup>th</sup> Feb			
Intermediate turbidity	20	70	105	157.5
Turbid	20	180	270	405
Very turbid	20	270	405	607.5

<sup>(i)</sup> The standard refers to the concentration of dissolved inorganic nitrogen at a mean salinity of 25 for the period of 1<sup>st</sup> November 28<sup>th</sup> February.

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Table 23. Example products for use in ground conditioning, their properties and percentage of key component substances and associated Predicted No Effect Concentrations for each substance or surrogate value for a group of similar substances

Chemical function	Product	Main active substance(s)	Active concentration per day assuming 100% use for 1 intake tunnel and 1 outfall tunnel. Mass (kg)	Predicted no effect concentration for aquatic environment ( $\mu\text{g l}^{-1}$ )
Anti-clogging agent	BASF Rheosoil 143	Sodium lauryl ether sulfate (<30%)	(16 rings x 64 l sec <sup>-1</sup> + 24 rings x 48 l sec <sup>-1</sup> ) x (30% in formulation, 0.3 x 0.1, 10% total residual from spoil x product density 1.05) = 68.5 kg <sup>1</sup>	40 <sup>2</sup>
Soil conditioning-additive	CLB F5 M	2,4-Pentanediol, 2-methyl-( $\leq 10\%$ )	(16 rings x 64 l sec <sup>-1</sup> + 24 rings x 48 l sec <sup>-1</sup> ) x (10% in formulation, 0.1 x 0.1, 10% total residual from spoil x product density 1.05) = 22.8kg <sup>1</sup> total	4300 <sup>3</sup>
		Alcohols, C10-16, ethoxylated, sulfates, sodium salts – ( $\leq 10\%$ )		35 <sup>2</sup>
		Mono-C10-16-alkyl, Sodium sulfate ( $\leq 10\%$ )		4.5 <sup>4</sup>

<sup>1</sup> This value takes account of substance density (1.05), % active substance, and assumes 90% associated to spoil (see later discussion); <sup>2</sup>see Table 15 HERA; <sup>3</sup>see SIDS, 2001, <sup>4</sup>see Table 13 HERA, 2002

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Table 24. Environment Agency screening assessment of surfactant components of products. Example chemicals for use in ground conditioning, their properties and fate

Conditioning product	Estimated Discharge concentration mg l <sup>-1</sup> of active substance. Case D	Saltwater AA EQS <sup>1</sup> µg l <sup>-1</sup>	Background concentration n µg l <sup>-1</sup>	Effective volume flux (Case D) (concentration in discharge (µg l <sup>-1</sup> ) x discharge volume (m <sup>3</sup> s <sup>-1</sup> )) / EQS or equivalent (µg l <sup>-1</sup> ) - background (µg l <sup>-1</sup> )	TraC Water test 5 EVF < 3.0 (Pass/Fail)
BASF Rheosoil 143	19.8	40	0	$(19800 \times 0.040) / (40 \times 0) = 19.80$	Fail
CLB F5 M Ethoxylated sulphates	6.6	35	0	$(6600 \times 0.040) / (35 \times 0) = 7.54$	Fail
CLB F5 M Mono- alkyl sodium sulphate	6.6	4.5	0	$(6600 \times 0.040) / (4.5 \times 0) = 58.67$	Fail

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Table 25: H1 Test 1 and 5 for discharges of commissioning chemicals and construction inputs.

Substance	Estimated discharge concentration $\mu\text{g l}^{-1}$	Saltwater AA EQS $\mu\text{g l}^{-1}$	Background concentration $\mu\text{g l}^{-1}$	Effective volume flux Total flow 70 l/s	TraC Water test 5 EVF < 3.0 (Pass/Fail)
Ethanolamine	4000	160	-	1.75	Pass
Total ammonia from commissioning including Case D inputs	281240 <sup>1</sup>	1100	124	21	Fail
Unionised ammonia - from construction wastewater and commissioning inputs including chemical breakdown products converted to un-ionised ammonia assuming commissioning wastewater pH 10 and mean temperature 12.5	187682	21	0.2	977	Fail
Hydrazine	10	0.0004	0.00015	2800	Fail

<sup>1</sup>Total ammonia includes 271206  $\mu\text{g l}^{-1}$  from commissioning + 10034  $\mu\text{g l}^{-1}$  from Case Dmax construction (see Table 8). Note that for modelling the construction discharges is modelled as a separate continuous input and the commissioning as a pulse discharge see section 4.10.2

100805769 / Revision 14 / NOT PROTECTIVELY MARKED / Hinkley Point C / Construction Discharge Modelling Assessment / Table 25: H1 Test 1 and 5 for discharges of commissioning chemicals and construction inputs.

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Table 26. Groundwater and sewage contributions of ammoniacal nitrogen, nitrogen, and phosphorus for Case D1max

Case Dmax	NH <sub>4</sub> -N µg l <sup>-1</sup>	Discharge rate litres/second	Total mass NH <sub>4</sub> -N µg	DIN µg l <sup>-1</sup>	Discharge rate litres/second	Total mass DIN µg	PO <sub>4</sub> -P µg l <sup>-1</sup>	Discharge rate litres/second	Total mass phosphate PO <sub>4</sub> -P µg
Sewage	20000 <sup>1</sup>	13.3	266000	20000	13.3	266000	10000 <sup>3</sup>	13.3	133000
Groundwater	4732 <sup>1</sup>	25	118300	2951 <sup>2</sup>	25	73775	48 <sup>4</sup>	25	1200
Total concentration in discharge		<b>38.3 (l/second)</b>	(total sewage + groundwater/ discharge rate) = <b>10034</b> (µg l <sup>-1</sup> )		<b>38.3 (l/second)</b>	(total sewage + groundwater/ discharge rate) = <b>8871</b> (µg l <sup>-1</sup> )		<b>38.3 (l/second)</b>	(total sewage + groundwater/ discharge rate) = <b>3504</b> (µg l <sup>-1</sup> )
Loading (kg/year)						<b>10713.44</b> <sup>5</sup>			<b>4227.40</b> <sup>6</sup>

<sup>1</sup> see section 4.6 for derivation of source values – these are 95 percentiles to assess most conservative case for toxicity.

<sup>2</sup> This is the mean dissolved inorganic nitrogen input level from groundwater to be used in support of annual assessment.

<sup>3</sup> A concentration 10mg l<sup>-1</sup> as P was derived for treated sewage from package units based on Natural England, 2016; 4: For groundwater a 50<sup>th</sup> percentile value of 0.048mg l<sup>-1</sup> as TP was derived for Wessex groundwater by Stuart and Lapworth, 2016 and is used here as a substitute prior to full site data becoming available. 5: ((38.3 x 60 x 60 x24) x(0.000008871) x 365 =10713.44 kg; 6: ((38.3 x 60 x 60 x24) x(0.000003504) x 365 =4227.40 kg. (Following Environment Agency recalculation of groundwater nitrogen inputs total sewage and groundwater inputs are 8160 (µg l<sup>-1</sup>) and total loading kg/yr is 9855.9 (µg l<sup>-1</sup>)

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Table 27. Potential ammonia, nitrogen, and phosphorus contributions from cold commissioning chemical breakdown products

Conditioning product	Estimated conditioning concentration $\mu\text{g l}^{-1}$	Contribution as un-ionised ammonia ( $\text{NH}_3\text{-N}$ ) $\mu\text{g l}^{-1}$	Nitrogen contribution (kg)	Phosphorus contribution (kg)
Hydrazine	400000	175000 <sup>1</sup>	3271	-
Un-ionised ammonia	12000	12000	505	-
Ethanolamine	1180	636.5	85.88	-
Total un-ionised ammonia	-	187637	-	-
Total equivalent proportion ammonia ( $\text{NH}_4\text{-N}$ ) <sup>2</sup>	-	<b>271206<sup>2</sup></b>	-	-
Total nitrogen (cold commissioning)			<b><u>3862</u></b>	-
Total $\text{PO}_4\text{-P}$ (cold commissioning)				<b><u>201.85<sup>3</sup></u></b>
Total nitrogen construction Case D and cold commissioning (kg/year)			10713.44 + 3862= <b><u>14575<sup>4</sup></u></b>	
Total phosphorus construction Case D and cold commissioning (kg/year)				4227.40 + 201.92= <b><u>4429</u></b>

<sup>1</sup> Hydrazine breakdown pathway assumed  $2\text{N}_2\text{H}_4 + 0.5 \text{O}_2 \rightarrow \text{N}_2 + 2\text{NH}_3 + \text{H}_2\text{O}$ ; <sup>2</sup> This value is derived using the un-ionised ammonia calculator assuming conditioning solution parameters of pH of 10, salinity of 1 and annual average temperature at Hinkley Point 12.5 C. <sup>3</sup> This value was rounded up to 272 mg/l for GETM modelling.

<sup>3</sup> The total phosphorus contribution is based on maximum dose rate of 500ppm trisodium phosphate resulting in a maximum annual loading of 1068.35 kg trisodium phosphate which is equivalent to the  $\text{PO}_4\text{-P}$  loading shown.

<sup>4</sup> Following Environment Agency recalculation of groundwater nitrogen a value of 9,855.9 kg/y is added to the input for commissioning 3862 kg/y and results in an overall reduced loading of 13,717.9 kg/y

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Table 29. Cumulative annual loading nitrogen based on variable groundwater discharge

Year	Calculation of annual loading
Year 1	$(365 \times 24 \times 3600)^1 \times (2951^2 \times 30.5^3 + 5000^4 \times 13.3^5) / (1000 \times 1000000)^6 = 4934 \text{ kg N}$ (following Environment Agency recalculation of the groundwater nitrogen input a mean dewatering concentration of 1861 is substituted for 2951= total loading of 3886.8 kg N)
Year 2	$365 \times 24 \times 3600 \times (2951 \times 27.5 + 5000 \times 13.3) / (1000 \times 1000000) = 4655 \text{ kg N}$ (Updated loading 3710.6 kg N)
Year 3	$365 \times 24 \times 3600 \times (2951 \times 23.8 + 5000 \times 13.3) / (1000 \times 1000000) = 4316 \text{ kg N}$ (Updated loading 3497.2 kg N)

Notes: <sup>1</sup>days, hours, minutes, seconds;

<sup>2</sup>mean dewatering concentration nitrogen ( $\mu\text{g l}^{-1}$ ); <sup>3</sup>groundwater ( $\text{l sec}^{-1}$ );

<sup>4</sup>ammoniacal nitrogen as a proxy for total nitrogen from sewage treatment ( $\mu\text{g l}^{-1}$ ) as other contributions e.g.  $\text{NO}_2$ ,  $\text{NO}_3$  are small ; <sup>5</sup>discharge rate ( $\text{l sec}^{-1}$ );

<sup>6</sup>conversion of units to kilograms.

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## Appendix D CORMIX modelling dilution rates.

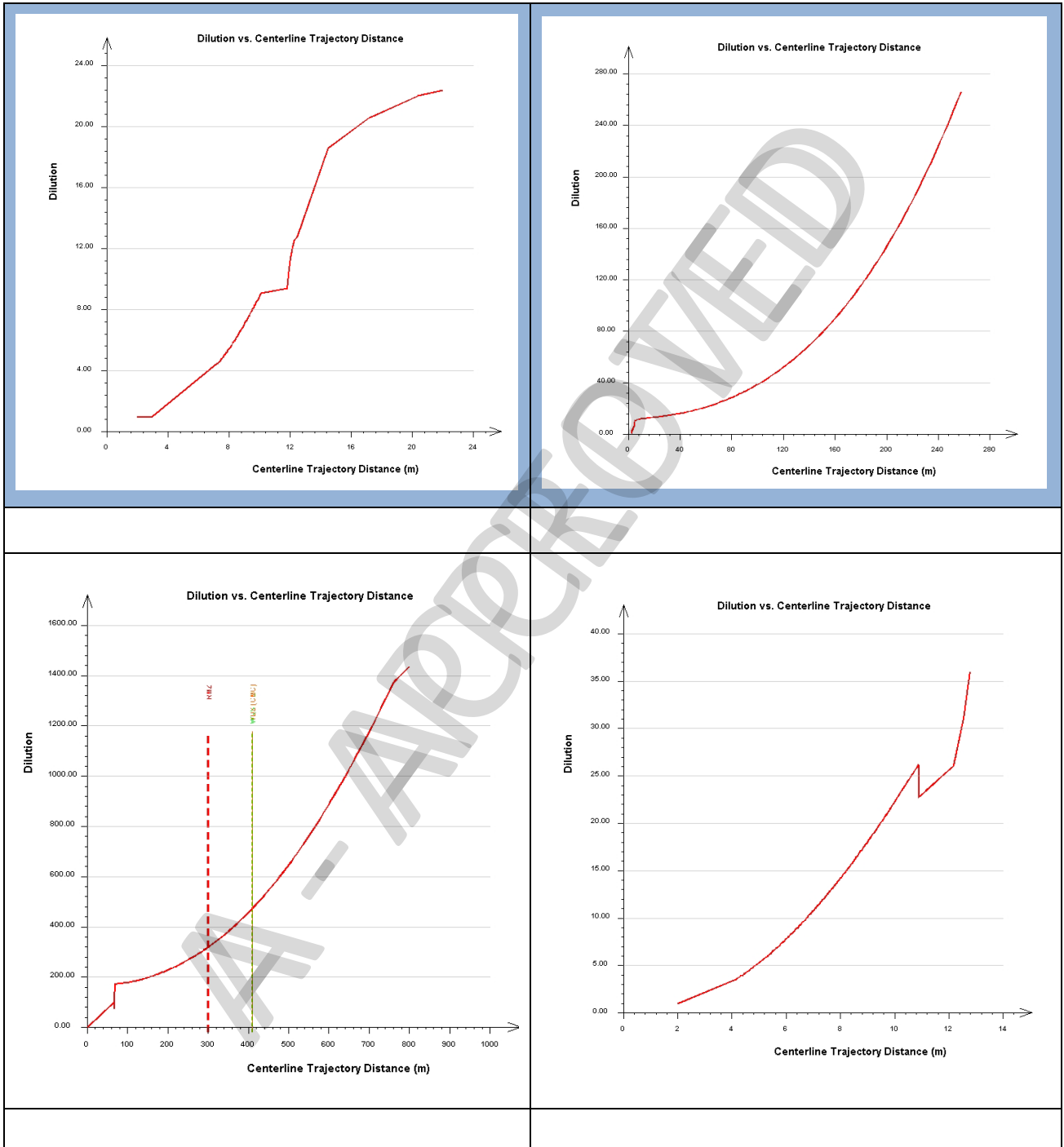


Figure 27. Dilution from low tide to high tide for a  $45 \text{ l s}^{-1}$  discharge at the jetty. Relevant for Case D.

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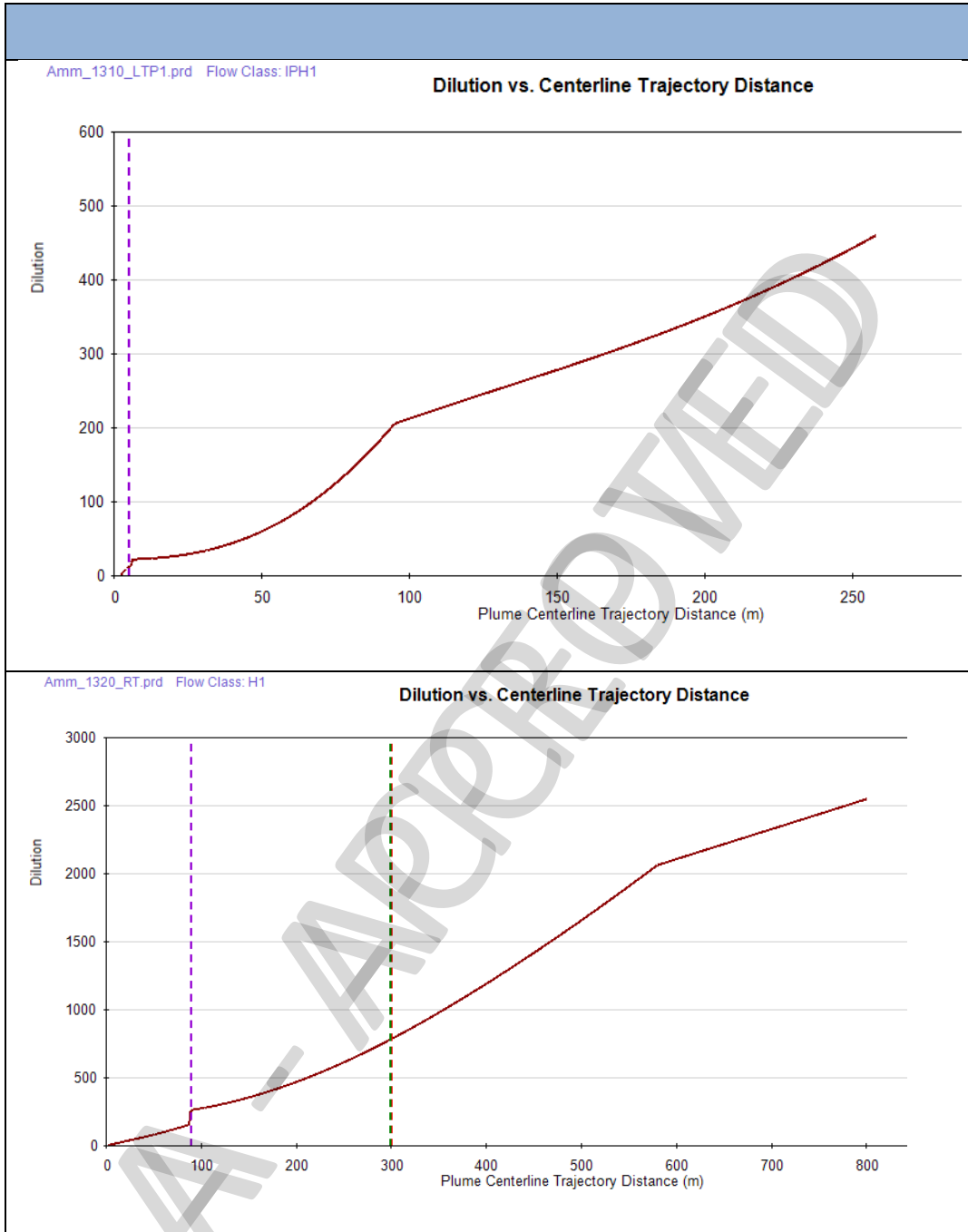


Figure 29. Dilution rates for 13.3 l s<sup>-1</sup> simulation for 1hr after low tide (top) and mid tide (bottom).

It is evident from the figures above that it is the shape of the plume around the low tide simulation that is a potential concern as this is when high concentrations at the seabed are most likely to occur.

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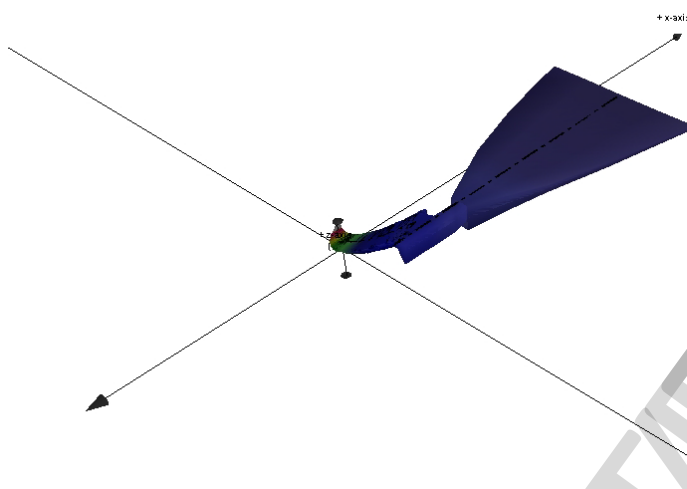


Figure 30. CORMIX output near low water slack, showing the buoyant nature of the plume for  $45 \text{ l s}^{-1}$  discharge.

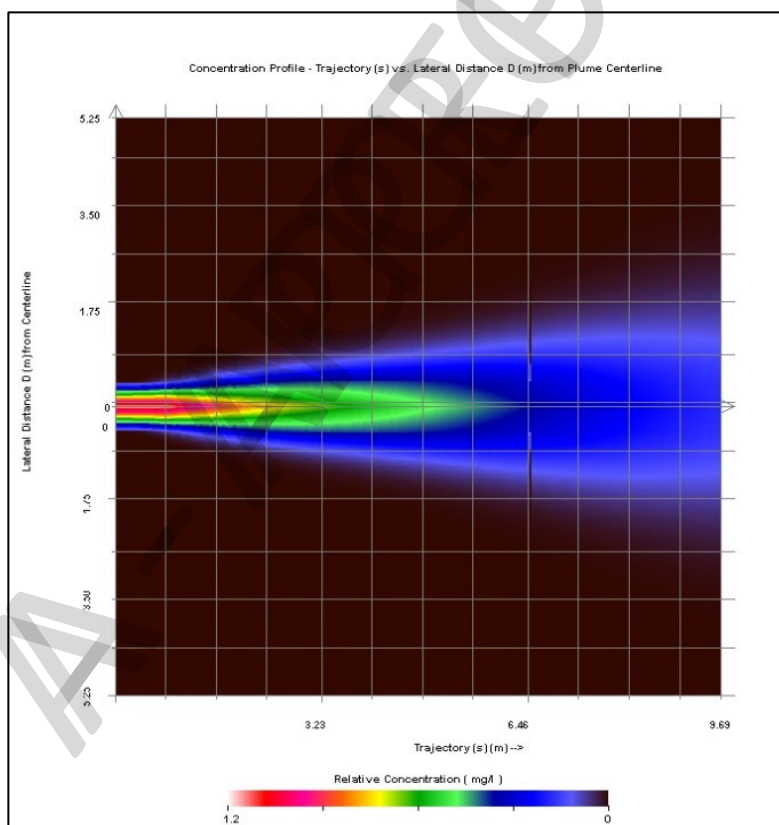


Figure 31. CORMIX outputs showing the dilution of the plume at higher spatial resolution than the GETM 25 m Hinkley Point model can achieve.

100805769-2023-09-14 10:08:05 100805769-2023-09-14 10:08:05 100805769-2023-09-14 10:08:05 100805769-2023-09-14 10:08:05 100805769-2023-09-14 10:08:05 100805769-2023-09-14 10:08:05

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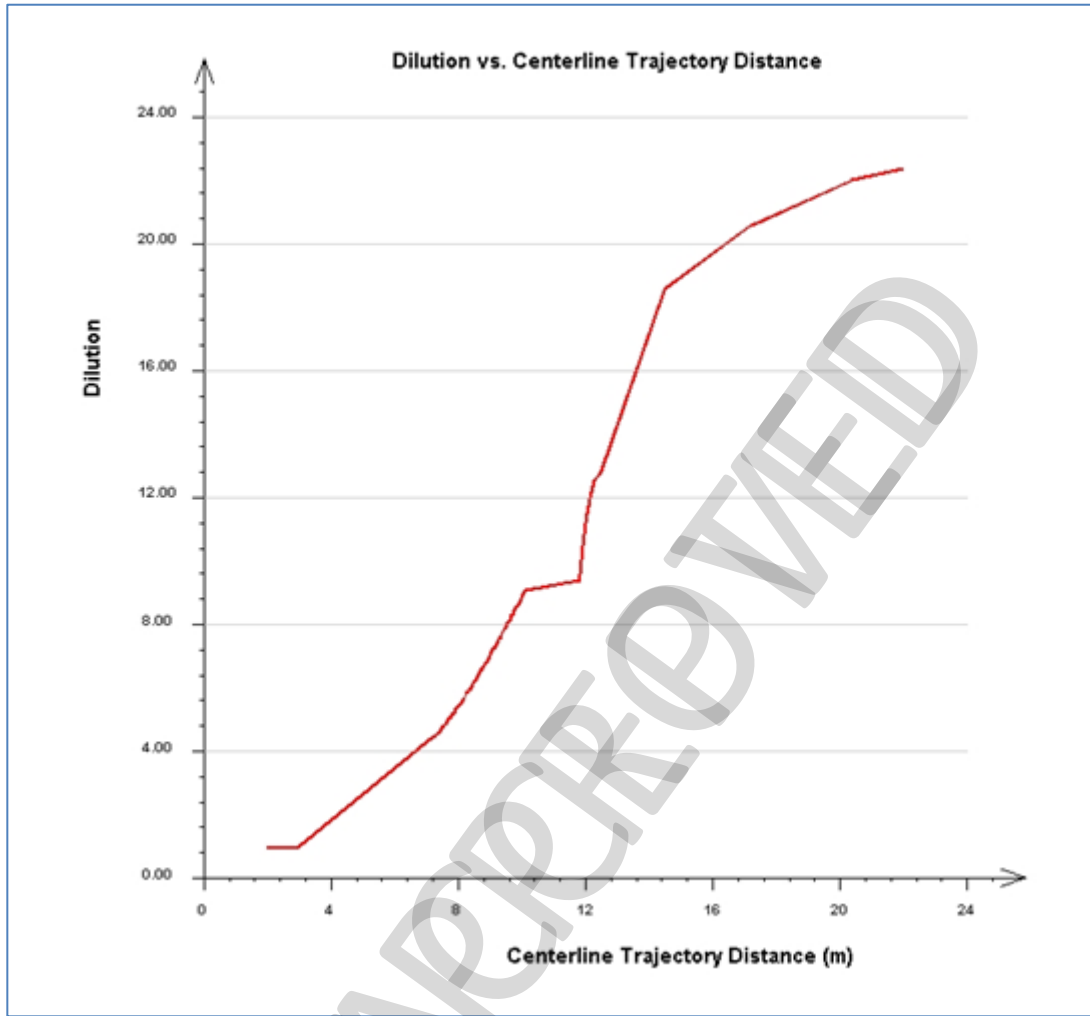


Figure 32. CORMIX outputs showing the dilution of the plume along the centreline 45 l s<sup>-1</sup> simulation at low water. The size of GETM grid cells used in the Hinkley Point model was 25m. CORMIX predicted dilution is approximately 22-fold at 25 m from the discharge i.e. by the edge of the 1<sup>st</sup> GETM grid cell.

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## Appendix E Simulation of ponded water when high concentrations of Zinc could occur.

The purpose of this appendix is to demonstrate that the model accurately replicates potentially high concentrations of zinc which could be formed around periods of slack water. These periods are mostly likely to occur around neap tide, and so this period has been investigated.

The purpose of this appendix is to demonstrate that the model accurately replicates potentially high concentrations of zinc which could be formed around periods of slack water. These periods are mostly likely to occur around neap tide, and so this period has been investigated.

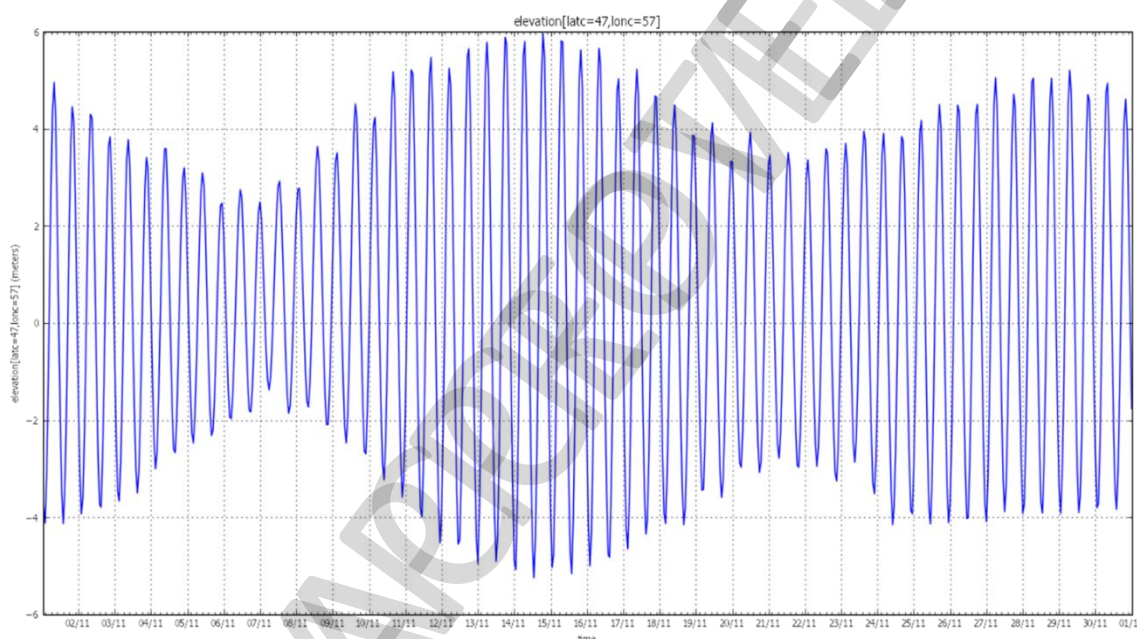


Figure 33. Spring Neap cycle (mean sea level) from model. Note the neap tides on 6th - 7th November, when it is most likely that water from the discharge will temporarily form a static pond.

As can be seen from the plots below, high concentrations above  $0.06 \text{ mg l}^{-1}$  (in fact up to  $0.18 \text{ mg l}^{-1}$ ) are simulated at neap tides. This is consistent with a peak discharge of  $1.2 \text{ mg l}^{-1}$  and an expected dilution of approximately 20 m by 25 m distance from the discharge. At other tidal state dilution occurs much quicker, and the area of high values is confined to the discharge.

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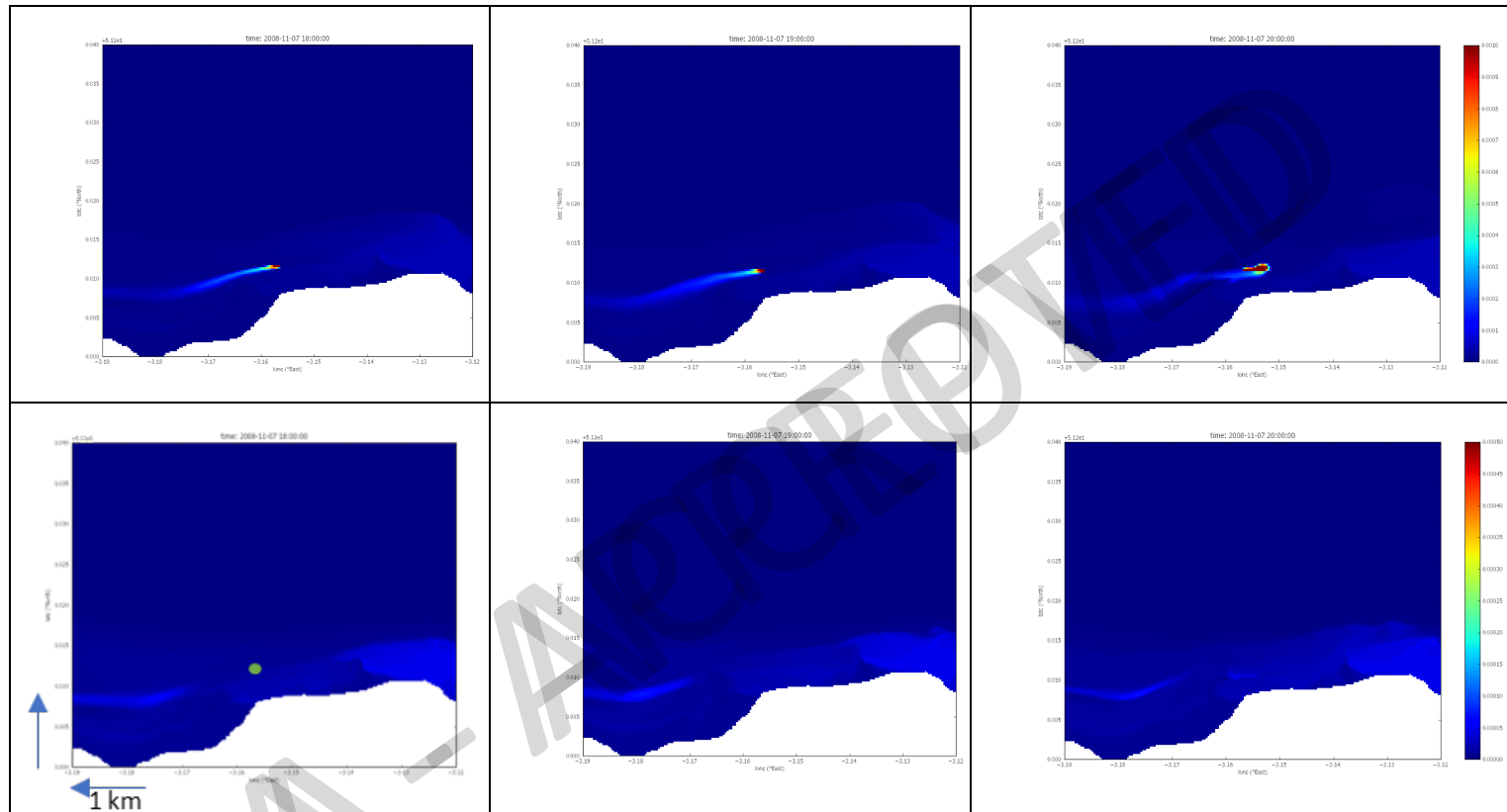


Figure 34. Top panel surface, bottom panel near bed (mg l<sup>-1</sup>). EQS is 0.0038 mg l<sup>-1</sup>. Green dot marks approximate position of the buoyant discharge. Note that the top panel concentrations are on different scale to the bottom panel concentrations, surface concentrations are approximately double those of the bottom. Tide is ebbing until 19:00 with low water slack at 19:30, the tide then changes to the flood tide, so that at 20:00 ponded water is in the same position at 18:00. Plots are not geographically projected thus the arrows indicate length of 1 km.

**Cefas BEEMS Technical Report TR428; Hinkley Point C  
construction discharge modelling assessment at the  
temporary jetty location**

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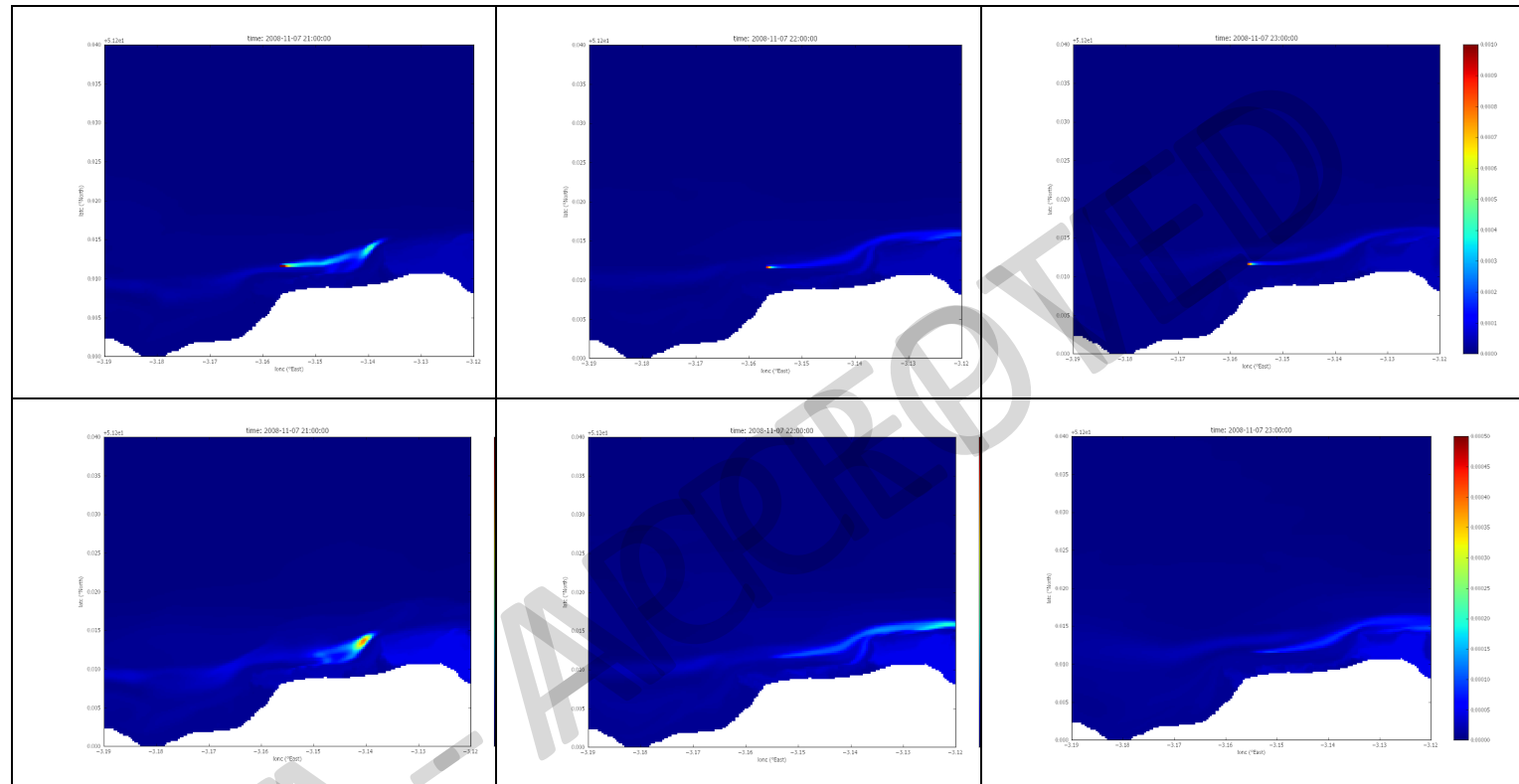


Figure 35. Top panel surface (mg l<sup>-1</sup>), bottom panel near bed (mg l<sup>-1</sup>). EQS is 0.0038 mg l<sup>-1</sup>. Green dot marks approximate position of the buoyant discharge. Note that the top panel concentrations are on different scale to the bottom panel concentrations, surface concentrations are approximately double those of the bottom. 21:00 is during the flood tide, not the passage of the peak to the East, with high water at 24:00.







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construction discharge modelling assessment at the  
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**F.3.1 Incorporation of nutrients.**

The model runs are a baseline run, with no additional nutrients, and a HPC construction and commissioning discharge run including the nutrients due to the discharge from conditioning chemicals, treated sewage, groundwater discharge, and due to the breakdown products of the hydrazine and other commissioning chemicals.

Table 31 Nutrient inputs to model

Waterbody Name	Nutrient addition per year kg	Phosphate per year kg
Bridgwater Bay Reference	No additional input	No additional input.
HPC Construction nutrients.	14575 <sup>1</sup>	4429

<sup>1</sup> Based on updated calculation by the Environment Agency of groundwater nitrogen inputs an adjusted total loading of nitrogen from groundwater+ sewage+ commissioning inputs is calculated as 13,717.9 kg/year

**Model Results - production**

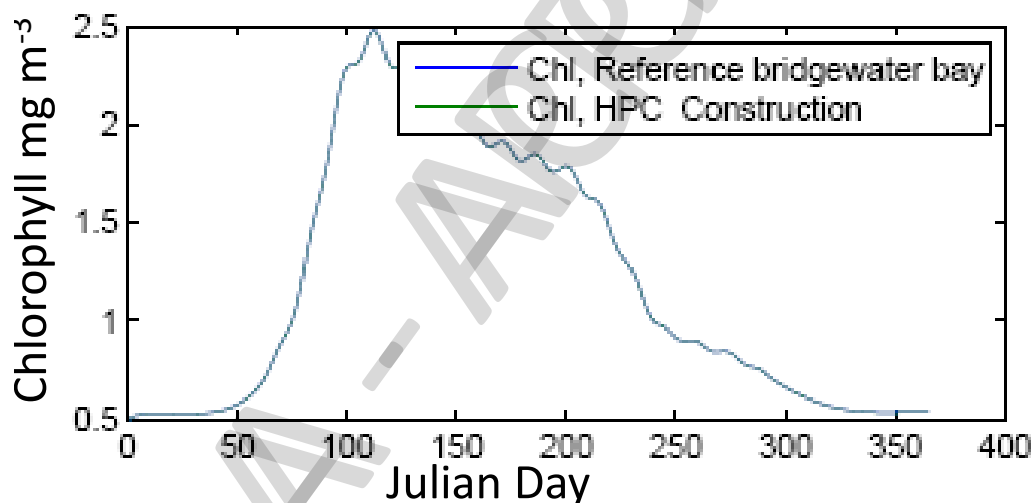


Figure 38: Instantaneous phytoplankton levels (mg Chlorophyll m<sup>-3</sup>), for Bridgwater Bay with no power station discharge, HPC construction, Note there is no discernible difference, construction and reference lines are the same.

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**Cefas BEEMS Technical Report TR428; Hinkley Point C  
construction discharge modelling assessment at the  
temporary jetty location**

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Table 32 Phytoplankton and Macro Algae production

Scenario kd ( 1)	Phyto Annual Gross Production, (g C m <sup>-2</sup> y <sup>-1</sup> )	Macro Annual Gross Production, (g C m <sup>-2</sup> y <sup>-1</sup> )
Bridgwater Bay	11.05	18.43
HPC Construction	11.05	18.43

Evident from above is that there is no difference between the simulations, which is entirely consistent with the known understanding of this high turbidity environment where nutrients are never limiting. Model results using Kd of 1 give estimates of 18 g C m<sup>-2</sup> y<sup>-1</sup> for macroalgal production which is broadly similar to values as estimated by Underwood (2010) of 33 g C m<sup>-2</sup> y<sup>-1</sup>, which applies to a wider geographic context.

**F.3.2 Limiting factors that control phytoplankton growth.**

The model shows which factors are limiting, during the annual cycle, as demonstrated below. Light is the limiting factor throughout the entire year. Therefore, additional nutrient input makes no difference to the output production.

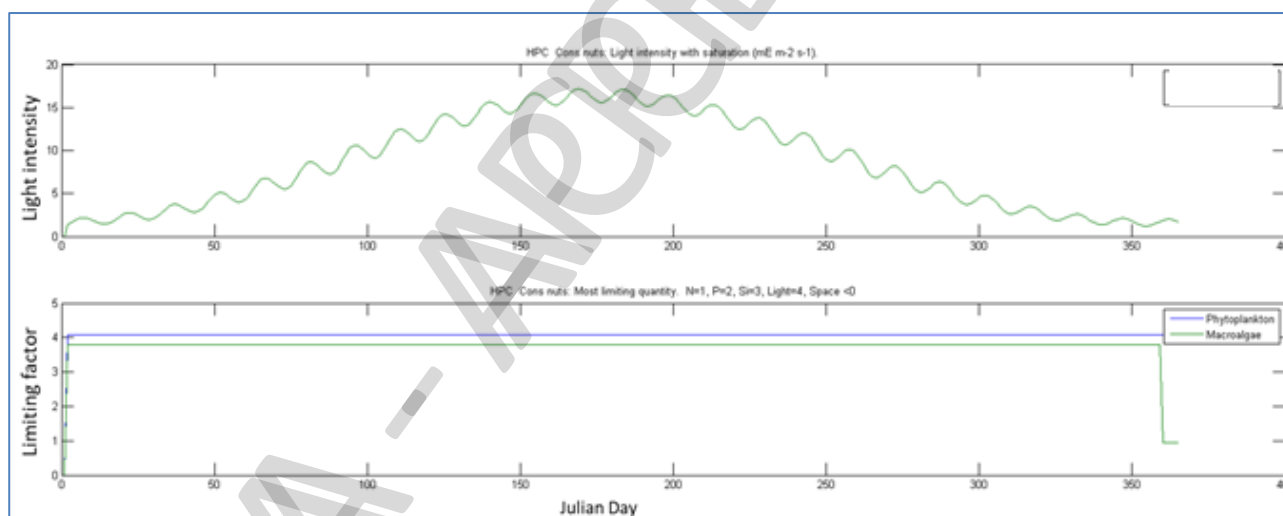


Figure 39: Limiting factors controlling phytoplankton growth, top figure is light intensity, bottom figure is the limiting parameter. Factor 4 'light' is the limiting factor for both phytoplankton and macroalgae.

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**APPENDIX C AMMONIACAL NITROGEN AND DIN DATA FOR  
OUTLET 12 EFFLUENTS**

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## C.1 Groundwater and Tunnel Effluent data

Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
23/03/2017	0.09			2.23		
24/03/2017	0.02			0.43		
25/03/2017	0.03			0.45		
26/03/2017	0.03			0.55		
27/03/2017	0.12			0.86		
28/03/2017	1.06			4.58		
01/04/2017	0.23			3.42		
02/04/2017	0.03			0.66		
03/04/2017	0.17			1.03		
04/04/2017	0.08			0.31		
05/04/2017	0.02			0.33		
06/04/2017	0.16			1.01		
07/04/2017	0.09			0.42		
08/04/2017	0.1			0.43		
09/04/2017	0.08			0.41		
10/04/2017	0.09			0.62		
11/04/2017	0.12			0.56		
12/04/2017	0.1			0.43		
13/04/2017	0.08			0.4		
19/04/2017	0.11			0.34		
26/04/2017	0.17			0.42		
27/04/2017	0.12			0.46		
03/05/2017	0.13			0.37		
10/05/2017	0.03			0.25		
12/05/2017	0.13			0.13		
18/05/2017	0.3			0.57		
24/05/2017	0.19			0.64		
25/05/2017	0.16			0.6		

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
01/06/2017	0.11			0.3		
08/06/2017	0.13			0.56		
15/06/2017	0.07			0.69		
29/06/2017	0.17			0.42		
13/07/2017	1.3			2.25		
27/07/2017	0.4			0.71		
10/08/2017	0.8			1.4		
24/08/2017	0.4			0.8		
14/09/2017	0.6			1.14		
28/09/2017	1.5			2.03		
12/10/2017	0.5			1.05		
26/10/2017	0.9			1.62		
09/11/2017	0.7			1.27		
24/11/2017	0.4			0.8		
07/12/2017	0.5			0.83		
14/12/2017	0.5			1		
21/12/2017	0.5			0.86		
11/01/2018	0.6			1.15		
25/01/2018	0.3			0.58		
08/02/2018	0.5			1.02		
22/02/2018	0.4			0.7		
08/03/2018	1.1			1.67		
09/03/2018	1.4			2.04		
22/03/2018	0.6			0.94		
12/04/2018	0.8			2.12		
26/04/2018	0.3			0.57		
10/05/2018	0.2			0.45		
11/05/2018	0.2			0.45		
24/05/2018	0.3			0.57		
14/06/2018	0.41			0.91		

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
28/06/2018	0.7			1.08		
12/07/2018	1.6			2.39		
26/07/2018	0.6			0.97		
09/08/2018	1.1			1.82		
23/08/2018	0.6			0.97		
13/09/2018	1.1			1.89		
27/09/2018	0.4			0.84		
11/10/2018	0.8			1.46		
25/10/2018	0.3			0.67		
08/11/2018	0.8			1.84		
21/11/2018		0.3			0.57	
13/12/2018		0.5			0.94	
10/01/2019		0.5			0.83	
26/01/2019		0.4			0.71	
27/01/2019		0.5			0.83	
28/01/2019		0.4			0.72	
29/01/2019		0.5			1.63	
30/01/2019		0.9			1.54	
31/01/2019		0.6			1.05	
01/02/2019		0.6			0.95	
02/02/2019		0.5			0.84	
03/02/2019		0.7			1.08	
04/02/2019		0.8			1.19	
05/02/2019		1			1.44	
06/02/2019		1.3			1.82	
07/02/2019		1.2			1.69	
08/02/2019		1.3			1.81	
09/02/2019		1.4			1.94	
10/02/2019		1.3			1.81	
11/02/2019		1.2			1.69	

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
12/02/2019		0.9			1.32	
14/02/2019		1			1.43	
14/03/2019		0.7			1.51	
11/04/2019		0.7			1.07	
09/05/2019		1.2			1.5	
13/06/2019		0.8			1.69	
11/07/2019		1			1.42	
18/07/2019		0.4			0.61	
25/07/2019		0.6			0.82	
01/08/2019		0.5			0.71	
08/08/2019		1.2			1.69	
15/08/2019		4			4.5	
22/08/2019		0.93			1.6	
29/08/2019		2.3			2.4	
05/09/2019		0.76			0.8	
12/09/2019		1.79			1.8	
19/09/2019		0.72			0.8	
26/09/2019		2.3			2.7	
03/10/2019		3.8			3.8	
10/10/2019		1.05			2.8	
17/10/2019		0.66			0.8	
24/10/2019		0.58			0.8	
31/10/2019		0.78			1.8	
07/11/2019		1.12			2.7	
14/11/2019		1.21			1.8	
21/11/2019		0.58			0.9	
28/11/2019		1.2			1.4	
05/12/2019		0.62			0.6	
12/12/2019		1.13			1.2	
19/12/2019		0.52			0.7	

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
27/12/2019		0.37			0.7	
02/01/2020		0.54			0.7	
09/01/2020		0.93			1.6	
16/01/2020		4.3			4.4	
23/01/2020		0.51			0.8	
30/01/2020		0.66			2.4	
13/02/2020		0.4	0.51		0.5	1.4
12/03/2020		0.53			0.7	
09/04/2020		0.54			0.6	
23/04/2020		0.5			0.6	
14/05/2020		0.55	1.2		0.7	2
11/06/2020		0.46			0.5	
18/06/2020			1			1.6
09/07/2020		0.44	1.2		0.4	1.2
16/07/2020			1.4			2.1
24/07/2020			0.36			1
30/07/2020			1			1.8
07/08/2020			0.61			0.6
13/08/2020		1.7	0.86		1.7	1.2
20/08/2020			1.9			2.1
27/08/2020			3			3
07/09/2020			1.2			1.7
10/09/2020		0.54			0.7	
11/09/2020			1.4			2
22/09/2020			1.2			1.6
01/10/2020			1.4			1.9
08/10/2020		0.42			0.5	
12/11/2020		0.59	0.75		0.6	1.1
01/12/2020		0.77	4.3		0.9	4.4
05/01/2021		0.48			0.6	

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
21/01/2021			0.47			1.4
02/02/2021		0.44			0.4	
16/02/2021			1.4			2.6
02/03/2021		1.3			1.3	
03/03/2021			1.7			2.8
24/03/2021			1.2			0
29/03/2021			0.12			0
06/04/2021		1	1.2		1	2.4
04/05/2021		0.57			0.6	
11/05/2021			1.2			2.4
18/05/2021			0.16			0
01/06/2021		0.59	1.8		0.8	2.1
15/06/2021		14.51			17.5	
29/06/2021		0.78			0.8	
06/07/2021		0.58	0.93		0.6	1.3
08/07/2021		0.45			0.7	
13/07/2021		0.51			0.5	
20/07/2021		0.594750563			0.5	
03/08/2021		1.4			1.4	
19/08/2021			0.12			1.1
07/09/2021		0.44	0.56		0.4	0.6
14/09/2021		0.45			0.5	
05/10/2021		1.5	0.16		1.5	1
02/11/2021		1.12	0.8		1.4	2.6
07/12/2021		0.6			0.8	
08/12/2021			1.1			1.8
04/01/2022		0.4	1.3		0.6	2.4
01/02/2022		0.4			0.4	
03/02/2022			2.3			2.5
01/03/2022		0.4			0.6	

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Date	Ammoniacal Nitrogen as N (mg/l)			Sum of Dissolved Inorganic Nitrogen (mg/l)		
	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE	Outlet 1 - GW	Outlet 12-GW	Outlet 12-TE
09/03/2022			1.2			2.3
04/04/2022		0.3			0.5	
07/04/2022			0.09			0.89
03/05/2022		0.3			0.5	
11/05/2022			16.5			17.1
07/06/2022		0.4			0.6	
08/06/2022			0.6			2
05/07/2022		0.6	5.2		0.5	2.8
01/08/2022		0.4			0.9	
02/08/2022			1.4			1.9
06/09/2022		0.3			0.6	
07/09/2022			6			6.8
04/10/2022		0.8	14		1.6	15.6
01/11/2022		0.3	5.4		0.5	6.3
06/12/2022		0.6	13.2		1	17.8
03/01/2023		0.3			0.5	
04/01/2023			4.3			9.3
17/01/2023			4.8			8.4
24/01/2023			2.9			11.5
01/02/2023			5.5			9.7
07/02/2023		0.4	2.8		0.6	10.8
14/02/2023			0.3			0.5
21/02/2023			1.7			2
28/02/2023			1.8			11.1
07/03/2023		0.3	1.5		0.5	10.7
14/03/2023			3.2			10.4
22/03/2023			1.4			10.8
28/03/2023			3.1			11.3
04/04/2023		0.3	1.5		0.7	10.3
02/05/2023		0.3	0.8		0.5	10



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**C.2 CSTP data**

Date Sampled	Ammoniacal nitrogen mg/l N
06/09/2022 11:34	7.85
20/09/2022 08:40	<0.2
27/09/2022 10:06	<0.200
04/11/2022 09:36	10.93
09/11/2022 10:24	16.83
11/11/2022 08:07	14.37
15/11/2022 11:28	0.25
17/11/2022 07:58	9.99
21/11/2022 08:10	<0.2
24/11/2022 11:33	16.63
28/11/2022 11:04	<0.2
02/12/2022 09:25	31.78
09/12/2022 11:05	25.10
12/12/2022 11:24	0.36
14/12/2022 12:12	9.38
19/12/2022 10:23	<0.2
21/12/2022 09:12	<0.2
23/12/2022 07:33	<0.2
19/01/2023 10:32	15.63
01/02/2023 10:22	21.97
14/02/2023 11:11	1.04
27/02/2023 09:33	<0.2
07/03/2023 11:15	12.28
11/04/2023 11:44	<0.2
22/04/2023 09:08	12.79

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**APPENDIX D MODELLING AND CALCULATION FILES**

(Provided separately)

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