

[illegible]



Mass Balance for Cory Decarbonisation Project - Provisional

Project Name	Cory Decarbonisation Project	Project Number	0042614
Client Name	Cory Environmental Holdings Ltd	Client Project No.	
Document No	0042614-WSP-01-XX-CA-PE-0001	Rev.	P1

Stream No.	1	2a-b	3a-b	4a-b	5a-b	6	7	8a-b	9a-b	10	11	12	13	14	15
Description	Combined Flue Gas from Riverside 1 & 2	Flue Gas to CCF Train 1/2	Treated Flue Gas from Absorber(s)	Treated Flue Gas to Atmosphere	CCF Train 1/2 to Liquefaction	To Liquid CO ₂ Storage	Liquid CO ₂ to Ship	Steam to CCF	Condensate Return to Existing Facility	Wastewater from CCF	Treated Water from ETP	Treatment Waste	Amine Top-up	Caustic Top-up	Reclaimer Waste
Pressure	barg			Atm	16	13 - 15	13 - 15	3.5							
Temperature	°C		40	80		-33 to -26	-33 to -26	148							
Quantity	-						1,200			167	172				
Flow Rate	m ³ /hr														
	Nm ³ /hr	515,000	382,000	382,000											
	t/hr				93.7	187.4		100	TBD			800t/a	200 t/a	1700 t/a	500 t/a

General Notes	3		4	4					7				5	5, 6	5
References															

Notes:

1. This document is a provisional mass balance and will be updated during detailed design.	References:
2. Streams with an a/b suffix are per train. Streams are only denoted by a number indicate a combined stream that accounts for both train 1 and 2.	1. To be read in conjunction with Process Flow Diagram 0042614-WSP-01-XX-DR-PE-0001
3. Flue gas flowrate from Riverside 1 & 2 at 100% load	2. More details on the effluent treatment and water recovery can be found on the associated water balance (0042614-WSP-01-XX-DR-PE-0002).
4. The treated flue gas leaves the absorber at 40°C, but is anticipated to require reheat prior to discharge. Reheat requirements are to be confirmed during detailed design.	
5. Flow is intermittent.	
6. Chemicals specified are for carbon capture process requirements only. Additional chemicals are required for water/effluent treatment.	
7. Condensate return conditions and losses to be determined at detailed design.	